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B.E. CHEMICAL ENGG. - I / II

CHEMICAL PROCESSES AND PLANT DESIGN

DATA - BOOK



Instructions - Do not write or mark anything on data book.



APPENDIX OF CALCULATION DATA

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APPENDIX OF CALCULATION DATA

TABLE 1. CONVERSION FACTORS AND CONSTANTS

Energy and power:

Btu = 0.252 kg-cal
Btu = 0.293 watt-hr
Btu = 0.555 pcu (pound centigrade unit)
Btu = 778 ft-lb
Btu/min = 0.236 hp
Hp = 42.4 Btu/min
Hp = 33,000 ft-lb/min
Hp = 0.7457 kw
Hp-hr = 2543 Btu
Kw = 1.3415 hp
Watt-hr = 3.415 Btu

Fluid flow:

Bbl/hr = 0.0936 cfm
Bbl/hr = 0.700 gpm
Bbl/day = 0.0292 gpm
Bbl/day = 0.0039 cfm
Cfm = 10.686 bbl/hr
Gpm = 1.429 bbl/hr
Gpm = 34.3 bbl/day
Gpm \times s (specific gravity) = 500 \times s lb/hr

Heat-transfer coefficients:

Btu/(hr)(ft²)(°F) = 1.0 pcu/(hr)(ft²)(°C)
Btu/(hr)(ft²)(°F) = 4.88 kg-cal/(hr)(m²)(°C)
Btu/(hr)(ft²)(°F) = 0.00204 watts/(in.²)(°F)

Length, area, and volume:

Bbl = 42 gal
Bbl = 5.615 ft³
Cm = 0.3937 in.
Ft³ = 0.1781 bbl
Ft³ = 7.48 gal
Ft³ = 0.0283 m³
M³ = 6.290 bbl
M³ = 35.314 ft³
Ft = 30.48 cm
Ft = 0.3048 m
Gal = 0.02381 bbl
Gal = 0.1337 ft³
Gal = 3.785 liter
Gal = 0.8327 gal (Imperial)
In. = 2.54 cm
Liter = 0.2642 gal
Liter = 1.0567 qt
M = 3.281 ft
Ft² = 0.0929 m²
M² = 10.76 ft²

PROCESS HEAT TRANSFER



APPENDIX OF CALCULATION DATA

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Pressure:

- Atm = 33.93 ft of water at 60°F
- Atm = 29.92 in. Hg at 32°F
- Atm = 760 mm Hg at 32°F
- Atm = 14.696 psi
- Atm = 2116.8 lb/ft²
- Atm = 1.033 kg/cm²
- Ft of water at 60°F = 0.4331 psi
- In. of water at 60°F = 0.0361 psi
- Kg/cm² = 14.223 psi
- Psi = 2.309 Ft of water at 60°F

Temperature:

- Temperature °C = $\frac{5}{9}(\text{°F} - 32)$
- Temperature °F = $\frac{9}{5}(\text{°C} + 32)$
- Temperature °F absolute (°R) = °F + 460
- Temperature °C absolute (°K) = °C + 273

Thermal conductivity:

- Btu/(hr)(ft²)(°F/ft) = 12 Btu/(hr)(ft²)(°F/in.)
- Btu/(hr)(ft²)(°F/ft) = 1.49 kg-cal/(hr)(m²)(°C/m)
- Btu/(hr)(ft²)(°F/ft) = 0.0173 watts/(cm²)(°C/cm)

Viscosity (additional factors are contained in Fig. 13):

- Poise = 1 g/(cm)(sec)
- Centipoise = 0.01 poise
- Centipoise = 2.42 lb/(ft)(hr)

Weight:

- Lb = 0.4536 kg
- Lb = 7000 grains
- Ton (short or net) = 2000 lb
- Ton (long) = 2240 lb
- Ton (metric) = 2205 lb
- Ton (metric) = 1000 kg

Constants:

- Acceleration of gravity = 32.2 ft/sec²
- Acceleration of gravity = 4.18×10^8 ft/hr²
- Density of a cubic foot of water = 62.5 lb/ft³

TABLE 2. THERMAL CONDUCTIVITIES OF SOME BUILDING AND INSULATING MATERIALS*
k = Btu/(hr)(ft²)(°F/ft)

Material	Apparent density ρ, lb/ft ³ at room temperature	°F	k	
Aerogel, silica, opacified.....	8.5	248	0.013	
		554	0.026	
Asbestos-cement boards.....	120	68	0.43	
Asbestos sheets.....	55.5	124	0.096	
Asbestos slate.....	112	32	0.087	
		140	0.114	
Asbestos.....	29.3	-328	0.043	
		32	0.090	
		36	0.087	
		36	212	0.111
		36	392	0.120
		36	752	0.129
		43.5	-328	0.090
Aluminum foil, 7 air spaces per 2.5 in.....	0.2	100	0.025	
		351	0.038	
Ashes, wood.....		32-212	0.041	
Asphalt.....	132	68	0.43	
Boiler scale (ref. 364).....				
Bricks				
Alumina (92-99% Al ₂ O ₃ by weight) fused.....		801	1.8	
Alumina (64-65% Al ₂ O ₃ by weight).....		2399	2.7	
(See also Bricks, fire clay).....	115	1472	0.62	
	115	2012	0.63	
Building brickwork.....		68	0.4	
Chrome brick (32% Cr ₂ O ₃ by weight).....	200	392	0.67	
	200	1202	0.85	
	200	2399	1.0	
Diatomaceous earth, natural, across strata	27.7	399	0.051	
	27.7	1600	0.077	
Diatomaceous, natural, parallel to strata	27.7	399	0.081	
	27.7	1600	0.106	
Diatomaceous earth, molded and fired.....	38	399	0.14	
	38	1600	0.18	
Diatomaceous earth and clay, molded and fired.....	42.3	399	0.14	
	42.3	1600	0.19	
Diatomaceous earth, high burn, large pores.....	37	392	0.13	
	37	1832	0.34	



PROCESS HEAT TRANSFER

TABLE 2. THERMAL CONDUCTIVITIES OF SOME BUILDING AND INSULATING MATERIALS.*—(Continued)

Material	Apparent density ρ , lb/ft ³ at room temperature	°F	k
Bricks: (Continued)			
Fire clay, Missouri		392	0.58
		1112	0.85
		1832	0.95
		2552	1.02
Kaolin insulating brick	27	932	0.15
	27	2102	0.26
Kaolin insulating firebrick	19	392	0.050
	19	1400	0.113
Magnesite (86.8% MgO, 6.3% Fe ₂ O ₃ , 3% CaO, 2.6% SiO ₂ by weight)	158	399	2.2
	158	1202	1.6
	158	2192	1.1
Silicon carbide brick, recrystallized	129	1112	10.7
	129	1472	9.2
	129	1832	8.0
	129	2192	7.0
	129	2552	6.3
Calcium carbonate, natural	162	86	1.3
White marble			1.7
Chalk	96		0.4
Calcium sulphate (4H ₂ O), artificial	84.6	104	0.22
Plaster, artificial	132	167	0.43
Building	77.9	77	0.25
Cambric, varnished		100	0.09
Carbon, gas		32-212	2.0
Cardboard, corrugated			0.037
Celluloid	87.3	86	0.12
Charcoal flakes	11.9	176	0.043
	15	176	0.051
Clinker, granular		32-1292	0.27
Coke, petroleum		212	3.4
		932	2.9
Coke, powdered		32-212	0.11
Concrete, cinder			0.20
1:4 dry			0.44
Stone			0.54
Cotton wool	5	86	0.024
Cork board	10	86	0.025
Cork, ground	9.4	86	0.025
Regranulated	8.1	86	0.026

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APPENDIX OF CALCULATION DATA

TABLE 2. THERMAL CONDUCTIVITIES OF SOME BUILDING AND INSULATING MATERIALS.*—(Continued)

Material	Apparent density ρ , lb/ft ³ at room temperature	°F	k
Diatomaceous earth powder, coarse	20.0	100	0.036
	20.0	1600	0.082
Fine	17.2	399	0.040
	17.2	1600	0.074
Molded pipe covering	26.0	399	0.051
	26.0	1600	0.088
4 vol. calcined earth and 1 vol. cement, poured and fired	61.8	399	0.16
	61.8	1600	0.23
Dolomite	167	122	1.0
Ebonite			0.10
Enamel, silicate	38		0.5-0.75
Felt, wool	20.6	86	0.03
Fiber insulating board	14.8	70	0.028
Fiber, red	80.5	68	0.27
With binder, baked		68-207	0.097
Gas carbon		32-212	2.0
Glass			0.2-0.73
Boro-silicate type	139	86-167	0.63
Soda glass			0.3-0.44
Window glass			0.3-0.61
Granite			1.0-2.3
Graphite, dense, commercial		32	86.7
Powdered, through 100 mesh	30	104	0.104
Gypsum, molded and dry	78	68	0.25
Hair, felt, perpendicular to fibers	17	86	0.021
Ice	57.5	32	1.3
Infusorial earth (see Diatomaceous earth)			
Kapok	0.88	68	0.020
Lampblack	10	104	0.038
Lava			0.49
Leather, sole	62.4		0.092
Limestone (15.3 vol % H ₂ O)	103	75	0.54
Linen		86	0.05
Magnesia, powdered	49.7	117	0.35
Magnesia, light carbonate	19	70	0.04
Magnesium oxide, compressed	49.9	68	0.32
Marble			1.2-1.7



PROCESS HEAT TRANSFER

TABLE 2. THERMAL CONDUCTIVITIES OF SOME BUILDING AND INSULATING MATERIALS. *—(Continued)

Material	Apparent density ρ , lb/ft ³ at room temperature	°F	k
Mica, perpendicular to planes.....	122	0.25
Mill shavings.....	0.033-0.05
Mineral wool.....	9.4	86	0.0225
Paper.....	19.7	86	0.024
Paraffin wax.....	0.075
Petroleum coke.....	32	0.14
.....	212	3.4
.....	932	2.9
Porcelain.....	392	0.88
Portland cement (see Concrete).....	194	0.17
Pumice stone.....	70-151	0.14
Pyroxylin plastics.....	0.075
Rubber, hard.....	74.8	32	0.087
Para.....	70	0.109
Soft.....	70	0.075-0.092
Sand, dry.....	94.6	68	0.19
Sandstone.....	140	104	1.06
Sawdust.....	12	70	0.03
Scale (ref. 364).....
Silk.....	6.3	0.026
Varnished.....	100	0.096
Slag, blast furnace.....	75-261	0.064
Slag wool.....	12	86	0.022
Slate.....	201	0.86
Snow.....	34.7	32	0.27
Sulphur, monoclinic.....	212	0.09-0.097
Rhombic.....	70	0.16
Wallboard, insulating type.....	14.8	70	0.028
Wallboard, stiff pasteboard.....	43	86	0.04
Wood shavings.....	8.8	86	0.034
Wood, across grain			
Balsa.....	7-8	86	0.025-0.03
Oak.....	51.5	59	0.12
Maple.....	44.7	122	0.11
Pine, white.....	34.0	59	0.087
Teak.....	40.0	59	0.10
White fir.....	28.1	140	0.062
Wood, parallel to grain			
Pine.....	34.4	70	0.20
Wool, animal.....	6.9	86	0.021

* From L. S. Marks, "Mechanical Engineers' Handbook," McGraw-Hill Book Company, Inc., New York, 1941.

APPENDIX OF CALCULATION DATA

TABLE 3. THERMAL CONDUCTIVITIES, SPECIFIC HEATS, SPECIFIC GRAVITIES OF METALS AND ALLOYS
 $k = \text{Btu}/(\text{hr})(\text{ft}^2)(^\circ\text{F}/\text{ft})$

Substance	Temp, °F	k^*	Specific heat, † Btu/(lb)(°F)	Specific gravity
Aluminum	32	117	0.183	2.55-7.8
Aluminum	212	119	0.1824	
Aluminum	932	155	0.1872	
Antimony	32	10.6	0.0493	
Antimony	212	9.7	0.0508	
Bismuth	64	4.7	0.0294	9.8
Bismuth	212	3.9	0.0304	
Brass (70-30)	32	56	0.1315†	8.4-8.7
Brass	212	60	0.1488†	
Brass	752	67	0.2015†	
Copper	32	224	0.1487	8.8-8.95
Copper	212	218	0.1712	
Copper	932	207	0.2634	
Cadmium	64	53.7	0.0550	8.65
Cadmium	212	52.2	0.0567	
Gold	64	169.0	0.030	19.25-19.35
Gold	212	170.8	0.031	
Iron, cast	32	32	0.1064	7.03-7.13
Iron, cast	212	30	0.1178	
Iron, cast	752	25	0.1519	
Iron, wrought	64	34.6	See Iron	7.6-7.9
Iron, wrought	212	27.6	See Iron	
Lead	32	20	0.0306	11.34
Lead	212	19	0.0315	
Lead	572	18	0.0335	
Magnesium	32-212	92	0.255	1.74
Mercury	32	4.8	0.0329	13.6
Nickel	32	36	0.1050	8.9
Nickel	212	34	0.1170	
Nickel	572	32	0.1408	
Silver	32	242	0.0557	10.4-10.6
Silver	212	238	0.0571	
Steel	32	26	See Iron	7.83
Steel	212	26	See Iron	
Steel	1112	21	See Iron	
Tantalum	64	32	0.0342	16.6
Zinc	32	65	0.0917	6.9-7.2
Zinc	212	64	0.0958	
Zinc	752	54	0.1082	

* From L. S. Marks, "Mechanical Engineers' Handbook," McGraw-Hill Book Company, Inc., New York, 1941.

† From E. R. Kelley, U.S. Bur. Mine Bull. 371 (1939).

‡ Weighted value for copper and zinc.

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TABLE 4. THERMAL CONDUCTIVITIES OF LIQUIDS*
 $k = \text{Btu}/(\text{hr})(\text{ft}^2)(^\circ\text{F}/\text{ft})$

A linear variation with temperature may be assumed. The extreme values given constitute also the temperature limits over which the data are recommended.

Liquid	°F	k	Liquid	°F	k
Acetic acid 100%	68	0.099	Heptyl alcohol (n-)	86	0.094
50%	68	0.20		167	0.091
Acetone	86	0.102	Hexyl alcohol (n-)	86	0.093
	107	0.095		167	0.090
Allyl alcohol	77-86	0.104	Kerosene	68	0.086
Ammonia	68	0.29		167	0.081
Ammonia, aqueous 26%	140	0.261	Lauric acid	212	0.102
Amyl acetate	50	0.083			
Alcohol (n-)	86	0.094	Mercury	82	4.83
	212	0.089	Methyl alcohol 100%	68	0.124
	86	0.088	80%	68	0.154
Aniline	167	0.087	60%	68	0.190
	32-68	0.100	40%	68	0.234
Benzene	86	0.092	20%	68	0.284
	140	0.087	100%	122	0.114
Bromobenzene	86	0.074	Chloride	5	0.111
	212	0.070		86	0.089
Butyl acetate (n-)	77-86	0.085	Nitrobenzene	86	0.095
Alcohol (n-)	86	0.097		212	0.088
(iso-)	167	0.095	Nitromethane	86	0.125
	50	0.091	Nonane (n-)	140	0.120
Calcium chloride brine 30%	86	0.32		86	0.084
15%	86	0.34		140	0.082
Carbon disulphide	86	0.093	Octane (n-)	86	0.083
	167	0.088		140	0.081
Tetrachloride	32	0.107	Oils		
Chlorobenzene	184	0.094	Castor	68	0.104
Chloroform	50	0.083		212	0.100
Cymene (para)	86	0.080	Olive	68	0.097
	140	0.079		212	0.095
Decane (n-)	86	0.085	Oleic acid	212	0.0925
	140	0.083	Palmitic acid	212	0.0835
Dichlorodifluoromethane	140	0.083	Paraldehyde	86	0.084
	60	0.057		212	0.078
	100	0.048	Pentane (n-)	86	0.078
	140	0.043		167	0.074
Dichloroethane	180	0.038	Perchloroethylene	122	0.092
Dichloromethane	122	0.082	Petroleum ether	86	0.075
	5	0.111	Propyl alcohol (n-)	167	0.073
	86	0.096		86	0.089
			Alcohol (iso-)	86	0.091
Ethyl acetate	68	0.101		140	0.090
Alcohol 100%	68	0.105	Sodium	212	49
80%	68	0.137		410	46
60%	68	0.176	Sodium chloride brine 25.0%	86	0.33
40%	68	0.224	12.5%	86	0.34
20%	68	0.281	Stearic acid	212	0.0786
100%	122	0.087	Sulfuric acid 90%	86	0.21
Benzene	86	0.086	60%	86	0.25
	140	0.082	30%	86	0.30
Bromide	86	0.070	Sulfur dioxide	5	0.128
Ether	167	0.079		86	0.111
Iodide	104	0.064	Toluene	86	0.086
	167	0.063		167	0.084
Ethylene glycol	167	0.153	β -trichloroethane	122	0.077
	32	0.163	Trichloroethylene	122	0.080
Gasoline	86	0.078	Turpentine	59	0.074
Glycerol 100%	86	0.164	Vaseline	59	0.106
80%	68	0.189	Water	32	0.330
60%	68	0.220		86	0.356
40%	68	0.259		140	0.381
20%	68	0.278	Xylene (ortho-)	68	0.090
100%	212	0.164	(meta-)	68	0.090
Heptane (n-)	86	0.081			
	140	0.079			
Hexane (n-)	86	0.080			
	140	0.078			

* From Perry, J. H., "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.

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TABLE 5. THERMAL CONDUCTIVITIES OF GASES AND VAPORS*
 $k = \text{Btu}/(\text{hr})(\text{ft}^2)(^\circ\text{F}/\text{ft})$

The extreme temperature values given constitute the experimental range. For extrapolation to other temperatures, it is suggested that the data given be plotted as $\log k$ vs. $\log T$ or that use be made of the assumption that the ratio c_p/k is practically independent of temperature (or of pressure, within moderate limits).

Substance	°F	k	Substance	°F	k
Acetone	32	0.0057	Dichlorodifluoromethane	32	0.0048
	115	0.0074		122	0.0064
	212	0.0099		212	0.0080
	303	0.0147		302	0.0097
Acetylene	-103	0.0068	Ethane	-94	0.0066
	32	0.0108		-29	0.0086
	122	0.0140		32	0.0106
	212	0.0172		212	0.0175
Air	-148	0.0095	Ethyl acetate	115	0.0072
	32	0.0140		212	0.0096
	212	0.0183		363	0.0141
	392	0.0226	Alcohol	68	0.0089
	572	0.0265		212	0.0124
Ammonia	-76	0.0095	Chloride	32	0.0055
	32	0.0128		212	0.0095
	122	0.0157		363	0.0135
	212	0.0185	Ether	413	0.0152
				32	0.0077
Benzene	32	0.0052		115	0.0099
	115	0.0073		212	0.0131
	212	0.0103		363	0.0189
	363	0.0152	Ethylene	413	0.0209
	413	0.0176		-96	0.0064
Butane (n-)	32	0.0078		32	0.0101
(iso-)	212	0.0135		122	0.0131
	32	0.0080		212	0.0161
	212	0.0139	Heptane (n-)	392	0.0112
Carbon dioxide	-58	0.0068		212	0.0103
	32	0.0085	Hexane (n-)	32	0.0072
	212	0.0133		68	0.0080
	392	0.0181	Hexene	32	0.0061
	572	0.0228		212	0.0109
Disulphide	32	0.0040	Hydrogen	-148	0.065
	45	0.0042		-58	0.083
Monoxide	-312	0.0041		32	0.100
	-294	0.0046		122	0.115
	32	0.0135		212	0.129
Tetrachloride	115	0.0041		572	0.178
	212	0.0052	Hydrogen and carbon dioxide	32	
	363	0.0085	0% H ₂		0.0083
Chlorine	32	0.0043	20%		0.0165
Chloroform	32	0.0038	40%		0.0270
	115	0.0046	60%		0.0410
	212	0.0058	80%		0.0620
	363	0.0077	100%		0.10
Cyclohexane	216	0.0095			

PROCESS HEAT TRANSFER



TABLE 5. THERMAL CONDUCTIVITIES OF GASES AND VAPORS.*—(Continued)

Substance	°F	k	Substance	°F	k
Hydrogen and nitrogen.....	32		Nitric oxide.....	-94	0.0103
0% H ₂		0.0133	32	0.0138	
20%.....		0.0212	Nitrogen.....	-148	0.0095
40%.....		0.0313	32	0.0140	
60%.....		0.0438	122	0.0160	
80%.....		0.0635	212	0.0180	
Hydrogen and nitrous oxide.....	32		Nitrous oxide.....	-98	0.0067
0% H ₂		0.0002	32	0.0087	
20%.....		0.0170	212	0.0128	
40%.....		0.0270	Oxygen.....	-148	0.0095
60%.....		0.0410	-58	0.0119	
80%.....		0.0650	32	0.0142	
Hydrogen sulphide.....	32	0.0076	122	0.0164	
Mercury.....	392	0.0197	212	0.0185	
Methane.....	-148	0.0100			
	-58	0.0145	Pentane (n-).....	32	0.0074
	32	0.0175	68	0.0083	
	122	0.0215	(iso-).....	32	0.0072
Methyl alcohol.....	32	0.0083	212	0.0127	
	212	0.0128	Propane.....	32	0.0087
Acetate.....	32	0.0059	212	0.0151	
	68	0.0068			
Methyl chloride.....	32	0.0053	Sulphur dioxide.....	32	0.0050
	115	0.0072	212	0.0069	
	212	0.0094			
	363	0.0130	Water vapor.....	115	0.0120
	413	0.0148	212	0.0137	
Methylene chloride.....	32	0.0039	392	0.0187	
	115	0.0049	572	0.0248	
	212	0.0063	762	0.0315	
	413	0.0095	932	0.0441	

* From Perry, J. H., "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.

APPENDIX OF CALCULATION DATA

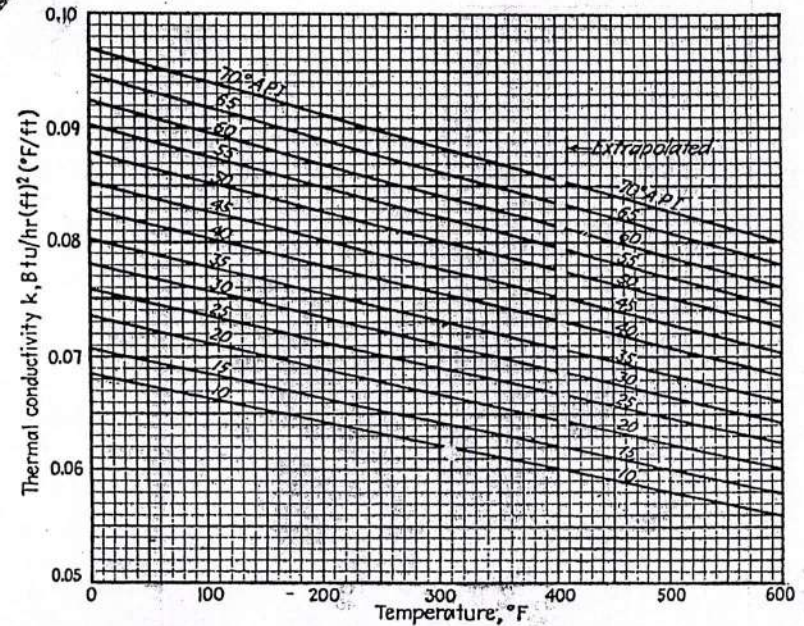


FIG. 1. Thermal conductivities of hydrocarbon liquids. (Adapted from Natl. Bur. Standards Misc. Pub. 97.)

115 - 0.0072
100 -

PROCESS HEAT TRANSFER

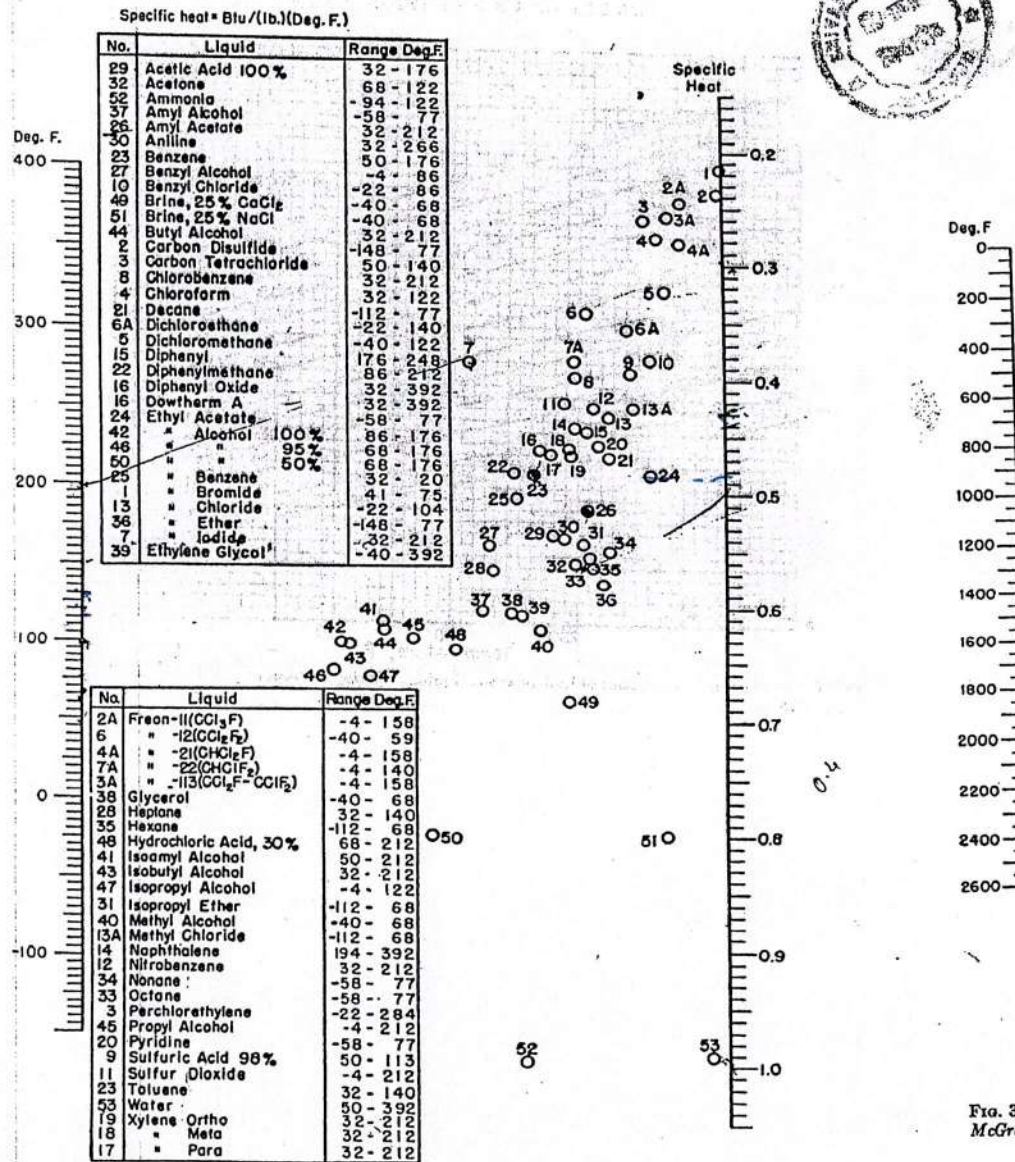


Fig. 2. Specific heats of liquids. (Chilton, Colburn, and Vernon, based mainly on data from International Critical Tables. Perry, "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.)

APPENDIX OF CALCULATION DATA

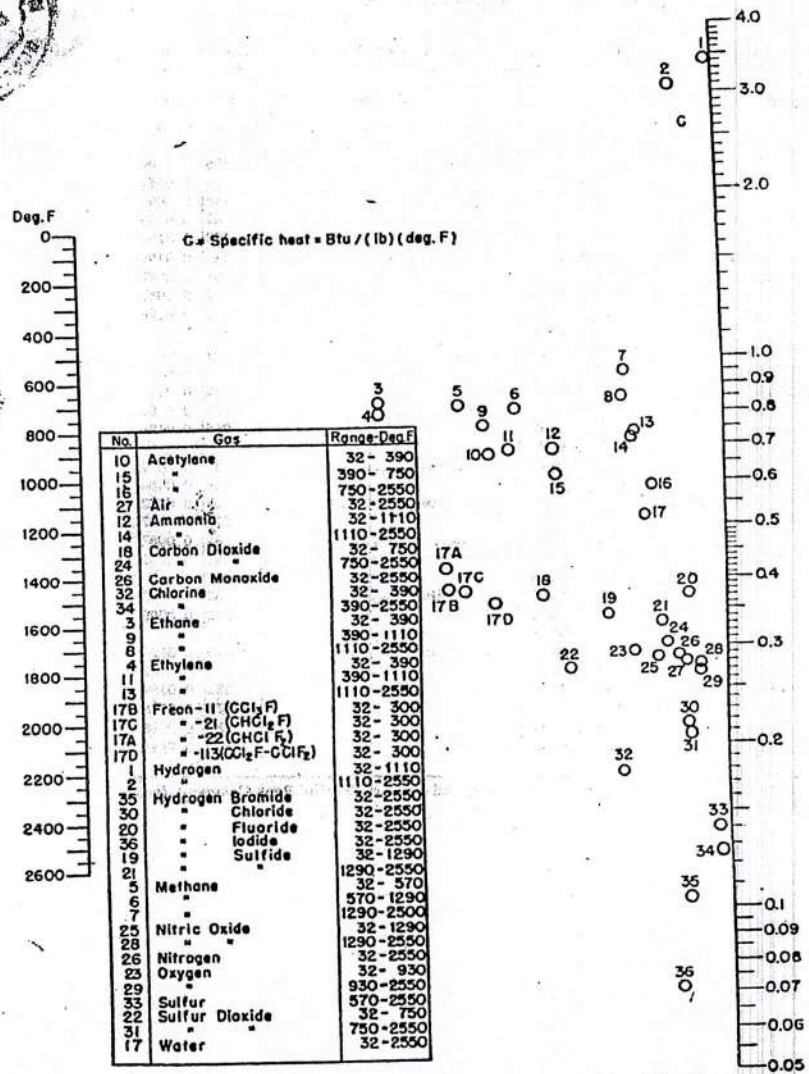


Fig. 3. Specific heats of gases at 1 atm. (Perry, "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.)

PROCESS HEAT TRANSFER

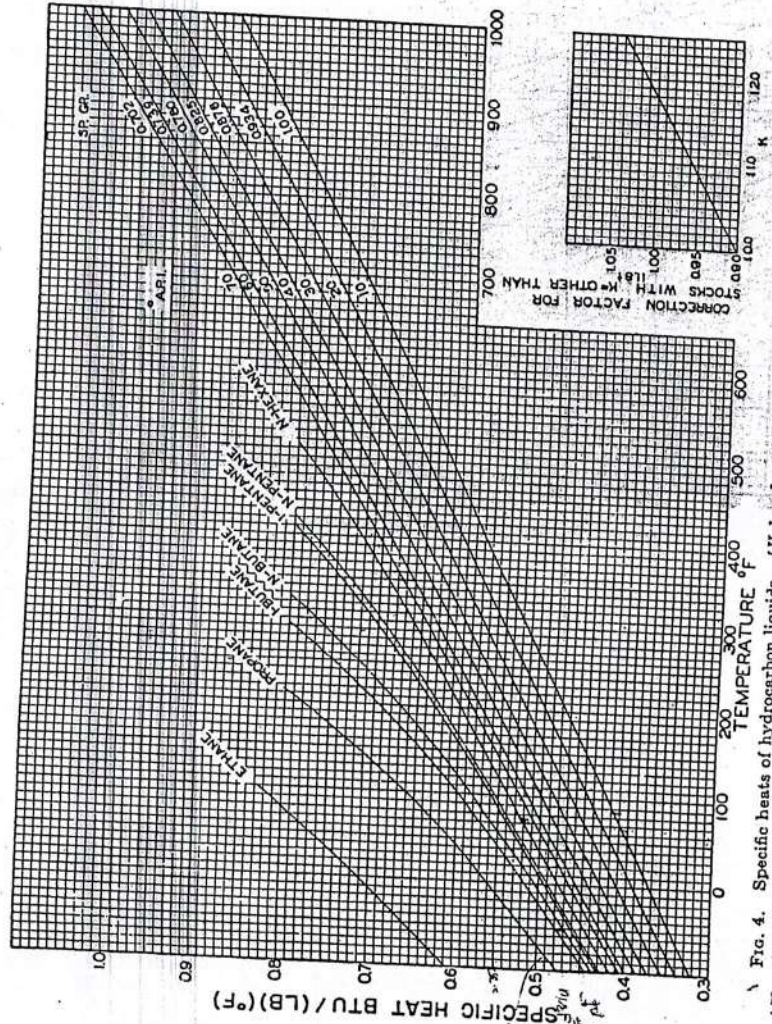


Fig. 4. Specific heats of hydrocarbon liquids. [Holcomb and Brown, Ind. Eng. Chem., 34, 595 (1942).]



APPENDIX OF CALCULATION DATA

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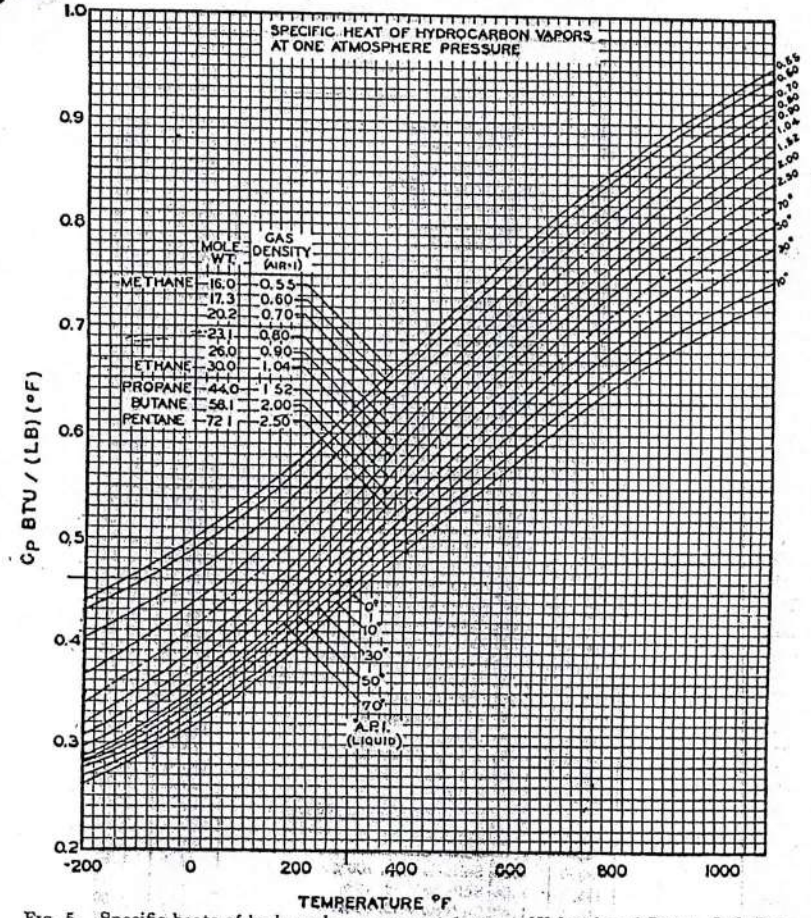


Fig. 5. Specific heats of hydrocarbon vapors at 1 atm. [Holcomb and Brown, Ind. Eng. Chem., 34, 595 (1942).]

PROCESS HEAT TRANSFER

TABLE 6. SPECIFIC GRAVITIES AND MOLECULAR WEIGHTS OF LIQUIDS



Compound	Mol. wt.	s*	Compound	Mol. wt.	s*
Acetaldehyde.....	44.1	0.78	Ethyl iodide.....	155.9	1.93
Acetic acid, 100 %	60.1	1.05	Ethyl glycol.....	88.1	1.04
Acetic acid, 70 %	1.07	Formic acid.....	46.0	1.22
Acetic anhydride.....	102.1	1.08	Glycerol, 100 %	92.1	1.26
Acetone.....	58.1	0.79	Glycerol, 50 %	1.13
Allyl alcohol.....	58.1	0.86	n-Heptane.....	100.2	0.68
Ammonia, 100 %	17.0	0.61	n-Hexane.....	86.1	0.66
Ammonia, 26 %	0.91	Isopropyl alcohol.....	60.1	0.79
Amyl acetate.....	130.2	0.88	Mercury.....	200.6	13.55
Amyl alcohol.....	88.2	0.81	Methanol, 100 %	32.5	0.79
Aniline.....	93.1	1.02	Methanol, 90 %	0.82
Anisole.....	108.1	0.99	Methanol, 40 %	0.94
Arsenic trichloride.....	181.3	2.16	Methyl acetate.....	74.9	0.93
Benzene.....	78.1	0.88	Methyl chloride.....	50.5	0.92
Brine, CaCl ₂ 25 %	1.23	Methyl ethyl ketone.....	72.1	0.81
Brine, NaCl 25 %	1.19	Naphthalene.....	128.1	1.14
Bromotoluene, ortho.....	171.0	1.42	Nitric acid, 95 %	1.50
Bromotoluene, meta.....	171.0	1.41	Nitric acid, 60 %	1.38
Bromotoluene, para.....	171.0	1.39	Nitrobenzene.....	123.1	1.20
n-Butane.....	58.1	0.60	Nitrotoluene, ortho.....	137.1	1.16
i-Butane.....	58.1	0.60	Nitrotoluene, meta.....	137.1	1.16
Butyl acetate.....	116.2	0.88	Nitrotoluene, para.....	137.1	1.29
n-Butyl alcohol.....	74.1	0.81	n-Octane.....	114.2	0.70
i-Butyl alcohol.....	74.1	0.82	Octyl alcohol.....	130.23	0.82
n-Butyric acid.....	88.1	0.96	Pentachloroethane.....	202.3	1.67
i-Butyric acid.....	88.1	0.96	n-Pentane.....	72.1	0.63
Carbon dioxide.....	44.0	1.29	Phenol.....	94.1	1.07
Carbon disulfide.....	76.1	1.26	Phosphorus tribromide.....	270.8	2.85
Carbon tetrachloride.....	153.8	1.60	Phosphorus trichloride.....	137.4	1.57
Chlorobenzene.....	112.6	1.11	Propane.....	44.1	0.69
Chloroform.....	119.4	1.49	Propionic acid.....	74.1	0.99
Chlorosulfonic acid.....	116.5	1.77	n-Propyl alcohol.....	60.1	0.80
Chlorotoluene, ortho.....	126.6	1.08	n-Propyl bromide.....	123.0	1.35
Chlorotoluene, meta.....	126.6	1.07	n-Propyl chloride.....	78.5	0.89
Chlorotoluene, para.....	126.6	1.07	n-Propyl iodide.....	170.0	1.75
Cresol, meta.....	108.1	1.03	Sodium.....	23.0	0.97
Cyclohexanol.....	100.2	0.96	Sodium hydroxide, 50 %	1.53
Dibromo methane.....	187.9	2.09	Stannic chloride.....	260.5	2.23
Dichloro ethane.....	99.0	1.17	Sulfur dioxide.....	64.1	1.38
Dichloro methane.....	88.9	1.34	Sulfuric acid, 100 %	98.1	1.83
Diethyl oxalate.....	146.1	1.08	Sulfuric acid, 98 %	1.84
Dimethyl oxalate.....	118.1	1.42	Sulfuric acid, 60 %	1.50
Diphenyl.....	154.2	0.99	Sulfuryl chloride.....	135.0	1.67
Dipropyl oxalate.....	174.1	1.02	Tetra chloroethane.....	167.9	1.60
Ethyl acetate.....	88.1	0.90	Tetra chloroethylene.....	165.9	1.63
Ethyl alcohol, 100 %	46.1	0.79	Titanium tetrachloride.....	189.7	1.73
Ethyl alcohol, 95 %	0.81	Toluene.....	92.1	0.87
Ethyl alcohol, 40 %	0.94	Trichloroethylene.....	131.4	1.46
Ethyl benzene.....	106.1	0.87	Vinyl acetate.....	86.1	0.93
Ethyl bromide.....	108.9	1.43	Water.....	18.0	1.0
Ethyl chloride.....	84.5	0.92	Xylene, ortho.....	106.1	0.87
Ethyl ether.....	74.1	0.71	Xylene, meta.....	106.1	0.86
Ethyl formate.....	74.1	0.92	Xylene, para.....	106.1	0.88

APPENDIX OF CALCULATION DATA

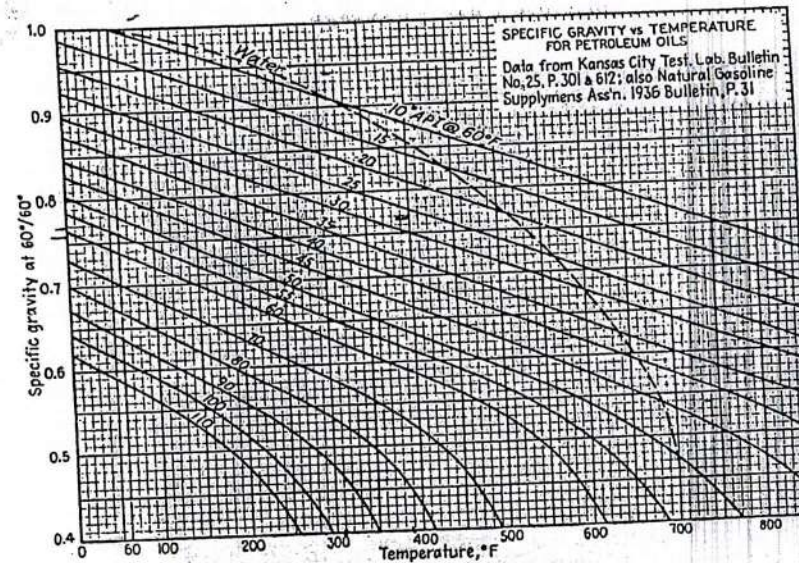


FIG. 6. Specific gravities of hydrocarbons.

* At approximately 68°F. These values will be satisfactory, without extrapolation, for most engineering problems.

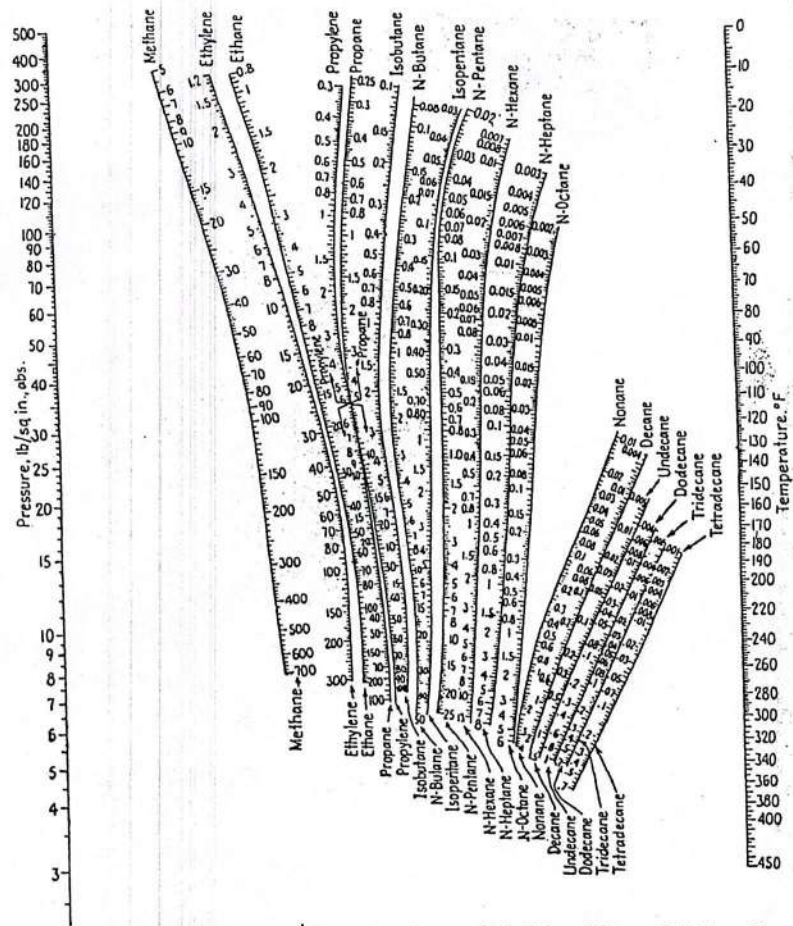


Fig. 7. Equilibrium constants for hydrocarbons. [Scheibel and Jenny, *Ind. Eng. Chem.*, 37, 81 (1945).]

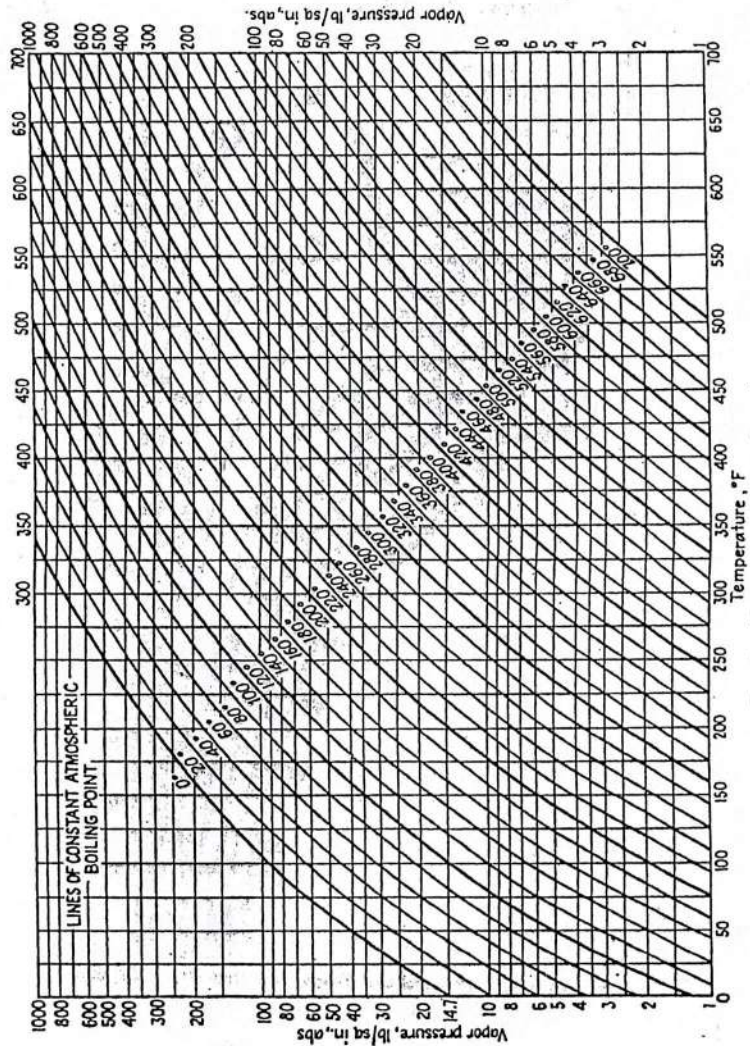


Fig. 8. Vapor pressures of hydrocarbons.

PROCESS HEAT TRANSFER

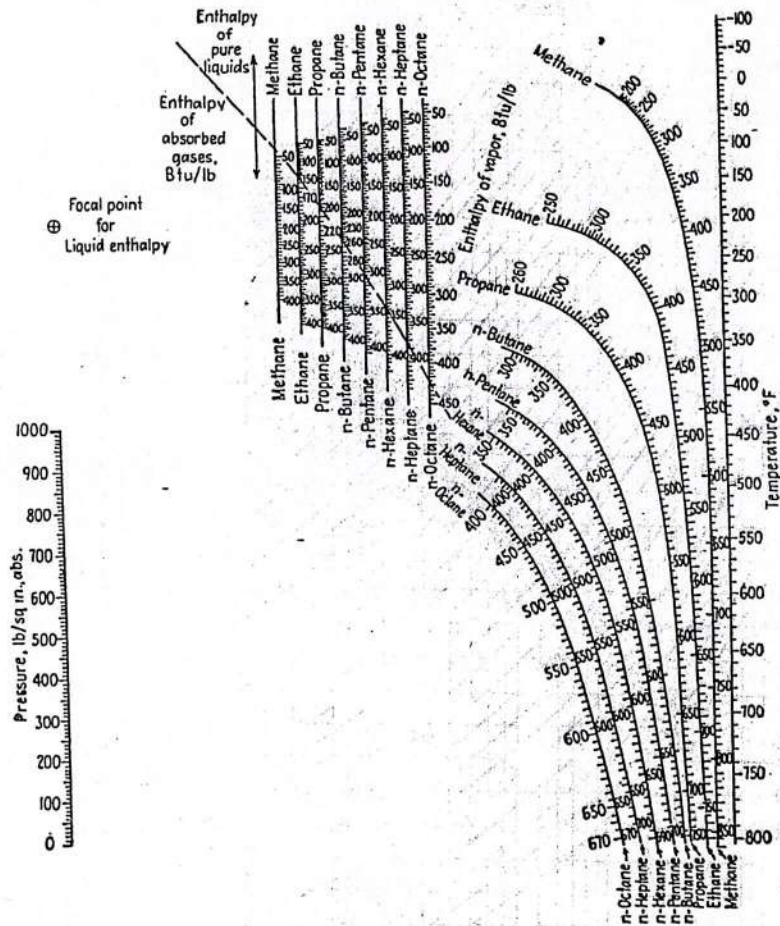


FIG. 9. Enthalpies of pure hydrocarbons. [Scheibel and Jenny, *Ind. Eng. Chem.*, **37**, 992 (1945).]

APPENDIX OF CALCULATION DATA

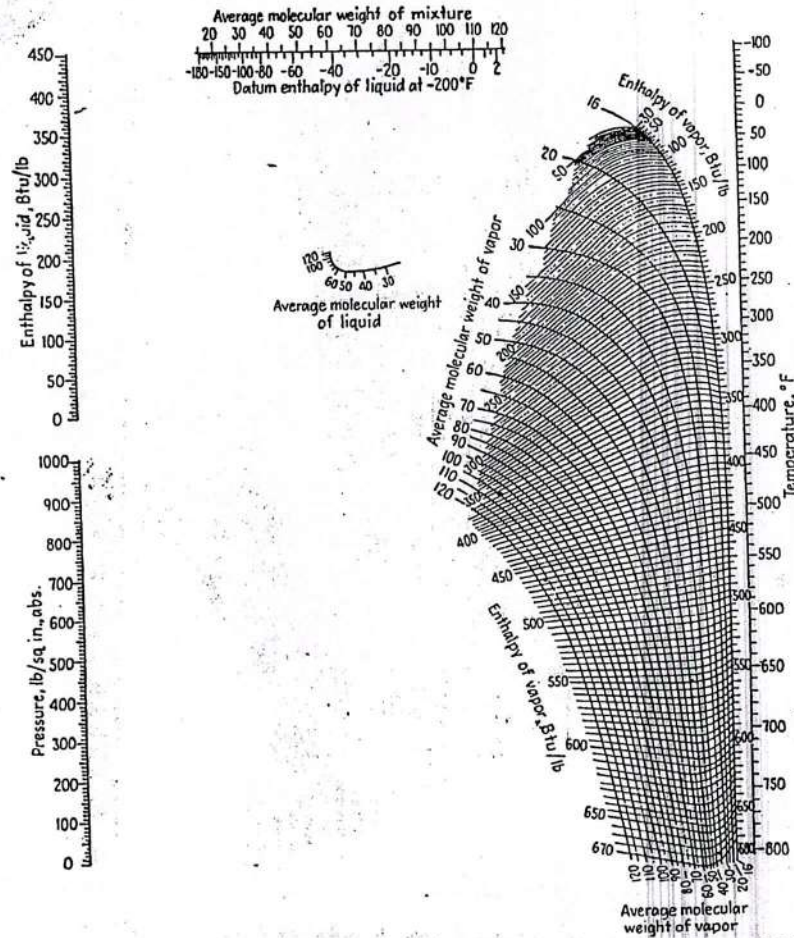


FIG. 10. Enthalpies of light hydrocarbons. [Scheibel and Jenny, *Ind. Eng. Chem.*, **37**, 993 (1945).]

PROCESS HEAT TRANSFER

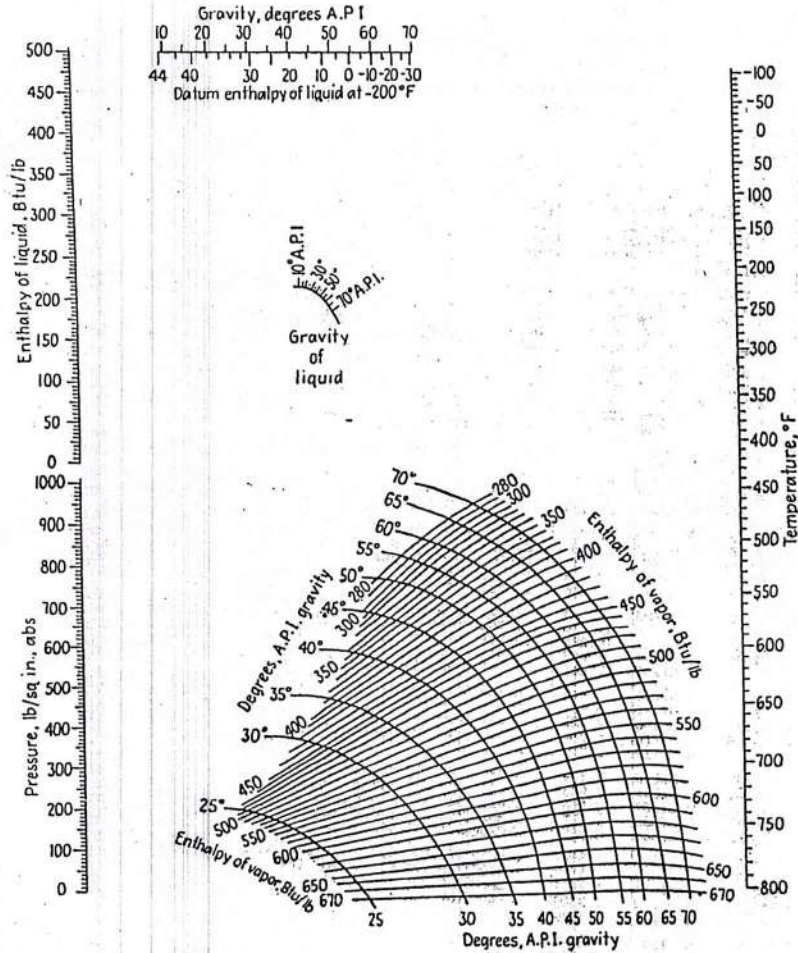


FIG. 11. Enthalpies of petroleum fractions. [Scheibel and Jenny, *Ind. Eng. Chem.*, 37, 994 (1945).]



APPENDIX OF CALCULATION DATA

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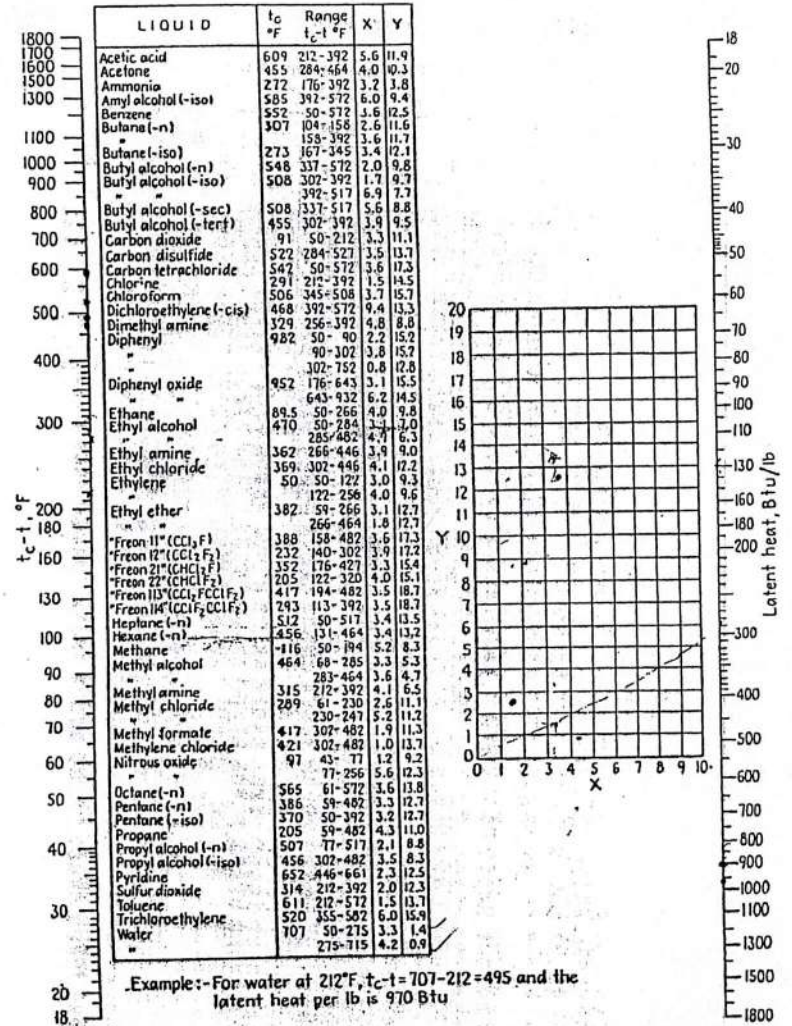


FIG. 12. Latent heats of vaporisation. [Reproduced by permission of Chilton, Colburn, and Vernon, personal communication (revised) 1947.]

PROCESS HEAT TRANSFER

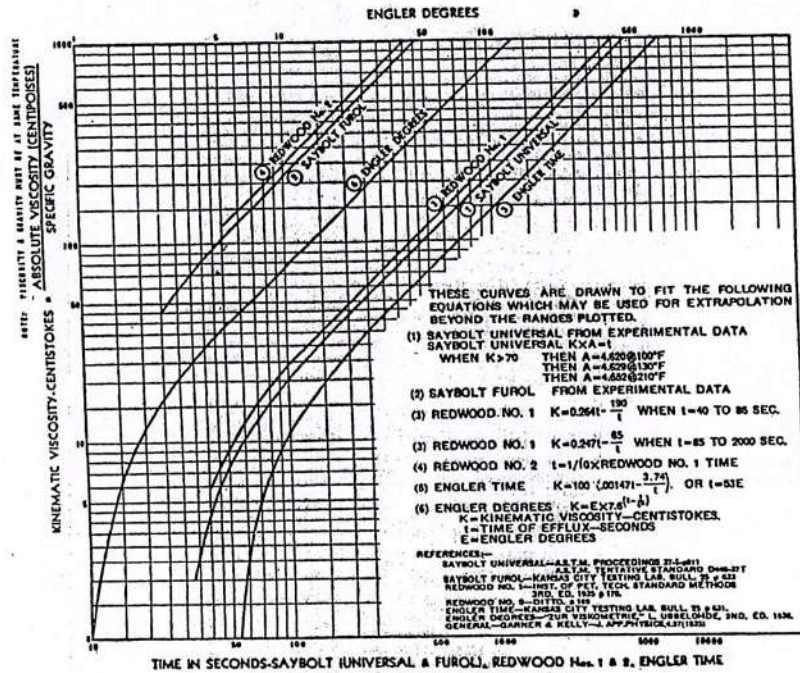


Fig. 13a. Viscosity conversion chart.

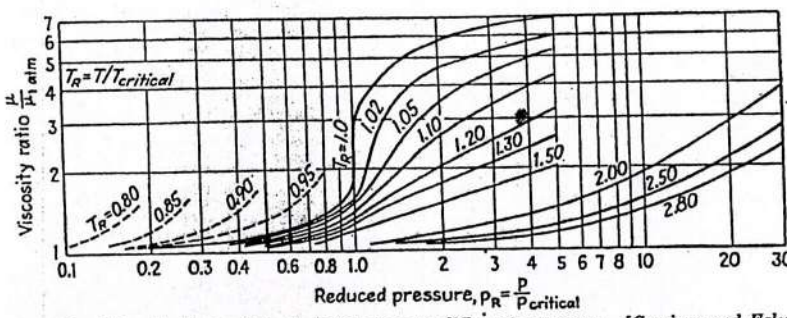


Fig. 13b. Viscosity correction chart for gases at different pressures. [Comings and Egly, Ind. Eng. Chem., 32, 715 (1940).]



APPENDIX OF CALCULATION DATA

VISCOSITIES OF PETROLEUM FRACTIONS
 For temperature ranges employed in the text
 Coordinates to be used with Fig. 14

	X	Y
76°API natural gasoline.....	14.4	6.4
56°API gasoline.....	14.0	10.5
42°API kerosene.....	11.6	16.0
35°API distillate.....	10.0	20.0
34°API mid-continent crude.....	10.3	21.3
28°API gas oil.....	10.0	23.6

VISCOSITIES OF ANIMAL AND VEGETABLE OILS*

	Acid No.	Sp gr, 20/4°C	X	Y
Almond.....	2.85	0.9188	6.9	28.2
Coconut.....	0.01	0.9226	6.9	26.9
Cod liver.....		0.9138	7.7	27.7
Cottonseed.....	14.24	0.9187	7.0	28.0
Lard.....	3.39	0.9138	7.0	28.2
Linseed.....	3.42	0.9297	6.8	27.5
Mustard.....		0.9237	7.0	28.5
Neatsfoot.....	13.35	0.9158	6.5	28.0
Olive.....		0.9158	6.6	28.3
Palm kernel.....	9.0	0.9190	7.0	26.9
Perilla, raw.....	1.36	0.9297	8.1	27.2
Rapeseed.....	0.34	0.9114	7.0	28.8
Sardine.....	0.57	0.9384	7.7	27.3
Soybean.....	3.50	0.9228	8.3	27.5
Sperm.....	0.80	0.8829	7.7	26.3
Sunflower.....	2.76	0.9207	7.5	27.6
Whale, refined.....	0.73	0.9227	7.5	27.5

* Based on data at 100 and 210°F of A. R. Rescorla and F. L. Carnahan, Ind. Eng. Chem., 28, 1212 (1936).

VISCOSITIES OF COMMERCIAL FATTY ACIDS*
 250 to 400°F

	Sp gr at 300°F	X	Y
Lauric.....	0.792	10.1	23.1
Oleic.....	0.799	10.0	25.2
Palmitic.....	0.786	9.2	25.9
Stearic.....	0.789	10.5	25.5

* From data of D. Q. Kern and W. Van Nostrand, Ind. Eng. Chem., 41, 2209 (1940).

PROCESS HEAT TRANSFER



VISCOSITIES OF LIQUIDS*
Coordinates to be used with Fig. 14.

APPENDIX OF CALCULATION DATA

Liquid	X	Y	Liquid	X	Y
Acetaldehyde	15.2	4.8	Freon-21	15.7	7.5
Acetic acid, 100%	12.1	14.2	Freon-22	17.2	4.7
Acetic acid, 70%	9.5	17.0	Freon-113	12.5	11.4
Acetic anhydride	12.7	12.8	Freon-114	14.6	8.3
Acetone, 100%	14.5	7.2	Glycerol, 100%	2.0	30.0
Acetone, 35%	7.9	15.0	Glycerol, 50%	6.9	19.6
Allyl alcohol	10.2	14.3	Heptane	14.1	8.4
Ammonia, 100%	12.6	2.0	Hexane	14.7	7.0
Ammonia, 26%	10.1	13.9	Hydrochloric acid, 31.5%	13.0	16.6
Amyl acetate	11.8	12.5	Isobutyl alcohol	7.1	18.0
Amyl alcohol	7.5	18.4	Isobutyric acid	12.2	14.4
Aniline	8.1	18.7	Isopropyl alcohol	8.2	16.0
Anisole	12.3	13.5	Mercury	18.4	16.4
Arsenic trichloride	13.9	14.5	Methanol, 100%	12.4	10.5
Benzene	12.5	10.9	Methanol, 90%	12.3	11.8
Brine, CaCl ₂ , 25%	6.6	15.9	Methanol, 40%	7.8	15.5
Brine, NaCl, 25%	10.2	16.6	Methyl acetate	14.2	8.2
Bromine	14.2	13.2	Methyl chloride	15.0	3.8
Bromotoluene	20.0	15.9	Methyl ethyl ketone	13.9	8.6
n-Butane	15.3	3.3	Naphthalene	7.9	18.1
Isobutane	14.5	3.7	Nitric acid, 95%	12.8	13.8
Butyl acetate	12.3	11.0	Nitric acid, 60%	10.8	17.0
Butyl alcohol	8.6	17.2	Nitrobenzene	10.6	16.2
Butyric acid	12.1	15.3	Nitrotoluene	11.0	17.0
Carbon dioxide	11.6	0.3	Octane	13.7	10.0
Carbon disulfide	16.1	7.5	Octyl alcohol	6.6	21.1
Carbon tetrachloride	12.7	13.1	Pentachloroethane	10.9	17.3
Chlorobenzene	12.3	12.4	Pentane	14.9	5.2
Chloroform	14.4	10.2	Phenol	6.9	20.8
Chlorosulfonic acid	11.2	18.1	Phosphorus tribromide	13.8	16.7
Chlorotoluene, ortho	13.0	13.3	Phosphorus trichloride	16.2	10.9
Chlorotoluene, meta	13.3	12.5	Propane	15.3	1.0
Chlorotoluene, para	13.3	12.5	Propionic acid	12.8	13.8
Cresol, meta	2.5	20.8	Propyl alcohol	9.1	16.5
Cyclohexanol	2.9	24.3	Propyl bromide	14.5	9.6
Dibromoethane	12.7	15.8	Propyl chloride	14.4	7.5
Dichloroethane	13.2	12.2	Propyl iodide	14.1	11.6
Dichloromethane	14.6	8.9	Sodium	16.4	13.9
Diethyl oxalate	11.0	16.4	Sodium hydroxide, 50%	3.2	25.8
Dimethyl oxalate	12.3	15.8	Stannic chloride	13.5	12.8
Diphenyl	12.0	18.3	Sulfur dioxide	15.2	7.1
Dipropyl oxalate	10.3	17.7	Sulfuric acid, 110%	7.2	27.4
Ethyl acetate	13.7	9.1	Sulfuric acid, 98%	7.0	24.8
Ethyl alcohol, 100%	10.5	13.8	Sulfuric acid, 60%	10.2	21.3
Ethyl alcohol, 95%	9.8	14.3	Sulfuryl chloride	15.2	12.4
Ethyl alcohol, 40%	6.5	16.6	Tetrachloroethane	11.9	15.7
Ethyl benzene	13.2	11.5	Tetrachloroethylene	14.2	12.7
Ethyl bromide	14.5	8.1	Titanium tetrachloride	14.4	12.3
Ethyl chloride	14.8	6.0	Toluene	13.7	10.4
Ethyl ether	14.5	5.3	Trichloroethylene	14.8	10.5
Ethyl formate	14.2	8.4	Turpentine	11.5	14.9
Ethyl iodide	14.7	10.3	Vinyl acetate	14.0	8.8
Ethylene glycol	6.0	23.6	Water	10.2	13.0
Formic acid	10.7	15.8	Xylene, ortho	13.5	12.1
Freon-11	14.4	9.0	Xylene, meta	13.9	10.6
Freon-12	16.8	5.6	Xylene, para	13.9	10.9

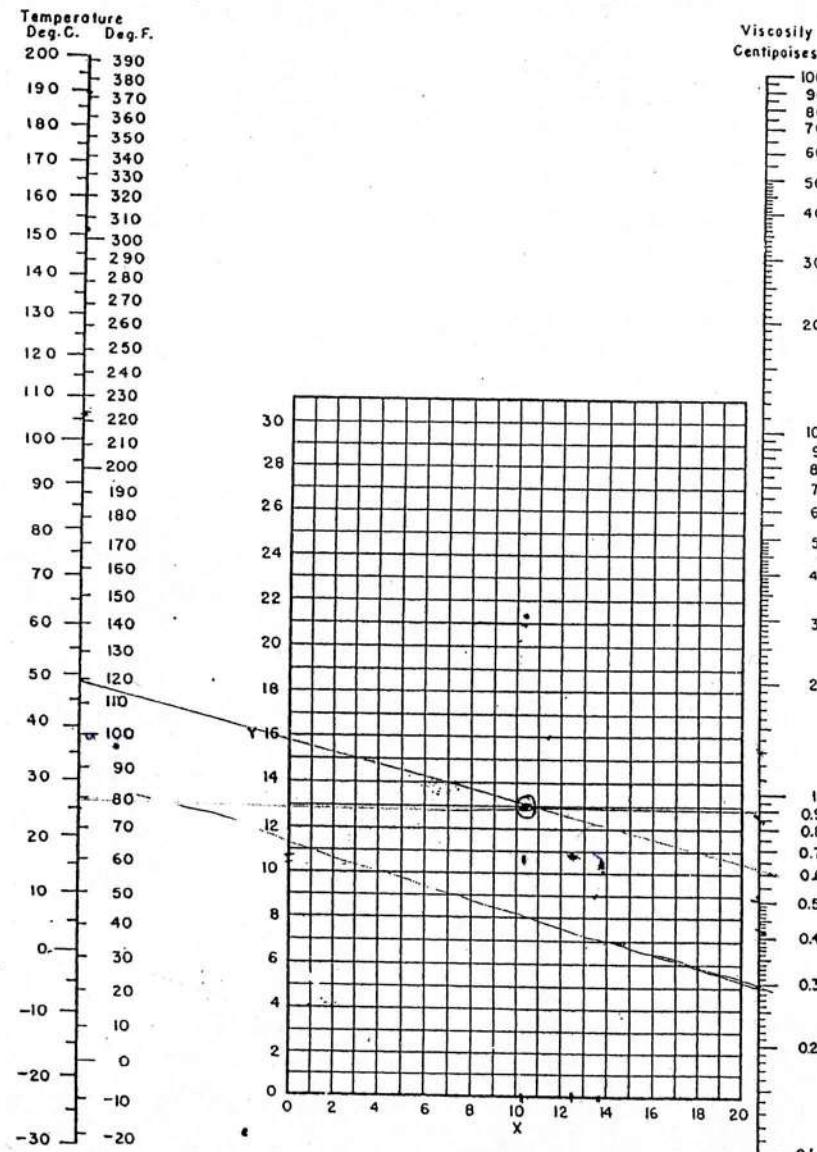


Fig. 14. Viscosities of liquids. (Perry, "Chemical Engineers' Handbook," 3d ed., McGraw Hill Book Company, Inc., New York, 1950.)

* From Perry, J. H., "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.



PROCESS HEAT TRANSFER

VISCOSITIES OF GASES*
Coordinates to be used with Fig. 15

Gas	X	Y
Acetic acid	7.7	14.3
Acetone	8.9	13.0
Acetylene	9.8	14.0
Air	11.0	20.0
Ammonia	8.4	16.0
Argon	10.5	22.4
Benzene	8.5	13.2
Bromine	8.9	19.2
Butene	9.2	13.7
Butylene	8.9	13.0
Carbon dioxide	9.5	18.7
Carbon disulfide	8.0	16.0
Carbon monoxide	11.0	20.0
Chlorine	9.0	18.4
Chloroform	8.9	15.7
Cyanogen	9.2	15.2
Cyclohexane	9.2	12.0
Ethane	9.1	14.5
Ethyl acetate	8.5	13.2
Ethyl alcohol	9.2	14.2
Ethyl chloride	8.5	15.6
Ethyl ether	8.9	13.0
Ethylene	9.5	15.1
Fluorine	7.3	23.8
Freon-11	10.6	15.1
Freon-12	11.1	16.0
Freon-21	10.8	15.3
Freon-22	10.1	17.0
Freon-113	11.3	14.0
Helium	10.9	20.5
Hexane	8.6	11.8
Hydrogen	11.2	12.4
3H ₂ + 1N ₂	11.2	17.2
Hydrogen bromide	8.8	20.9
Hydrogen chloride	8.8	18.7
Hydrogen cyanide	9.8	14.9
Hydrogen iodide	9.0	21.3
Hydrogen sulfide	8.6	18.0
Iodine	9.0	18.4
Mercury	5.3	22.9
Methane	9.9	15.5
Methyl alcohol	8.5	15.6
Nitric oxide	10.9	20.5
Nitrogen	10.6	20.0
Nitrosyl chloride	8.0	17.6
Nitrous oxide	8.8	19.0
Oxygen	11.0	21.3
Pentane	7.0	12.8
Propane	9.7	12.9
Propyl alcohol	8.4	13.4
Propylene	9.0	13.8
Sulfur dioxide	9.6	17.0
Toluene	8.6	12.4
2, 3, 3-Trimethylbutane	9.5	10.5
Water	8.0	16.0
Xenon	9.3	23.0

APPENDIX OF CALCULATION DATA

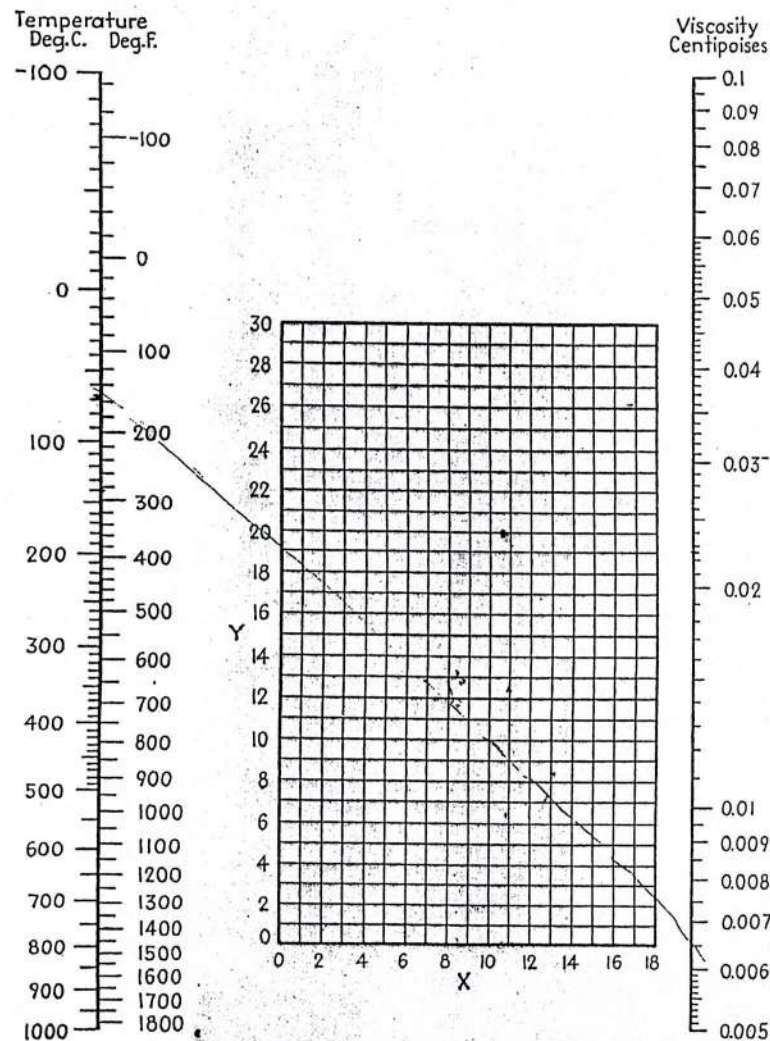


FIG. 15. Viscosities of gases. (Perry, "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.)

* From Perry, J. H., "Chemical Engineers' Handbook," 3d ed., McGraw-Hill Book Company, Inc., New York, 1950.

PROCESS HEAT TRANSFER

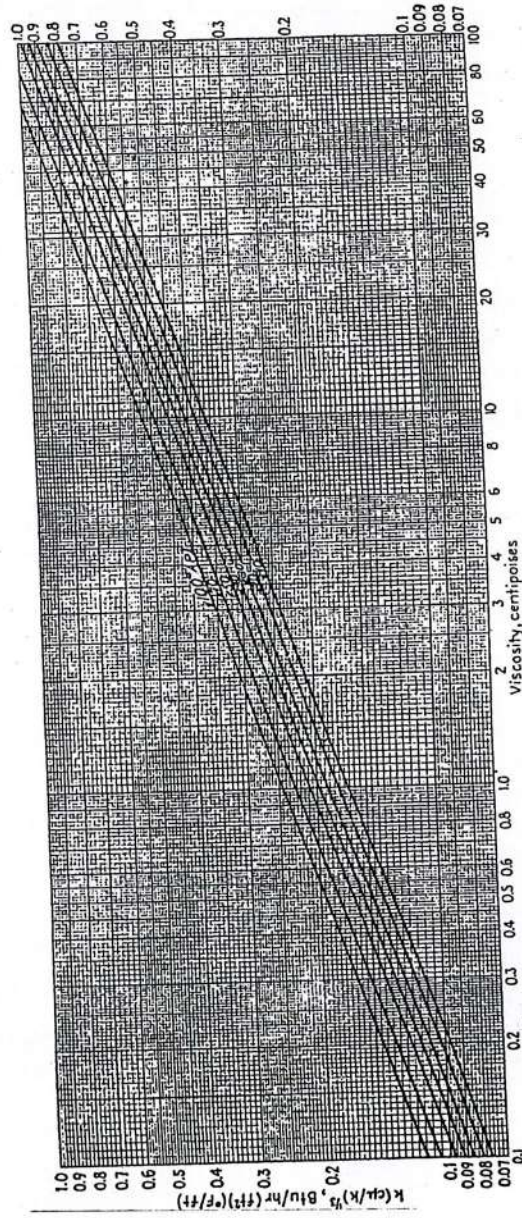


Fig. 16. Values of k (cp/k) for hydrocarbons.



APPENDIX OF CALCULATION DATA

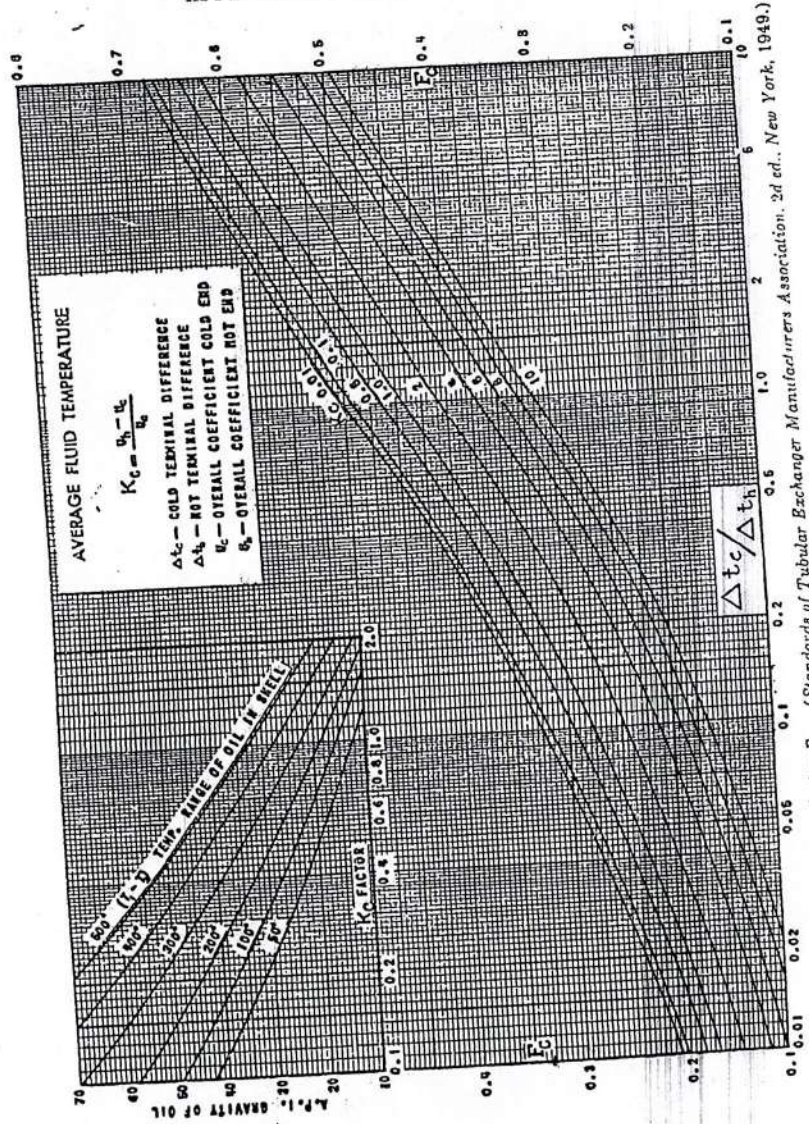


Fig. 17. The caloric temperature factor F_c . (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)

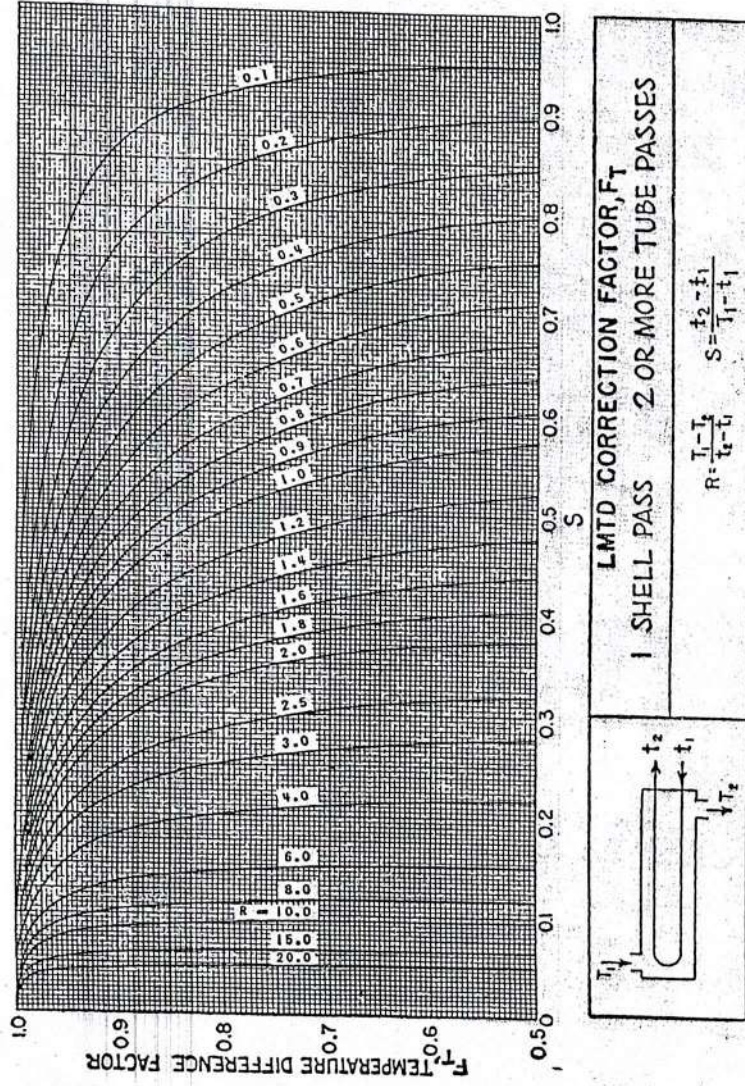


FIG. 18. LMTD correction factors for 1-2 exchangers. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1946.)

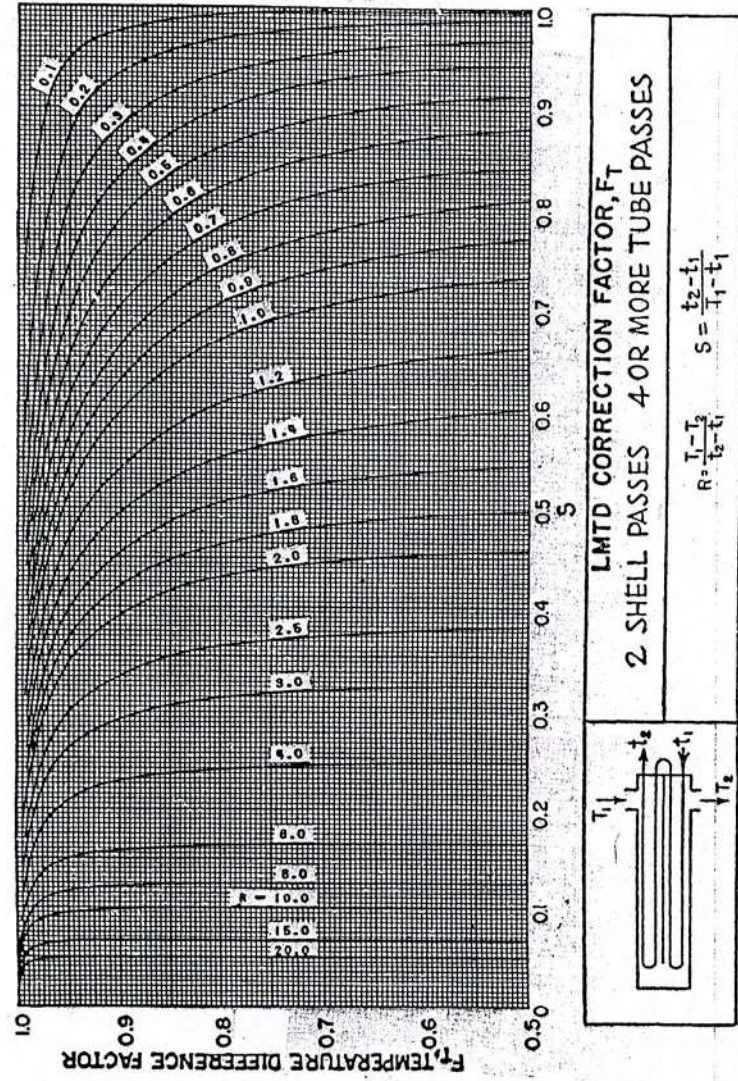


FIG. 19. LMTD correction factors for 2-4 exchangers. (Standards of Tubular Exchanger Manufacturers Association 2d ed., New York, 1946.)

PROCESS HEAT TRANSFER

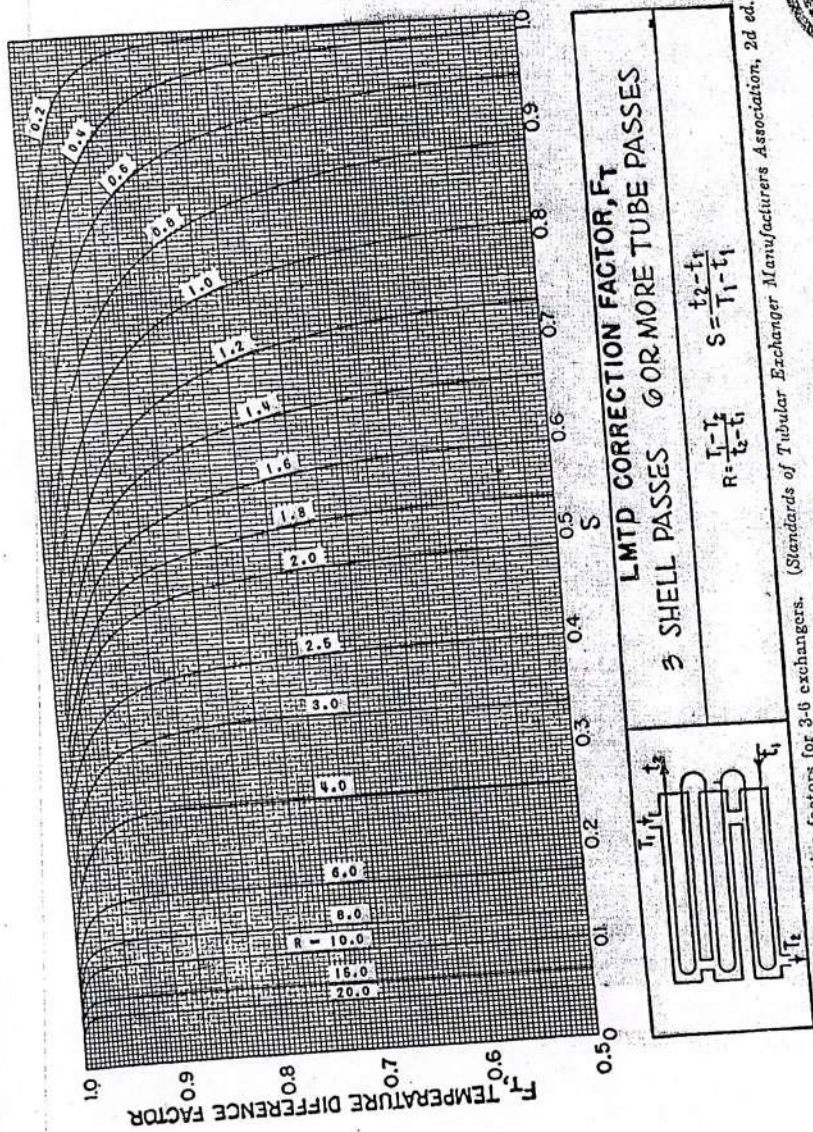


Fig. 20. LMTD correction factors for 3-6 exchangers. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)

APPENDIX OF CALCULATION DATA

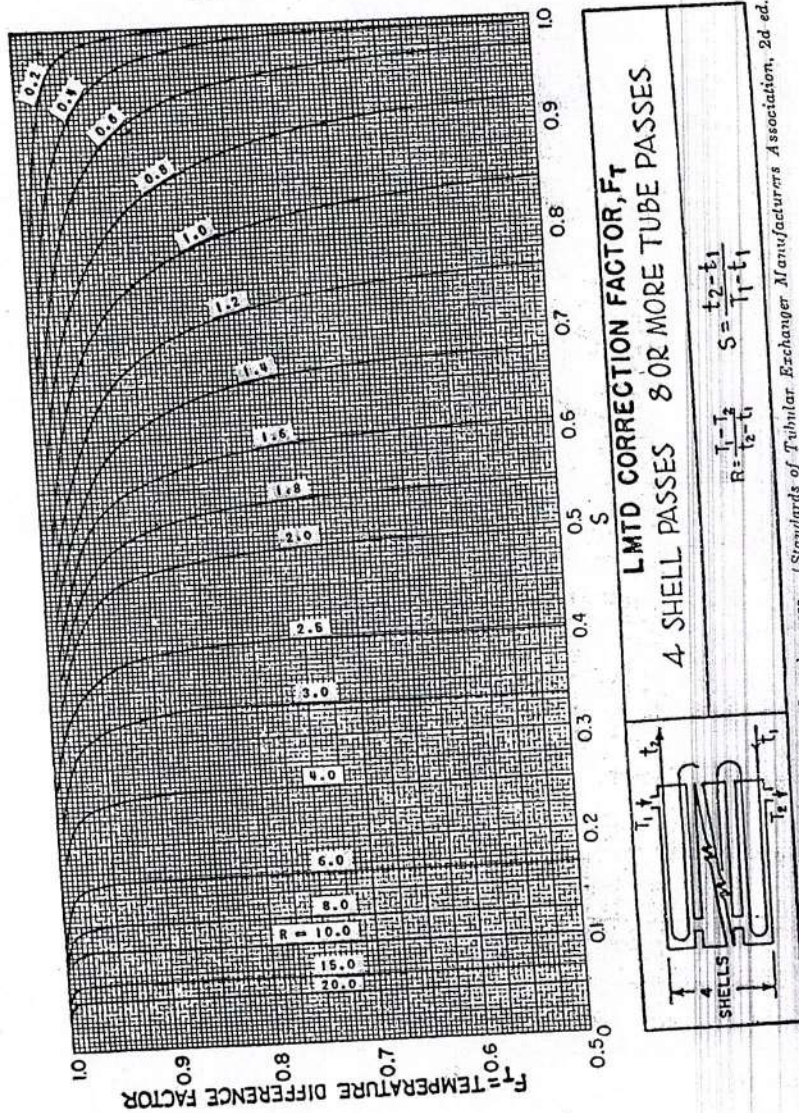
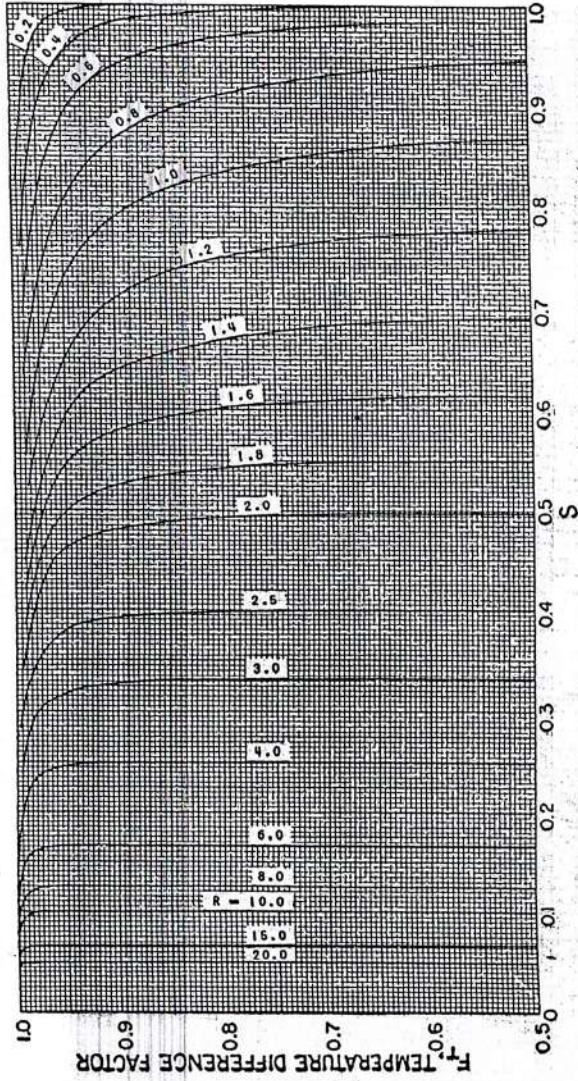



Fig. 21. LMTD correction factors for 4-8 exchangers. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)



LMTD CORRECTION FACTOR, F_T

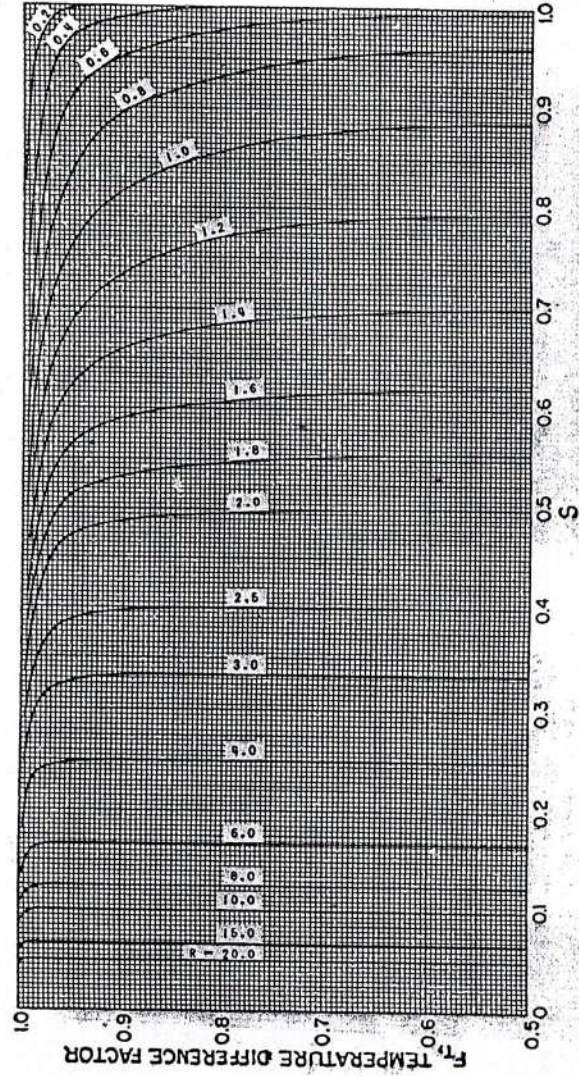
5 SHELL PASSES 10 OR MORE TUBE PASSES



$$R = \frac{T_1 - T_2}{t_2 - t_1}$$


$$S = \frac{t_2 - t_1}{T_1 - t_1}$$

FIG. 22. LMTD correction factors for 5-10 exchangers. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)



LMTD CORRECTION FACTOR, F_T

6 SHELL PASSES 12 OR MORE TUBE PASSES



$$R = \frac{T_1 - T_2}{t_2 - t_1}$$

$$S = \frac{t_2 - t_1}{T_1 - t_1}$$

FIG. 23. LMTD correction factors for 6-12 exchangers. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)

PROCESS HEAT TRANSFER

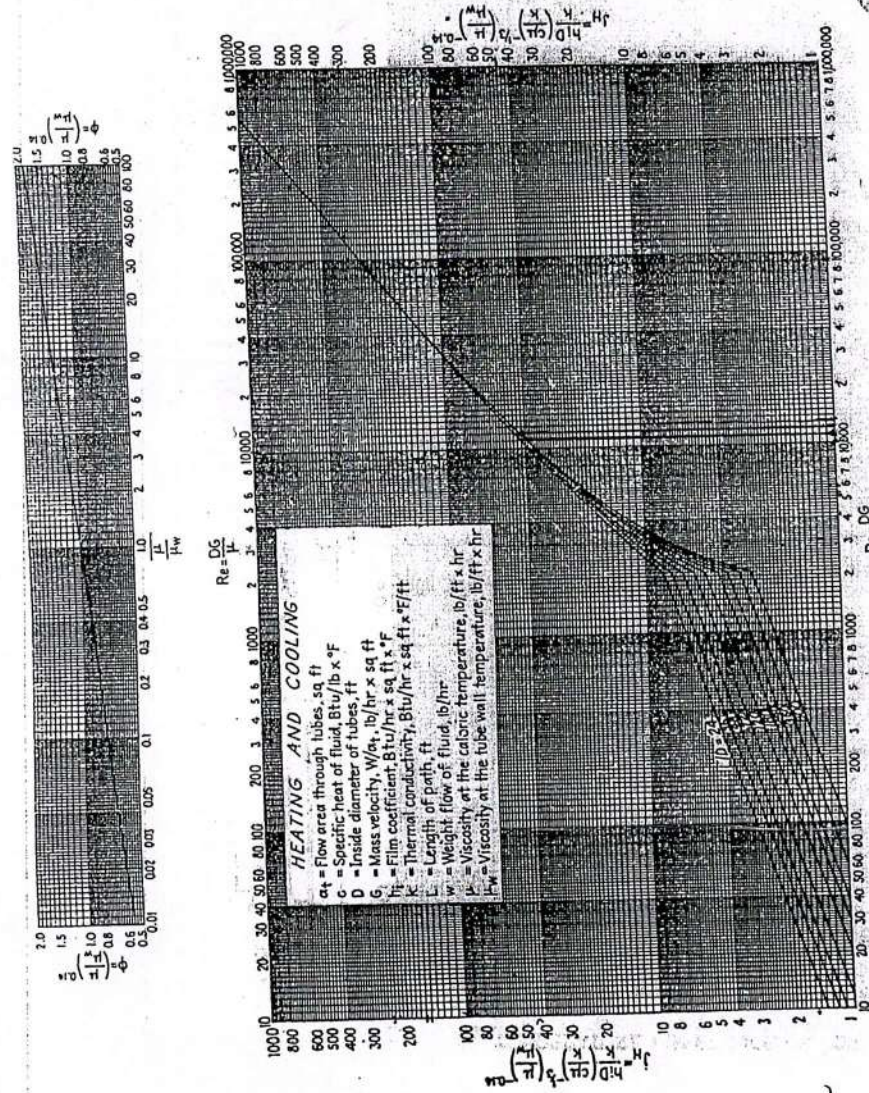


Fig. 24. Tube-side heat-transfer curve. (Adapted from Sieder and Tate.)

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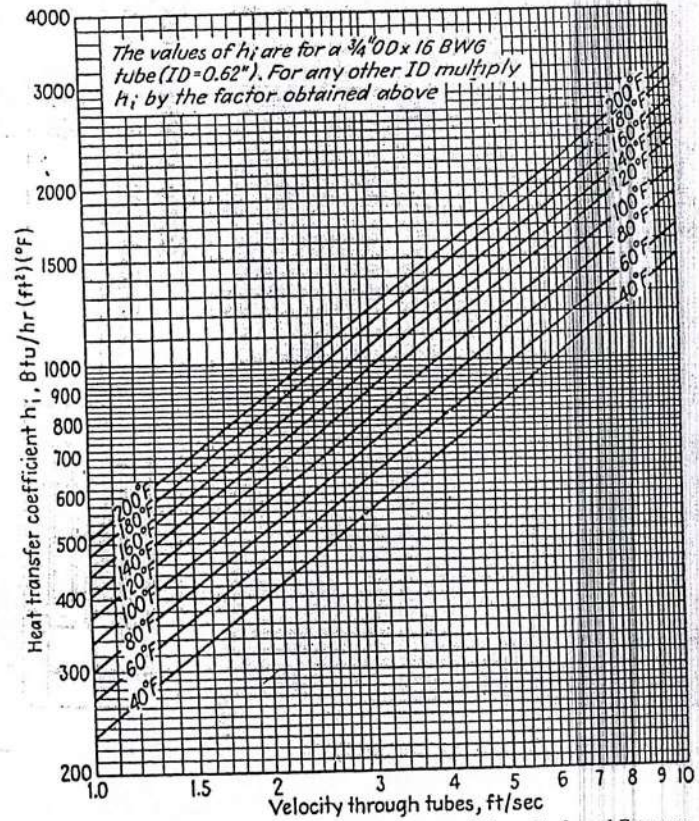
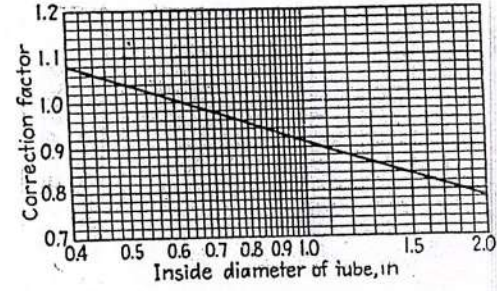


Fig. 25. Tube-side water-heat-transfer curve. [Adapted from Eagle and Ferguson, Proc. Roy. Soc., A127, 640 (1930).]

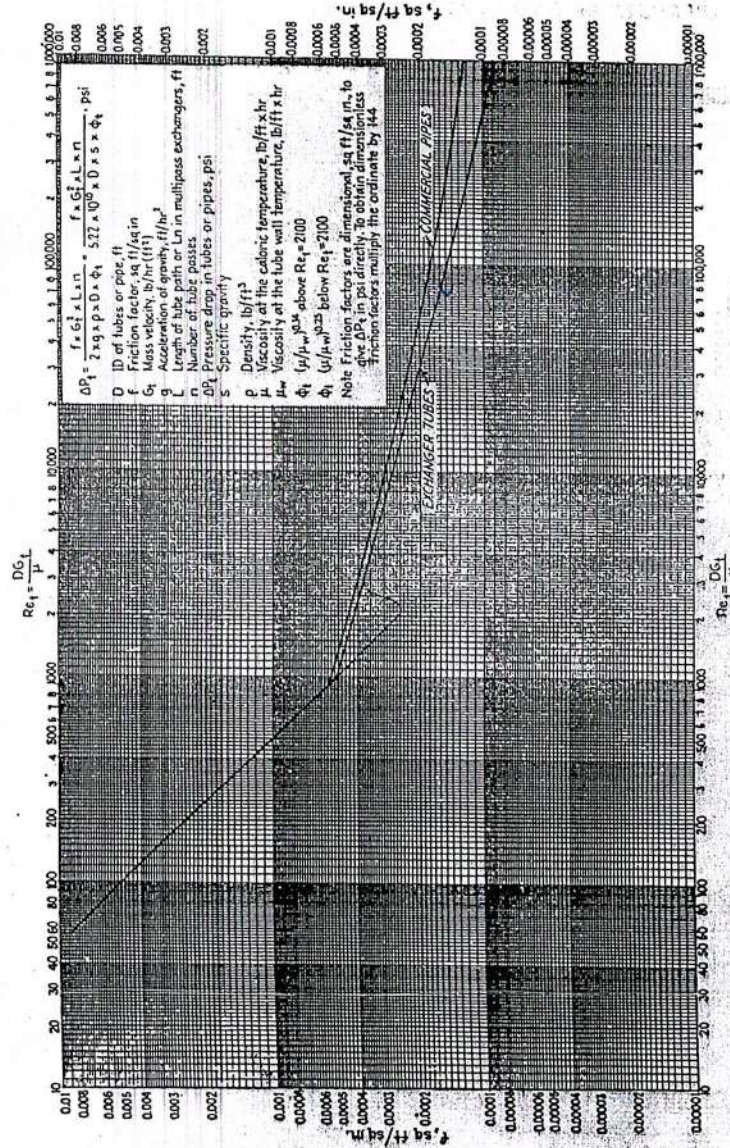


Fig. 26. Tube-side friction factors. (Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.)

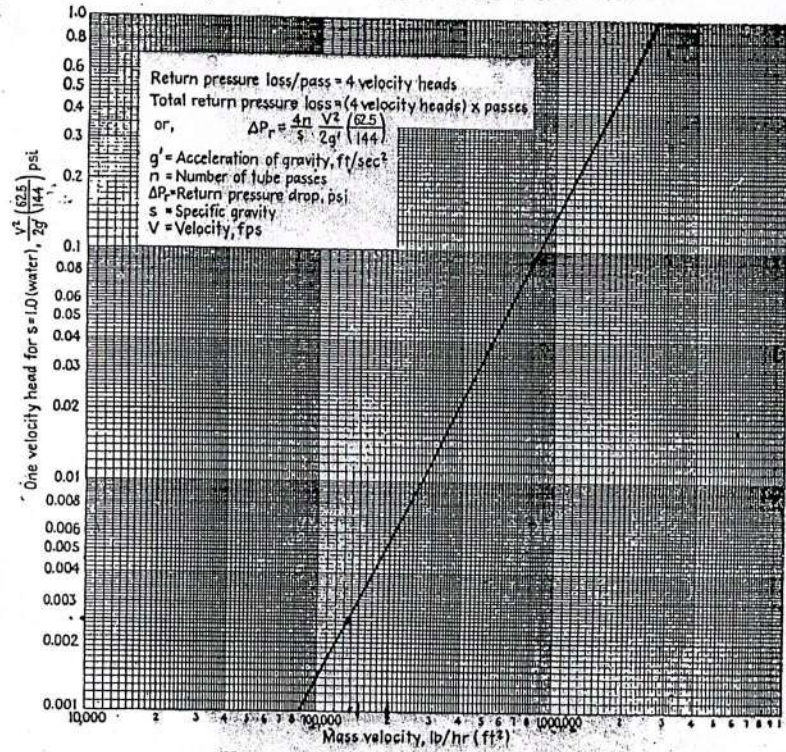


Fig. 27. Tube-side return pressure loss.

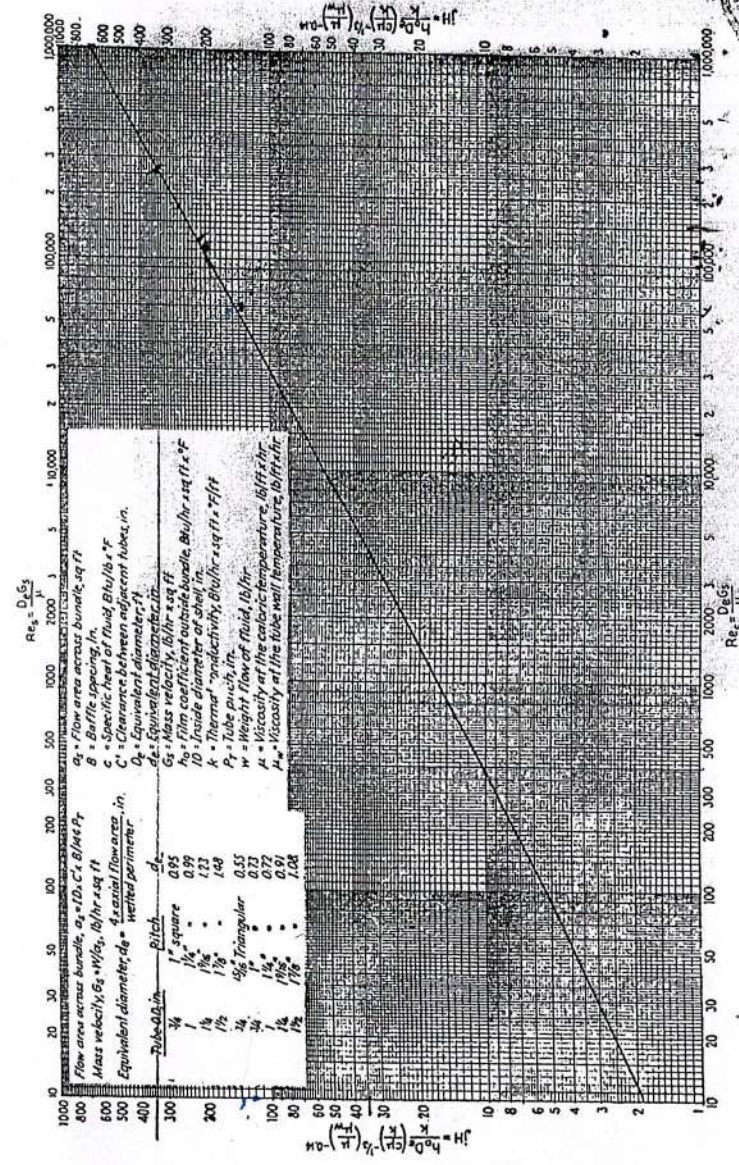


Fig. 28. Shell-side heat-transfer curve for bundles with 25% cut segmental baffles.

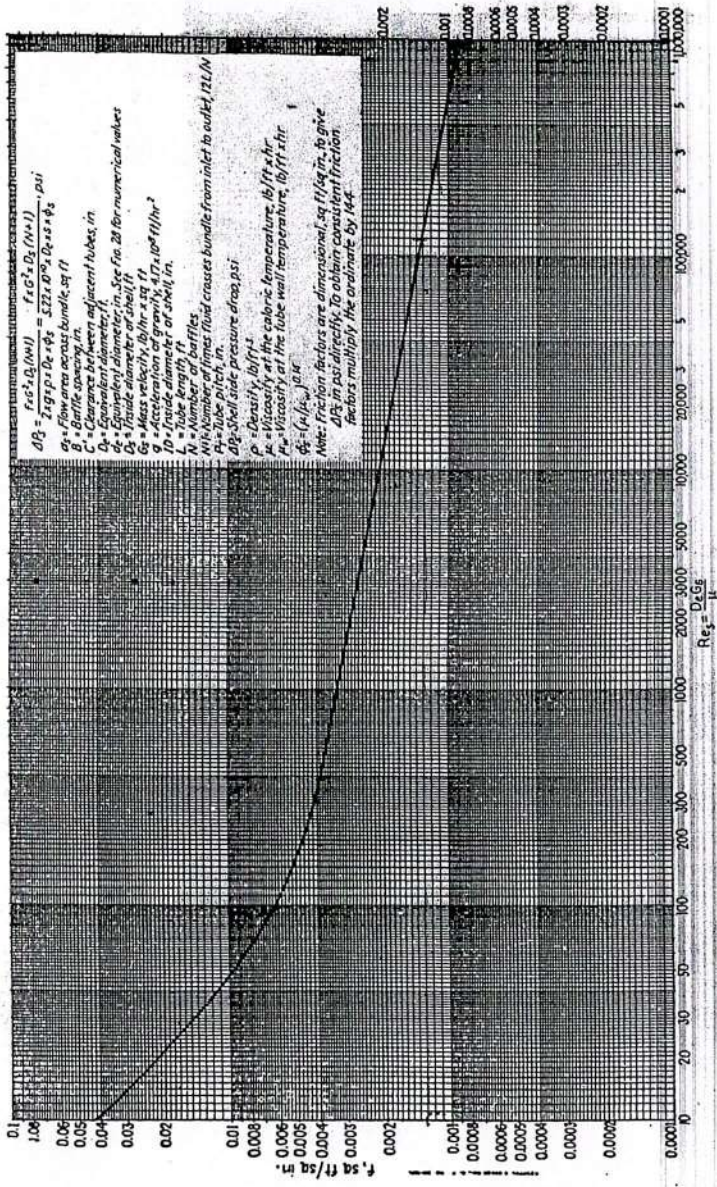


Fig. 29. Shell-side friction factors for bundles with 25% cut segmental baffles.

PROCESS HEAT TRANSFER

TABLE 8. APPROXIMATE OVERALL DESIGN COEFFICIENTS
Values include total dirt factors of 0.003 and allowable pressure drops of 5 to 10 psi on the controlling stream

Coolers		
Hot fluid	Cold fluid	Overall U_D
Water	Water	250-500§
Methanol	Water	250-500§
Ammonia	Water	250-500§
Aqueous solutions	Water	250-500§
Light organics*	Water	75-150
Medium organics†	Water	50-125
Heavy organics‡	Water	5-75
Gases	Water	2-50¶
Water	Brine	100-200
Light organics	Brine	40-100
Heaters		
Hot fluid	Cold fluid	Overall U_D
Steam	Water	200-700§
Steam	Methanol	200-700§
Steam	Ammonia	200-700§
Steam	Aqueous solutions: Less than 2.0 cp	200-700
Steam	More than 2.0 cp	100-500§
Steam	Light organics	100-200
Steam	Medium organics	50-100
Steam	Heavy organics	6-60
Steam	Gases	5-50¶
Exchangers		
Hot fluid	Cold fluid	Overall U_D
Water	Water	250-500§
Aqueous solutions	Aqueous solutions	250-500§
Light organics	Light organics	40-75
Medium organics	Medium organics	20-60
Heavy organics	Heavy organics	10-40
Heavy organics	Light organics	30-60
Light organics	Heavy organics	10-40

* Light organics are fluids with viscosities of less than 0.5 centipoise and include benzene, toluene, acetone, ethanol, methyl ethyl ketone, gasoline, light kerosene, and naphtha.

† Medium organics have viscosities of 0.5 to 1.0 centipoise and include kerosene, straw oil, hot gas oil, hot absorber oil, and some crudes.

‡ Heavy organics have viscosities above 1.0 centipoise and include cold gas oil, lube oils, fuel oils, reduced crude oils, tars, and asphalts.

§ Dirt factor 0.001.

|| Pressure drop 20 to 30 psi.

¶ These rates are greatly influenced by the operating pressure.



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TABLE 9. TUBE-SHEET LAYOUTS. (TUBE COUNTS)
Square Pitch

¾ in. OD tubes on 1-in. square pitch						1 in. OD tubes on 1¼-in. square pitch					
Shell ID, in.	1-P	2-P	4-P	6-P	8-P	Shell ID, in.	1-P	2-P	4-P	6-P	8-P
8	32	26	20	20		8	21	16	14		
10	52	52	40	36		10	32	32	26	24	
12	81	76	68	68	60	12	48	45	40	38	36
13¼	97	90	82	76	70	13¼	61	56	52	48	44
15¼	137	124	116	108	108	15¼	81	76	68	68	64
17¼	177	166	158	150	142	17¼	112	112	96	90	82
19¼	224	220	204	192	188	19¼	138	132	128	122	116
21¼	277	270	246	240	234	21¼	177	166	158	152	148
23¼	341	324	308	302	292	23¼	213	208	192	184	184
25	413	394	370	356	346	25	260	252	238	226	222
27	481	460	432	420	408	27	300	288	278	268	260
29	553	526	480	468	456	29	341	326	300	294	286
31	657	640	600	580	560	31	406	398	380	368	358
33	749	718	688	676	648	33	465	460	432	420	414
35	845	824	780	766	748	35	522	518	488	484	472
37	934	914	886	866	838	37	596	574	562	544	532
39	1049	1024	982	968	948	39	665	644	624	612	600
1¼ in. OD tubes on 1½-in. square pitch						1½ in. OD tubes on 1⅞-in. square pitch					
Shell ID, in.	1-P	2-P	4-P	6-P	8-P	Shell ID, in.	1-P	2-P	4-P	6-P	8-P
10	16	12	10			10	16	16	12	12	
12	30	24	22	16	16	12	22	22	16	16	
13¼	32	30	30	22	22	13¼	29	29	25	24	22
15¼	44	40	37	35	31	15¼	39	39	34	32	29
17¼	56	53	51	48	44	17¼	50	48	45	43	39
19¼	78	73	71	64	56	19¼	62	60	57	54	50
21¼	96	90	86	82	78	21¼	78	74	70	66	62
23¼	127	112	106	102	96	23¼	94	90	86	84	78
25	140	135	127	123	115	25	112	108	102	98	94
27	166	160	151	146	140	27	131	127	120	116	112
29	193	188	178	174	166	29	151	146	141	138	131
31	226	220	209	202	193	31	176	170	164	160	151
33	258	252	244	238	226	33	202	196	188	182	176
35	293	287	275	268	258	35	224	220	217	210	202
37	334	322	311	304	293	37	252	246	237	230	224
39	370	362	348	342	336	39					

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TABLE 9. TUBE-SHEET LAYOUTS (TUBE COUNTS).—(Continued)
Triangular Pitch

¾ in. OD tubes on 1½-in. triangular pitch						¾ in. OD tubes on 1-in. triangular pitch					
Shell ID, in.	1-P	2-P	4-P	6-P	8-P	Shell ID, in.	1-P	2-P	4-P	6-P	8-P
8	36	32	26	24	18	8	37	30	24	24	
10	62	56	47	42	36	10	61	52	40	36	
12	109	98	86	82	78	12	92	82	76	74	70
13¼	127	114	96	90	86	13¼	109	106	86	82	74
15¼	170	160	140	136	128	15¼	151	138	122	118	110
17¼	239	224	194	188	178	17¼	203	196	178	172	166
19¼	301	282	252	244	234	19¼	262	250	226	216	210
21¼	361	342	314	306	290	21¼	316	302	278	272	260
23¼	442	420	386	378	364	23¼	384	376	352	342	328
25	532	506	468	446	434	25	470	452	422	394	382
27	637	602	550	536	524	27	559	534	488	474	464
29	721	692	640	620	594	29	630	604	556	538	508
31	847	822	766	722	720	31	745	728	678	666	640
33	974	938	878	852	826	33	856	830	774	760	732
35	1102	1068	1004	988	958	35	970	938	882	864	848
37	1240	1200	1144	1104	1072	37	1074	1044	1012	986	870
39	1377	1330	1258	1248	1212	39	1206	1176	1128	1100	1078
1 in. OD tubes on 1¼-in. triangular pitch						1¼ in. OD tubes on 1½-in. triangular pitch					
Shell ID, in.	1-P	2-P	4-P	6-P	8-P	Shell ID, in.	1-P	2-P	4-P	6-P	8-P
8	21	16	16	14		10	20	18	14		
10	32	32	26	24		12	32	30	26	22	20
12	55	52	48	46	44	13¼	38	36	32	28	26
13¼	68	66	58	54	50	15¼	54	51	45	42	38
15¼	91	86	80	74	72	17¼	69	66	62	58	54
17¼	131	118	106	104	94	19¼	95	91	86	78	69
19¼	163	152	140	136	128	21¼	117	112	105	101	95
21¼	199	188	170	164	160	23¼	140	136	130	123	117
23¼	241	232	212	212	202	25	170	164	155	150	140
25	294	282	256	252	242	27	202	196	185	179	170
27	349	334	302	296	286	29	235	228	217	212	202
29	397	376	338	334	316	31	275	270	255	245	235
31	472	454	430	424	400	33	315	305	297	288	275
33	538	522	486	470	454	35	357	348	335	327	315
35	608	592	562	546	532	37	407	390	380	374	357
37	674	664	632	614	598	39	449	436	425	419	407
39	766	736	700	688	672						
1½ in. OD tubes on 1½-in. triangular pitch											
Shell ID, in.	1-P	2-P	4-P	6-P	8-P	Shell ID, in.	1-P	2-P	4-P	6-P	8-P
12	18	14	14	12	12						
13¼	27	22	18	16	14						
15¼	36	34	32	30	27						
17¼	48	44	42	38	36						
19¼	61	58	55	51	48						
21¼	76	72	70	66	61						
23¼	95	91	86	80	76						
25	115	110	105	98	95						
27	136	131	125	118	115						
29	160	154	147	141	136						
31	184	177	172	165	160						
33	215	206	200	190	184						
35	246	238	230	220	215						
37	275	268	260	252	246						
39	307	299	290	284	275						

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TABLE 10. HEAT EXCHANGER AND CONDENSER TUBE DATA

Tube OD, in.	BWG	Wall thickness, in.	ID, in.	Flow area per tube, in. ²	Surface per lin ft, ft ²		Weight per lin ft, lb steel
					Outside	Inside	
¾	12	0.109	0.282	0.0625	0.1309	0.0748	0.493
	14	0.083	0.334	0.0876			
	16	0.065	0.370	0.1076			
	18	0.049	0.402	0.127			
	20	0.035	0.430	0.145			
¾	10	0.134	0.482	0.182	0.1963	0.1263	0.965
	11	0.120	0.510	0.204			
	12	0.109	0.532	0.223			
	13	0.095	0.560	0.247			
	14	0.083	0.584	0.268			
	15	0.072	0.606	0.289			
	16	0.065	0.620	0.302			
	17	0.058	0.634	0.314			
	18	0.049	0.652	0.334			
	1	8	0.165	0.670			
9		0.148	0.704	0.389			
10		0.134	0.732	0.421			
11		0.120	0.760	0.455			
12		0.109	0.782	0.479			
13		0.095	0.810	0.515			
14		0.083	0.834	0.546			
15		0.072	0.856	0.576			
16		0.065	0.870	0.594			
17		0.058	0.884	0.613			
18	0.049	0.902	0.639				
1¼	8	0.165	0.920	0.665	0.3271	0.2409	2.09
	9	0.148	0.954	0.714			
	10	0.134	0.982	0.757			
	11	0.120	1.01	0.800			
	12	0.109	1.03	0.836			
	13	0.095	1.06	0.884			
	14	0.083	1.08	0.923			
	15	0.072	1.11	0.960			
	16	0.065	1.12	0.985			
	17	0.058	1.13	1.01			
18	0.049	1.15	1.04				
1½	8	0.165	1.17	1.075	0.3925	0.3063	2.57
	9	0.148	1.20	1.14			
	10	0.134	1.23	1.19			
	11	0.120	1.26	1.25			
	12	0.109	1.28	1.29			
	13	0.095	1.31	1.35			
	14	0.083	1.33	1.40			
	15	0.072	1.36	1.44			
	16	0.065	1.37	1.47			
	17	0.058	1.38	1.50			
18	0.049	1.40	1.54				

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TABLE 11. DIMENSIONS OF STEEL PIPE (IPS)

Nominal pipe size, IPS, in.	OD, in.	Schedule No.	ID, in.	Flow area per pipe, in. ²	Surface per lin ft, ft. ² /ft.		Weight per lin ft, lb steel
					Outside	Inside	
1/8	0.405	40*	0.269	0.058	0.106	0.070	0.25
		80†	0.215	0.036		0.056	0.32
1/4	0.540	40*	0.364	0.104	0.141	0.095	0.43
		80†	0.302	0.072		0.079	0.54
3/8	0.675	40*	0.493	0.192	0.177	0.129	0.57
		80†	0.423	0.141		0.111	0.74
1/2	0.840	40*	0.622	0.304	0.220	0.163	0.85
		80†	0.546	0.235		0.143	1.09
3/4	1.05	40*	0.824	0.534	0.275	0.216	1.13
		80†	0.742	0.432		0.194	1.48
1	1.32	40*	1.049	0.864	0.344	0.274	1.68
		80†	0.957	0.718		0.250	2.17
1 1/4	1.66	40*	1.380	1.50	0.435	0.362	2.28
		80†	1.278	1.28		0.335	3.00
1 1/2	1.90	40*	1.610	2.04	0.498	0.422	2.72
		80†	1.500	1.76		0.393	3.64
2	2.38	40*	2.067	3.35	0.622	0.542	3.66
		80†	1.939	2.95		0.508	5.03
2 1/2	2.88	40*	2.469	4.79	0.753	0.647	5.80
		80†	2.323	4.23		0.609	7.67
3	3.50	40*	3.068	7.38	0.917	0.804	7.58
		80†	2.900	6.61		0.760	10.3
4	4.50	40*	4.026	12.7	1.178	1.055	10.8
		80†	3.826	11.5		1.002	15.0
6	6.625	40*	6.065	28.9	1.734	1.590	19.0
		80†	5.761	26.1		1.510	28.6
8	8.625	40*	7.981	50.0	2.258	2.090	28.6
		80†	7.625	45.7		2.000	43.4
10	10.75	40*	10.02	78.8	2.814	2.62	40.5
		60	9.75	74.6		2.55	54.8
12	12.75	30	12.09	115	3.338	3.17	43.8
14	14.0	30	13.25	138	3.665	3.47	54.6
16	16.0	30	15.25	183	4.189	4.00	62.6
18	18.0	20‡	17.25	234	4.712	4.52	72.7
20	20.0	20	19.25	291	5.236	5.05	78.6
22	22.0	20‡	21.25	355	5.747	5.56	84.0
24	24.0	20	23.25	425	6.283	6.09	94.7

* Commonly known as standard.
 † Commonly known as extra heavy.
 ‡ Approximately.

TABLE 12. FOULING FACTORS*

Temperature of heating medium	Up to 240°F		240-400°F†	
	125°F or less		Over 125°F	
	Water velocity, fps		Water velocity, fps	
Temperature of water	3 ft and less	Over 3 ft	3 ft and less	Over 3 ft
Water				
Sea water	0.0005	0.0005	0.001	0.001
Brackish water	0.002	0.001	0.003	0.002
Cooling tower and artificial spray pond:				
Treated make-up	0.001	0.001	0.002	0.002
Untreated	0.003	0.003	0.005	0.004
City or well water (such as Great Lakes)	0.001	0.001	0.002	0.002
Great Lakes	0.001	0.001	0.002	0.002
River water:				
Minimum	0.002	0.001	0.003	0.022
Mississippi	0.003	0.002	0.004	0.003
Delaware, Schuylkill	0.003	0.002	0.004	0.003
East River and New York Bay	0.003	0.002	0.004	0.003
Chicago sanitary canal	0.008	0.006	0.010	0.008
Muddy or silty	0.003	0.002	0.004	0.003
Hard (over 15 grains/gal)	0.003	0.003	0.005	0.005
Engine jacket	0.001	0.001	0.001	0.001
Distilled	0.0005	0.0005	0.0005	0.0005
Treated boiler feedwater	0.001	0.0005	0.001	0.001
Boiler blowdown	0.002	0.002	0.002	0.002

† Ratings in the last two columns are based on a temperature of the heating medium of 240 to 400°F. If the heating medium temperature is over 400°F, and the cooling medium is known to scale these ratings should be modified accordingly.

Petroleum Fractions	
Oils (industrial):	Liquids (industrial):
Fuel oil	Organic
Clean recirculating oil	Refrigerating liquids, heating, cooling, or evaporating
Machinery and transformer oils	Brine (cooling)
Quenching oil	Atmospheric distillation units:
Vegetable oils	Residual bottoms, less than 25°API
Gases, vapors (industrial):	Distillate bottoms, 25°API or above
Coke-oven gas, manufactured gas	Atmospheric distillation units:
Diesel-engine exhaust gas	Overhead untreated vapors
Organic vapors	Overhead treated vapors
Steam (non-oil bearing)	Side-stream cuts
Alcohol vapors	Vacuum distillation units:
Steam, exhaust (oil bearing from reciprocating engines)	Overhead vapors to oil:
Refrigerating vapors (condensing from reciprocating compressors)	From bubble tower (partial condenser)
Air	From flash pot (no appreciable reflux)

* Standards of Tubular Exchanger Manufacturers Association, 2d ed., New York, 1949.

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TABLE 12. FOULING FACTORS.*—(Continued)

Overhead vapors in water-cooled condensers:	Lean oil.....	0.002
From bubble tower (final condenser).....	Overhead vapors.....	0.001
From flash pot.....	Gasoline.....	0.0005
Side stream:	Debutanizer, Depropanizer, Depentanizer, and Alkylation Units:	
To oil.....	Feed.....	0.001
To water.....	Overhead vapors.....	0.001
Residual bottoms, less than 20°API.....	Product coolers.....	0.001
Distillate bottoms, over 20°API.....	Product reboilers.....	0.002
	Reactor feed.....	0.002
Natural gasoline stabilizer units:	Lube treating units:	
Feed.....	Solvent oil mixed feed.....	0.002
O.H. vapors.....	Overhead vapors.....	0.001
Product coolers and exchangers.....	Refined oil.....	0.001
Product reboilers.....	Refined oil heat exchangers water cooled†.....	0.003
H ₂ S Removal Units:	Gums and tars:	
For overhead vapors.....	Oil-cooled and steam generators.....	0.005
Solution exchanger coolers.....	Water-cooled.....	0.003
Reboiler.....	Solvent.....	0.001
Cracking units:	Deasphalting units:	
Gas oil feed:	Feed oil.....	0.002
Under 500°F.....	Solvent.....	0.001
500°F and over.....	Asphalt and resin:	
Naphtha feed:	Oil-cooled and steam generators.....	0.005
Under 500°F.....	Water-cooled.....	0.003
500°F and over.....	Solvent vapors.....	0.001
Separator vapors (vapors from separator, flash pot, and vaporizer).....	Refined oil.....	0.001
Bubble-tower vapors.....	Refined oil water cooled.....	0.003
Residuum.....	Dewaxing units:	
Absorption units:	Lube oil.....	0.001
Gas.....	Solvent.....	0.001
Fat oil.....	Oil wax mix heating.....	0.001
	Oil wax mix cooling†.....	0.003

† Precautions must be taken against deposition of wax.

Crude Oil Streams:

	0-199°F			200-299°F			300-499°F			500°F and over		
	Velocity, fps											
	Under 2 ft	2-4 ft	4 ft and over	Under 2 ft	2-4 ft	4 ft and over	Under 2 ft	2-4 ft	4 ft and over	Under 2 ft	2-4 ft	4 ft and over
Dry...	0.003	0.002	0.002	0.003	0.002	0.002	0.004	0.003	0.002	0.005	0.004	0.003
Salt§	0.003	0.002	0.002	0.005	0.004	0.004	0.006	0.005	0.004	0.007	0.006	0.005

§ Refers to a wet crude—any crude that has not been dehydrated.

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APPENDIX D

Physical Property Data Bank

Inorganic compounds are listed in alphabetical order of the principal element in the empirical formula.

Organic compounds with the same number of carbon atoms are grouped together, and arranged in order of the number of hydrogen atoms, with other atoms in alphabetical order.

- n = Number in list
MW = Molecular weight
FP = Normal freezing point, deg C
BP = Normal boiling point, deg C
T_c = Critical temperature, deg K
P_c = Critical pressure, bar
V_c = Critical volume, cubic metre/mol
DEN = Liquid density, kg/cubic metre
DEN = Reference temperature for liquid density, deg C
H_vVAP = Heat of vaporisation at normal boiling point, J/mol
VISA, VISB = Constants in the liquid viscosity equation:
 $\text{LOG}[\text{viscosity}] = [\text{VISA}] * [(1/T) - (1/\text{VISB})]$, viscosity mNs/sq.m, T deg K.
DELHF = Standard enthalpy of formation of vapour at 298 K, kJ/mol.
DELGF = Standard Gibbs energy of formation of vapour at 298 K, kJ/mol.
CPVAPA, CPVAPB, CPVAPC, CPVAPD = Constants in the ideal gas heat capacity equation:
 $C_p = \text{CPVAPA} + (\text{CPVAPB}) * T + (\text{CPVAPC}) * T **2 + (\text{CPVAPD}) * T **3$,
 C_p J/mol K, T deg K.
ANTA, ANTB, ANTC = Constants in the Antoine equation:
 $\text{Ln}(\text{vapour pressure}) = \text{ANTA} - \text{ANTB}/(T + \text{ANTC})$, vap. press. mmHg, T deg K.
To convert mmHg to N/sq.m multiply by 133.32.
To convert degrees Celsius to Kelvin add 273.15.
TMN = Minimum temperature for Antoine constant, deg C
TMX = Maximum temperature for Antoine constant, deg C

Most of the values in this data bank were taken, with the permission of the publisher from: The Properties of Gases and Liquids, by Reid, R. C., Sherwood, T. K. & Prausnitz, J. M., 3rd edn, McGraw-Hill.

CHEMICAL ENGINEERING

Table with columns: NO, FORMULA, COMPOUND NAME, MOLWT, TFP, TBP, TC, PC, VC, LDEN, TDEN, HVAP, NO. Lists chemical compounds and their properties.



Table with columns: NO, VISA, VISB, DELHF, DELGF, CPVAPA, CPVAPB, CPVAPC, CPVAPD, ANTA, ANTB, ANTC, TMIN, TMAX, NO. Lists chemical compounds and their properties.

NO	FORMULA	COMPOUND NAME	MOLWT	TFP	TBP	TC	PC	VC	LDEN	TDEN	HVAP	NO
51	CHCLF2	CHLORODIFLUOROMETHANE	86.469	-160.2	-40.8	369.2	49.8	0.165	1230	16	20.205	51
52	CHCLF3	CHLOROTRIFLUOROMETHANE	102.923	-135.2	8.8	451.6	51.7	0.197	1380	9	24.953	52
53	CHCL3	CHLOROFORM	119.378	-63.6	61.1	536.4	54.7	0.239	1489	20	29.726	53
54	CHN	HYDROGEN CYANIDE	27.026	-13.3	25.7	456.8	53.9	0.139	688	20	25.234	54
55	CHBR2	DIBROMOMETHANE	173.835	-52.6	96.8	583.0	71.9	0.193	2500	20	28.010	55
56	CH2CL2	DICHLOROMETHANE	84.993	-95.1	39.8	510.0	60.8	0.193	1317	25	28.010	56
57	CH2O	FORMALDEHYDE	30.026	-117.2	-19.2	408.0	65.9	0.193	815	15	21.919	57
58	CH2O2	FORMIC ACID	46.025	8.3	100.6	580.0	86.1	0.139	1226	15	21.919	58
59	CH3BR	METHYL BROMIDE	94.939	-91.7	3.5	464.0	86.1	0.139	1737	5	23.928	59
60	CH3CL	METHYL CHLORIDE	50.488	-91.8	-74.3	416.3	66.8	0.124	915	5	21.436	60
61	CH3F	METHYL FLUORIDE	34.033	-141.8	-78.4	317.8	58.8	0.124	843	-60	21.436	61
62	CH3I	METHYL IODIDE	141.939	-66.5	42.4	528.0	65.9	0.190	2279	-60	27.214	62
63	CH3NO2	NITROMETHANE	61.041	-28.6	101.2	588.0	63.1	0.173	1128	20	34.436	63
64	CH4	METHANE	16.043	-182.5	-161.5	190.6	46.0	0.099	425	-161	81.85	64
65	CH4O	METHANOL	32.042	-97.7	64.6	512.6	81.0	0.118	791	20	35.278	65
66	CH4S	METHYL MERCAPTAN	48.107	-123.2	5.9	470.0	72.3	0.145	866	20	24.577	66
67	CH5N	METHYL AMINE	31.058	-93.5	-6.4	430.0	74.6	0.140	703	-14	26.000	67
68	CH6N2	METHYL HYDRAZINE	46.072	-156.5	90.8	567.0	80.4	0.271	1590	-78	16.161	68
69	CH6Si	METHYL SILANE	46.145	-106.2	-57.6	352.5	35.5	0.252	1455	25	19.469	69
70	C2CLF5	CHLOROPENTAFLUOROETHANE	154.467	-106.2	-39.2	353.2	31.6	0.252	1455	25	19.469	70
71	C2CL2F4	1,1-DICHLORO-1,2,2,2-TETRAFLUOROETHANE	170.992	-94.2	3.8	418.6	33.0	0.294	1480	4	23.279	71
72	C2CLF4	1,2-DICHLORO-1,1,2,2-TETRAFLUOROETHANE	170.992	-93.9	3.7	418.9	32.6	0.293	1480	4	23.279	72
73	C2CL3F3	1,2-DICHLORO-1,1,2,2-TETRAFLUOROETHANE	187.380	-95.0	47.5	487.2	34.1	0.304	1580	16	27.507	73
74	C2CL4	TETRACHLOROETHYLENE	165.834	-22.2	121.1	620.0	44.6	0.290	1620	20	34.750	74
75	C2CL4F2	1,1,2,2-TETRACHLORO-1,2-DIFLUOROETHANE	203.831	24.8	91.5	551.0	39.4	0.175	1645	25	33.327	75
76	C2F4	TETRAFLUOROETHYLENE	100.016	-142.5	-75.7	306.4	37.6	0.221	1519	-76	16.161	76
77	C2F6	HEXAFLUOROETHANE	138.012	-100.8	-78.3	292.8	37.6	0.221	1590	-78	16.161	77
78	C2N2	CYANOGEN	52.035	-27.9	-20.7	400.0	59.8	0.256	1462	0	31.401	78
79	CH2CL3	TRICHLOROETHYLENE	131.389	-116.4	87.2	571.0	49.1	0.256	1462	0	31.401	79
80	CH2FO2	TRIFLUOROACETIC ACID	114.024	-15.3	72.4	491.3	32.6	0.113	1535	20	16.957	80
81	CH2	ACETYLENE	26.038	-80.8	-84.0	308.3	61.4	0.113	615	-84	16.957	81
82	CH2F2	1,1-DIFLUOROETHYLENE	64.035	-135.2	-113.2	380.8	44.6	0.154	1104	-14	20.641	82
83	CH2O	KETENE	42.038	-153.8	-13.4	379.0	64.8	0.145	969	-14	20.641	83
84	CH3CL	VINYL CHLORIDE	62.499	-84.1	43.2	480.0	56.0	0.169	1100	30	20.641	84
85	CH3CLF2	1-CHLORO-1,1-DIFLUOROETHANE	100.490	-131.2	-9.8	410.2	41.2	0.231	1104	20	28.680	85
86	CH3CLO	ACETYL CHLORIDE	78.98	-113.0	50.7	508.0	58.8	0.204	1104	20	28.680	86
87	CH3CL3	1,1,2-TRICHLOROETHANE	133.400	-36.7	113.7	602.0	41.5	0.294	1441	20	33.327	87
88	CH3F	VINYL FLUORIDE	46.044	-143.2	-37.7	327.8	52.4	0.144	1441	20	33.327	88
89	CH3F3	1,1,1-TRIFLUOROETHANE	84.041	-111.3	-47.7	346.2	37.6	0.221	19176	20	19.176	89
90	CH3N	ACETONITRILE	41.053	-43.9	81.6	346.2	37.6	0.221	19176	20	19.176	90
91	CH3NO	METHYL ISOCYANATE	57.052	-169.2	38.8	491.0	55.7	0.173	782	20	31.401	91
92	CH3H	ETHYLENE	28.054	-97.0	-103.8	282.4	50.4	0.129	958	20	29.601	92
93	CH3CL2	1,2-DICHLOROETHANE	98.960	-117.0	57.2	523.0	50.7	0.240	1168	25	13.553	93
94	CH3CLO	1,2-DICHLOROETHANE	98.960	-117.0	57.2	523.0	50.7	0.240	1168	25	13.553	94
95	CH3HO	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	95
96	CH3O	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	96
97	CH4O2	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	97
98	CH4O2	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	98
99	CH4O2	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	99
100	CH4O2	ACETALDEHYDE	44.054	-125.0	20.3	386.6	45.0	0.181	1250	16	32.029	100

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CHEMICAL ENGINEERING

Table with columns: NO, FORMULA, COMPOUND NAME, MOLWT, TBP, TC, PC, VC, LDBEN, TDBEN, HVAP, NO. Lists various chemical compounds and their properties.



Table with columns: NO, VISA, VISB, DELHF, DELQF, CPVAPA, CPVAPB, CPVAPC, CPVAPD, ANTA, ANTB, ANTC, TMN, TMX, NO. Lists chemical compounds and their properties.

NO	FORMULA	COMPOUND NAME	MOL.WT	TPP	TBP	TC	PC	VC	LDEN	TDEN	HVAP	NO
251	C6H5CL	CHLOROBENZENE	112.559	-45.6	131.7	632.4	45.2	0.308	1106	20	36.572	251
252	C6H5F	FLUOROBENZENE	106.104	-39.2	85.3	560.1	45.5	0.271	1024	20		252
253	C6H5I	IODOBENZENE	204.011	-31.4	188.2	721.0	45.2	0.351	1024	4	39.523	253
254	C6H5NO2	NITROBENZENE	123.112	4.8	210.6	712.0	35.0	0.337	1203	20	44.031	254
255	C6H6	BENZENE	78.114	5.5	80.1	562.1	48.9	0.259	885	16	30.781	255
256	C6H6O	PHENOL	94.113	40.8	181.8	694.2	61.3	0.229	1052	40	45.636	256
257	C6H7N	ANILINE	93.129	-6.2	184.3	699.0	53.1	0.270	1022	20	41.868	257
258	C6H7N	4-METHYL PYRIDINE	93.129	3.7	145.3	646.0	44.6	0.311	955	20	37.472	258
259	C6H10	1,5-HEXADIENE	82.146	-141.2	59.4	507.0	34.5	0.328	692	20	27.470	259
260	C6H10	CYCLOHEXENE	82.146	-103.5	82.9	500.4	43.5	0.292	816	16	30.480	260
261	C6H10O	CYCLOHEXANONE	98.145	-31.2	155.6	629.0	38.5	0.312	951	15	39.775	261
262	C6H12	CYCLOHEXANE	84.162	6.5	80.7	553.4	40.7	0.308	779	20	29.977	262
263	C6H12	METHYLCYCLOPENTANE	84.162	-42.5	71.8	532.7	37.9	0.319	754	16	29.098	263
264	C6H12	1-HEXENE	84.162	-139.9	63.4	540.0	31.7	0.350	673	20	28.303	264
265	C6H12	CIS-3-HEXENE	84.162	-141.2	68.8	518.0	32.8	0.351	687	20	29.140	265
266	C6H12	TRANS-2-HEXENE	84.162	-133.2	67.8	516.0	32.7	0.351	678	20	28.931	266
267	C6H12	CIS-3-HEXENE	84.162	-137.9	66.4	517.0	32.8	0.350	680	20	28.721	267
268	C6H12	TRANS-3-HEXENE	84.162	-135.1	67.1	519.0	32.5	0.350	677	20	28.973	268
269	C6H12	2-METHYL-2-PENTENE	84.162	-134.9	67.7	518.0	32.8	0.351	691	16	29.015	269
270	C6H12	3-METHYL-CIS-2-PENTENE	84.162	-138.5	70.4	490.0	30.4	0.360	669	20	28.847	270
271	C6H12	3-METHYL-TRANS-2-PENTENE	84.162	-134.2	56.4	493.0	30.4	0.360	669	20	27.988	271
272	C6H12	4-METHYL-CIS-2-PENTENE	84.162	-141.2	58.5	493.0	30.4	0.360	669	20	27.968	272
273	C6H12	4-METHYL-TRANS-2-PENTENE	84.162	-157.3	55.6	501.0	32.4	0.343	678	20	21.424	273
274	C6H12	2,3-DIMETHYL-1-BUTENE	84.162	-74.3	73.2	524.0	33.6	0.351	708	20	29.655	274
275	C6H12	2,3-DIMETHYL-2-BUTENE	84.162	-115.2	41.2	490.0	32.5	0.340	653	20	25.665	275
276	C6H12	3,3-DIMETHYL-1-BUTENE	100.161	-84.2	74.8	625.0	37.5	0.327	942	30	45.511	276
277	C6H12O	CYCLOHEXANOL	100.161	-84.2	116.4	571.0	32.7	0.371	801	20	35.888	277
278	C6H12O	METHYL ISOBUTYL KETONE	100.161	-73.5	116.4	579.0	31.4	0.400	898	0	36.006	278
279	C6H12O2	N-BUTYL ACETATE	116.160	-98.9	128.8	561.0	30.4	0.414	875	20	35.873	279
280	C6H12O2	ISOBUTYL ACETATE	116.160	-91.2	120.8	566.0	31.4	0.395	879	20	34.332	280
281	C6H12O2	ETHYL BUTYRATE	116.160	-88.2	111.0	553.0	30.4	0.410	869	20	34.332	281
282	C6H12O2	ETHYL ISOBUTYRATE	116.160	-75.9	122.5	578.0	29.7	0.370	881	20	36.383	282
283	C6H12O2	N-PROPYL PROPIONATE	116.160	-95.4	68.7	507.4	29.7	0.370	659	20	28.872	283
284	C6H14	N-HEXANE	86.178	-153.7	60.2	497.5	30.1	0.367	653	20	28.800	284
285	C6H14	2-METHYL PENTANE	86.178	-118.2	63.2	504.4	31.2	0.367	664	20	28.093	285
286	C6H14	3-METHYL PENTANE	86.178	-99.9	49.7	488.7	30.8	0.359	649	20	26.322	286
287	C6H14	2,2-DIMETHYL BUTANE	86.178	-128.6	58.0	495.9	31.3	0.358	662	20	27.298	287
288	C6H14	2,3-DIMETHYL BUTANE	86.178	-44.0	157.0	610.0	40.5	0.381	819	20	48.567	288
289	C6H14O	1-HEXANOL	102.177	-103.2	92.2	531.0	30.4	0.390	749	20	31.820	289
290	C6H14O	ETHYL BUTYL ETHER	102.177	-85.5	68.3	500.0	28.8	0.386	724	20	29.349	290
291	C6H15N	DIISOPROPYL ETHER	102.177	-63.2	109.2	550.0	31.4	0.407	738	20	37.011	291
292	C6H15N	DIPROPYLAMINE	101.193	-114.8	89.5	535.0	30.4	0.390	728	20	31.401	292
293	C6H15N	TRIETHYLAMINE	101.193	-114.8	89.5	535.0	30.4	0.390	728	20	31.401	293
294	C7F14	PERFLUOROMETHYLCYCLOHEXANE	350.055	-78.2	76.3	486.8	23.3	0.664	1733	15		294
295	C7F16	PERFLUORO-N-HEPTANE	388.051	-13.2	190.8	699.4	42.2	0.664	1733	15		295
296	C7H5N	BENZONITRILE	103.124	-57.2	178.8	695.0	46.6	0.341	1045	20	42.705	296
297	C7H6O	BENZALDEHYDE	106.124	12.4	249.8	752.0	44.0	0.371	1075	130	40.660	297
298	C7H6O2	BENZOIC ACID	122.124	14.2	249.8	752.0	44.0	0.371	1075	130	40.660	298
299	C7H8O2	O-NITROTOLUENE	137.139	14.2	249.8	752.0	44.0	0.371	1075	130	40.660	299
300	C7H8O2	M-NITROTOLUENE	137.139	14.2	249.8	752.0	44.0	0.371	1075	130	40.660	300



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CHEMICAL ENGINEERING

NO	FORMULA	COMPOUND NAME	MOLWT	TFP	TBP	TC	PC	VC	LDEN	TDEN	HVAP	NO
301	C7H7NO2	P-NITROTOLUENE	137.139	54.8	238.0	735.0	30.1	0.371	1164	20	46.875	301
302	C7H8	TOLUENE	92.141	-95.2	110.6	110.6	41.7	0.316	867	20	33.201	302
303	C7H8	METHYL PHENYL ETHER	108.140	-37.5	153.6	641.0	41.7		996	25	50.535	303
304	C7H8O	BENZYL ALCOHOL	108.140	-15.4	205.4	677.0	46.6	0.334	1041	20	45.217	304
305	C7H8O	O-CRESOL	108.140	30.9	191.0	697.6	50.1	0.282	1034	40	47.436	305
306	C7H8O	M-CRESOL	108.140	12.2	201.9	705.8	45.6	0.310	1019	40	47.478	306
307	C7H8O	P-CRESOL	107.156	34.7	168.8	704.6	51.5		942	0		307
308	C7H9N	2,3-DIMETHYLPYRIDINE	107.156		157.0	644.2			938	0		308
309	C7H9N	2,5-DIMETHYLPYRIDINE	107.156		179.1	683.8			954	25		309
310	C7H9N	3,4-DIMETHYLPYRIDINE	107.156		171.9	667.2			939	20		310
311	C7H9N	3,5-DIMETHYLPYRIDINE	107.156	-57.2	195.9	701.0	52.0	0.343	989	20	45.364	311
312	C7H9N	METHYLPHENYLAMINE	107.156	-14.8	200.1	694.0	37.5	0.343	998	20	45.636	312
313	C7H9N	O-TOLUIDINE	107.156	-30.4	200.3	709.0	41.5		964	50	44.799	313
314	C7H9N	M-TOLUIDINE	107.156	43.7	200.1	667.0			917	20	33.076	314
315	C7H9N	P-TOLUIDINE	98.189	-68.8	118.7	589.0	37.2	0.390	759	16	30.312	315
316	C7H14	CYCLOHEPTANE	98.189	-33.9	99.5	547.0	34.5	0.368	777	16	31.719	316
317	C7H14	1,1-DIMETHYLCYCLOPENTANE	98.189	-117.6	91.8	564.8	34.5	0.362	756	16	30.878	317
318	C7H14	CIS-1,2-DIMETHYLCYCLOPENTANE	98.189	-117.6	103.4	553.2	34.5	0.375	771	16	32.301	318
319	C7H14	TRANS-1,2-DIMETHYLCYCLOPENTANE	98.189	-126.6	100.9	572.1	34.8	0.368	774	16	31.108	319
320	C7H14	ETHYLCYCLOHEXANE	98.189	-118.9	93.6	537.2	28.4	0.440	679	20	28.889	320
321	C7H14	1-HEPTENE	98.189	-109.9	77.8	533.0	29.0	0.400	705	20	28.889	321
322	C7H14	N-HEPTANE	100.205	-90.6	98.4	540.2	27.4	0.432	684	20	31.719	322
323	C7H16	2-METHYLHEXANE	100.205	-173.2	91.8	535.2	27.4	0.404	679	20	30.689	323
324	C7H16	3-METHYLHEXANE	100.205	-123.8	79.2	520.4	28.2	0.416	674	20	30.815	324
325	C7H16	2,2-DIMETHYLPENTANE	100.205	-119.2	89.7	537.3	29.1	0.393	665	20	30.409	325
326	C7H16	2,3-DIMETHYLPENTANE	100.205	-134.5	80.5	536.3	29.5	0.414	693	20	29.517	326
327	C7H16	2,4-DIMETHYLPENTANE	100.205	-118.6	93.4	540.6	28.9	0.416	698	20	30.978	327
328	C7H16	3,3-DIMETHYLPENTANE	100.205	-24.9	80.8	531.1	29.6	0.398	690	20	28.968	328
329	C7H16	3-ETHYLPENTANE	116.204	-34.0	176.3	633.0	30.4	0.435	822	20	48.148	329
330	C7H16	2,2,3-TRIMETHYLBUTANE	148.118	130.8	286.8	810.0	47.6	0.368	906	20	49.614	330
331	C7H16	1-HEPTANOL	104.152	-30.7	145.1	647.0	39.9		1032	15	36.844	331
332	C8H8O3	PHTHALIC ANHYDRIDE	120.151	19.6	201.7	701.0	38.5	0.376	1083	20	43.124	332
333	C8H8O3	STYRENE	136.151	-12.4	199.0	692.0	36.5	0.366	1083	20	36.844	333
334	C8H8O3	METHYL PHENYL KETONE	106.168	-25.2	144.4	630.2	37.3	0.396	880	20	36.844	334
335	C8H8O3	METHYL BENZOATE	106.168	-47.9	139.1	617.0	35.5	0.376	864	20	36.844	335
336	C8H10	O-XYLENE	106.168	13.2	138.3	616.2	35.2	0.379	861	20	36.006	336
337	C8H10	P-XYLENE	106.168	-95.0	136.1	617.1	36.1		867	20	48.106	337
338	C8H10	M-XYLENE	122.167	-3.4	204.5	703.0			1025	0	50.660	338
339	C8H10	ETHYL BENZENE	122.167	-4.2	218.4	716.4			979	4	47.311	339
340	C8H10	O-ETHYLPHENOL	122.167	44.8	169.8	647.0			1032	20	47.143	340
341	C8H10	M-ETHYLPHENOL	122.167	-10.2	169.8	647.0			1032	20	47.143	341
342	C8H10	P-ETHYLPHENOL	122.167	74.8	216.9	722.8			1032	20	47.143	342
343	C8H10	ETHYL PHENYL ETHER	122.167	74.8	216.9	722.8			1032	20	47.143	343
344	C8H10	2,3-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	344
345	C8H10	2,4-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	345
346	C8H10	2,5-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	346
347	C8H10	2,6-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	347
348	C8H10	2,7-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	348
349	C8H10	2,8-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	349
350	C8H10	2,9-XYLENOL	122.167	74.8	216.9	722.8			1032	20	47.143	350



NO	FORMULA	COMPOUND NAME	MOLWT	TPP	TBP	TC	PC	VC	LDBN	TDBN	HVAP	NO
451	C12H10	DIPHENYL	154.212	69.2	255.2	789.0	38.5	0.502		74	45.636	451
452	C12H10O	DIPHENYL ETHER	170.211	26.8	238.0	766.0	31.4		1066	30	47.143	452
453	C12H24	N-HEPTYL-CYCLOPENTANE	168.324	-35.2	213.3	657.0	18.5	0.713	758	20	43.998	453
454	C12H24	N-DODECANE	170.440	-9.6	216.3	658.3	18.2	0.720	748	20	43.668	454
455	C12H26	N-DODECANE	186.339	-43.2	226.4	657.0	19.3	0.718	794	20	45.636	455
456	C12H26O	DIREXYL ETHER	186.339	23.9	259.9	679.0	18.2		835	20	44.380	456
457	C12H26O	DODECANOL	186.335			643.0	18.2	0.534	779			457
458	C12H27N	TRIBUTYLAMINE	166.233	114.0	297.9	822.3	29.9		1006	20	45.427	458
459	C13H12	FLUORENE	166.239	26.8	264.3	694.0	29.8			20	45.008	459
460	C13H12	DIPHENYLMETHANE	182.331	-23.1	232.7	674.0	17.0	0.780	766	20	45.678	460
461	C13H26	N-TRIDECANE	184.367	-5.4	235.4	675.8	17.2		755		56.522	461
462	C13H28	N-TRIDECANE	178.234	216.5	341.2	883.0	16.5	0.830	786	0	55.684	462
463	C14H10	ANTHRACENE	178.234	100.5	262.1	710.5	15.6		763	20	47.269	463
464	C14H10	PHENANTHRENE	196.378	-12.9	251.1	689.0	16.2				46.934	464
465	C14H28	N-NONYL-CYCLOPENTANE	198.394	5.8	255.5	694.0	16.2				46.934	465
466	C14H28	I-TETRADECANE	198.394			694.0	16.2				47.646	466
467	C14H30	N-TETRADECANE	192.261			843.7	27.0	0.598				467
468	C15H12	I-PHENYLINDENE	194.277			811.1	24.6	0.629				468
469	C15H14	2-ETHYLFLUORENE	210.405	-3.8	279.3	723.8	15.2		791	0	49.027	469
470	C15H30	N-DECYL-CYCLOPENTANE	212.421	9.8	270.6	707.0	15.2	0.880	769	20	48.692	470
471	C15H30	I-PENTADECANE	202.256	110.0	393.0	956.6	26.0	0.660			50.409	471
472	C15H32	N-PENTADECANE	202.256	151.0	362.0	892.1	26.0	0.637			50.409	472
473	C16H10	FLUORANTHENE	204.272	-35.2	334.8	840.1	26.3	0.605	1047	20	49.488	473
474	C16H10	PYRENE	278.350			750.0	13.6				79.131	474
475	C16H12	N-PHENYLNAPHTHALENE	224.432	4.1	284.8	717.0	13.4				50.409	475
476	C16H22O4	DIBUTYL-O-PHTHALATE	224.432	63.0	348.5	791.0	19.0	0.946	828	10	50.451	476
477	C16H32	N-DECYL-CYCLOHEXANE	226.448	17.8	286.8	717.0	14.2		773	20	66.992	477
478	C16H32	I-HEXADECANE	226.448			717.0	14.2				51.246	478
479	C16H32	PALMYIC ACID	238.459			750.0	13.0		848	54	52.628	479
480	C16H34	N-HEXADECANE	238.459	53.8	310.9	736.0	14.2	1.000	778	20	60.709	480
481	C17H34	N-DODECYL-CYCLOPENTANE	256.474	21.8	302.0	733.0	13.2				52.921	481
482	C17H34	HEPTADECANOL	228.294	255.0	448.0	993.6	23.9	0.736				482
483	C17H36	N-HEPTADECANE	230.310	56.8	331.8	891.0	35.1	0.769				483
484	C18H12	CHRYSENE	230.310	86.8	364.8	924.8	33.2	0.779				484
485	C18H14	O-TERPHENYL	230.310	211.8	375.8	926.0	17.0	1.035	893	20	68.131	485
486	C18H14	M-TERPHENYL	230.310	13.3	362.3	797.0	11.3		889	20	54.303	486
487	C18H14	P-TERPHENYL	282.469	17.6	325.4	797.0	12.1	1.054	844	70	70.049	487
488	C18H14O2	OLEIC ACID	252.486	70.1	371.9	810.0	12.1		889	20	54.345	488
489	C18H36	I-OCTADECANE	252.486	28.1	316.3	745.0	14.2				70.049	489
490	C18H36	N-TRIDECYL-CYCLOPENTANE	254.502	57.8	334.8	747.0	14.2				54.512	490
491	C18H36	STEARIC ACID	270.501			772.0	11.1				56.019	491
492	C18H36O2	N-OCTADECANOL	266.513	31.8	325.9	756.0	11.1		789	32	56.061	492
493	C18H36O	I-OCTADECANE	266.513			756.0	11.1				56.061	493
494	C19H36	N-TETRADECYL-CYCLOPENTANE	286.529			760.0	10.2					494
495	C19H40	N-NONADECANE				760.0	10.2					495
496	C19H40	N-NONADECANE				760.0	10.2					496
497	C19H40	N-NONADECANE				760.0	10.2					497
498	C19H40	N-NONADECANE				760.0	10.2					498
499	C19H40	N-NONADECANE				760.0	10.2					499
500	C19H40	N-NONADECANE				760.0	10.2					500





APPENDIX E

Conversion Factors for Some Common SI Units

* An asterisk (*) denotes an exact relationship.

Length	*1 in.	: 25.4 mm	
	*1 ft	: 0.3048 m	
	*1 yd	: 0.9144 m	
	1 mile	: 1.6093 km	
	*1 Å (angstrom)	: 10^{-10} m	
Time	*1 min	: 60 s	
	*1 h	: 3.6 ks	
	*1 day	: 86.4 ks	
	1 year	: 31.5 Ms	
	*1 in. ²	: 645.16 mm ²	
Area	1 ft ²	: 0.092903 m ²	
	1 yd ²	: 0.83613 m ²	
	1 acre	: 4046.9 m ²	
	1 mile ²	: 2.590 km ²	
	1 in. ³	: 16.387 cm ³	
Volume	1 ft ³	: 0.02832 m ³	
	1 yd ³	: 0.76453 m ³	
	1 UK gal	: 4546.1 cm ³	
	1 US gal	: 3785.4 cm ³	
	1 oz	: 28.352 g	
Mass	*1 lb	: 0.45359237 kg	
	1 cwt	: 50.8023 kg	
	1 ton	: 1016.06 kg	
	1 pdl	: 0.13826 N	
	1 lbf	: 4.4482 N	
Force	1 kgf	: 9.8067 N	
	1 tonf	: 9.9640 kN	
	*1 dyn	: 10^{-5} N	
	Temperature difference	*1 deg F (deg R)	: $\frac{5}{9}$ deg C (deg K)
	Energy (work, heat)	1 ft lbf	: 1.3558 J
1 ft pdl		: 0.04214 J	
*1 cal (internat. table)		: 4.1868 J	
1 erg		: 10^{-7} J	
1 Btu		: 1.05506 kJ	
1 hp h		: 2.6845 MJ	
*1 kW h		: 3.6 MJ	
1 therm		: 105.51 MJ	
1 thermie		: 4.1855 MJ	
Calorific value (volumetric)		1 Btu/ft ³	: 37.259 kJ/m ³

Velocity	1 ft/s	: 0.3048 m/s
	1 mile/h	: 0.44704 m/s
Volumetric flow	1 ft ³ /s	: 0.028316 m ³ /s
	1 ft ³ /h	: 7.8658 cm ³ /s
	1 UK gal/h	: 1.2628 cm ³ /s
	1 US gal/h	: 1.0515 cm ³ /s
	1 lb/h	: 0.12600 g/s
Mass flow	1 ton/h	: 0.28224 kg/s
	1 lb/in. ²	: 703.07 kg/m ²
Mass per unit area	1 lb/ft ²	: 4.8824 kg/m ²
	1 ton/sq mile	: 392.30 kg/km ²
	1 lb/in. ³	: 27.680 g/cm ³
Density	1 lb/ft ³	: 16.019 kg/m ³
	1 lb/UK gal	: 99.776 kg/m ³
	1 lb/US gal	: 119.83 kg/m ³
	1 lbf/in. ²	: 6.8948 kN/m ²
	1 tonf/in. ²	: 15.444 MN/m ²
Pressure	1 lbf/ft ²	: 47.880 N/m ²
	*1 standard atm	: 101.325 kN/m ²
	*1 atm (1 kgf/cm ²)	: 98.0665 kN/m ²
	*1 bar	: 10^5 N/m ²
	1 ft water	: 2.9891 kN/m ²
	1 in. water	: 249.09 N/m ²
	1 in. Hg	: 3.3864 kN/m ²
	1 mmHg (1 torr)	: 133.32 N/m ²
	1 hp (British)	: 745.70 W
	1 hp (metric)	: 735.50 W
Power (heat flow)	1 erg/s	: 10^{-7} W
	1 ft lbf/s	: 1.3558 W
	1 Btu/h	: 0.29307 W
	1 ton of refrigeration	: 3516.9 W
	1 lb ft ²	: 0.042140 kg m ²
	1 lb ft/s	: 0.13826 kg m/s
	1 lb ft ² /s	: 0.042140 kg m ² /s
	1 P (Poise)	: 0.1 N [] s/m ²
	1 lb/ft h	: 0.41338 mN s/m ²
	1 lb/ft s	: 1.4882 N s/m ²
Viscosity, kinematic	*1 S (Stokes)	: 10^{-4} m ² /s
	1 ft ² /h	: 0.25806 cm ² /s
	1 erg/cm ²	: 10^{-3} J/m ²
Surface energy (surface tension)	(1 dyn/cm)	: (10 ⁻³ N/m)
	1 lb/h ft ²	: 1.3562 g/s m ²
Mass flux density	1 Btu/h ft ²	: 3.1546 W/m ²
Heat flux density	*1 kcal/h m ²	: 1.163 W/m ²
Heat transfer coefficient	1 Btu/h ft ² F	: 5.6783 W/m ² K
	Specific enthalpy (latent heat, etc.)	*1 Btu/lb
Specific heat capacity Thermal conductivity	*1 Btu/lb °F	: 4.1868 kJ/kg K
	1 Btu/h ft °F	: 1.7307 W/m K
	1 kcal/h m °C	: 1.163 W/m K

from MULLIN, J. W.; *The Chemical Engineer* No. 211 (Sept. 1967), 176.
SI units in chemical engineering.)

Where temperature difference is involved K = °C.

APPENDIX 1

(4)

Conversion Factors and
Constants of Nature

To convert from	To	Multiply by ¹
acre	ft ²	43,560*
	m ²	4,046.85
atm	N/m ²	1.01325* × 10 ⁵
	lb _f /in. ²	14.696
Avogadro's number	particles/g mol	6.022169 × 10 ²³
	ft ³	5.6146
bbl (petroleum)	gal (U.S.)	42*
	m ³	0.15899
bar	N/m ²	1* × 10 ⁵
	lb _f /in. ²	14.504
Boltzmann's constant	J/K	1.380622 × 10 ⁻²³
	cal _{IT}	251.996
Btu	ft·lb _f	778.17
	J	1,055.06
Btu/lb	kWh	2.9307 × 10 ⁻⁴
	cal _{IT} /g	0.55556
Btu/lb·°F	cal _{IT} /g·°C	1*
Btu/ft ² ·h	W/m ²	3.1546
Btu/ft ² ·h·°F	W/m ² ·°C	5.6783
	kcal/m ² ·h·K	4.882
Btu·ft/ft ² ·h·°F	W·m/m ² ·°C	1.73073
	kcal/m·h·K	1.488
cal _{IT}	Btu	3.9683 × 10 ⁻³
	ft·lb _f	3.0873
cal	J	4.1868*
	J	4.184*
cm	in.	0.39370
	ft	0.0328084
cm ³	ft ³	3.531467 × 10 ⁻³
	gal (U.S.)	2.64172 × 10 ⁻⁴

(Continue)

APPENDIX 1: Conversion Factors and Constants of Nature*



To convert from	To	Multiply by [†]
cP (centipoise)	kg/m·s	$1^* \times 10^{-3}$
	lb/ft·h	2.4191
	lb/ft·s	6.7197×10^{-4}
cSt (centistoke)	m ² /s	$1^* \times 10^{-6}$
faraday	C/g mol	9.648670×10^4
ft	m	0.3048*
ft·lb _f	Btu	1.2851×10^{-3}
	cal _{IT}	0.32383
	J	1.35582
ft·lb _f /s	Btu/h	4.6262
	hp	1.81818×10^{-3}
ft ² /h	m ² /s	2.581×10^{-5}
	cm ² /s	0.2581
ft ³	m ³	0.0283168
	gal (U.S.)	7.48052
ft ³ ·atm	L	28.31684
	Btu	2.71948
	cal _{IT}	685.29
	J	2.8692×10^3
ft ³ /s	gal (U.S.)/min	448.83
gal (U.S.)	ft ³	0.13368
	in. ³	231*
gas law constant, R, see Table 1.2, p. 11		
gravitational constant	N·m ² /kg ²	6.673×10^{-11}
gravity acceleration, standard	m/s ²	9.80665*
h	min	60*
	s	3,600*
hp	Btu/h	2,544.43
	kW	0.74624
hp/1,000 gal	kW/m ³	0.197
in.	cm	2.54*
in. ³	cm ³	16.3871
J	erg	$1^* \times 10^7$
	ft·lb _f	0.73756
kg	lb	2.20462
kWh	Btu	3,412.1
L	m ³	$1^* \times 10^{-3}$
lb	kg	0.45359237*
lb/ft ³	kg/m ³	16.018
	g/cm ³	0.016018
lb _f /in. ²	N/m ²	6.89473×10^3
lb mol/ft ² ·h	kg mol/m ² ·s	1.3562×10^{-3}
	g mol/cm ² ·s	1.3562×10^{-4}
light, speed of	m/s	2.997925×10^8
m	ft	3.280840
	in.	39.3701
m ³	ft ³	35.3147
N	gal (U.S.)	264.17
	dyn	$1^* \times 10^5$
N/m ²	lb _f	0.22481
	lb _f /in. ²	1.4503×10^{-4}

(Continued)

APPENDIX 1: Conversion Factors and Constants of Nature

42

To convert from	To	Multiply by [†]
Planck's constant	J·s	6.626196×10^{-34}
proof (U.S.)	percent alcohol by volume	0.5
ton (long)	kg	1,016
	lb	2,240*
ton (short)	lb	2,000*
t (metric)	kg	1,000*
	lb	2,204.6
	ft	3*
yd	m	0.9144*

[†]Values that end in an asterisk are exact, by definition.

APPENDIX 2

Dimensionless Groups



Symbol	Name	Definition
Bi	Biot number	$\frac{hs}{k}$ for slab
		$\frac{hr_m}{k}$ for cylinder or sphere
C_D	Drag coefficient	$\frac{2F_{Dc}}{\rho u_0^2 A_p}$
Fo	Fourier number	$\frac{\alpha t}{r^2}$
Fr	Froude number	$\frac{u^2}{gL}$
f	Fanning friction factor	$\frac{\Delta p_{sc} D}{2L\rho \bar{V}^2}$
Gr	Grashof number	$\frac{L^3 \rho^2 \beta g \Delta T}{\mu^2}$
Gz	Graetz number	$\frac{\dot{m} c_p}{kL}$
Gz'	Graetz number for mass transfer	$\frac{\dot{m}}{\rho D_v L}$
j_H	Heat-transfer factor	$\frac{h}{c_p G} \left(\frac{c_p \mu}{k} \right)^{2/3} \left(\frac{\mu_w}{\mu} \right)^{0.14}$
j_M	Mass-transfer factor	$\frac{k \bar{M}}{G} \left(\frac{\mu}{D_v \rho} \right)^{2/3}$

(Continued)

Symbol	Name	Definition
Ma	Mach number	$\frac{u}{a}$
N_{Ae}	Aeration number	$\frac{q_g}{n D_a^3}$
N_P	Power number	$\frac{P_c}{\rho n^3 D^5}$
N_Q	Flow number	$\frac{q}{n D_a^3}$
Nu	Nusselt number	$\frac{hD}{k}$
Pe	Peclet number	$\frac{D\bar{V}}{\alpha}$ or $\frac{Du_o}{D_v}$
Pr	Prandtl number	$\frac{c_p \mu}{k}$
Re	Reynolds number	$\frac{DG}{\mu}$
N_s	Separation number	$\frac{u_1 u_0}{g D_p}$
Sc	Schmidt number	$\frac{\mu}{D_v \rho}$
Sh	Sherwood number	$\frac{k_c D}{D_v}$
We	Weber number	$\frac{D\rho \bar{V}^2}{\sigma}$

Properties of Saturated Steam and Water†



Temperature <i>T</i> , °F	Vapor pressure <i>p_s</i> , lb _f /in. ²	Specific volume, ft ³ /lb		Enthalpy, Btu/lb		
		Liquid <i>v_x</i>	Saturated vapor <i>v_y</i>	Liquid <i>H_x</i>	Vaporization <i>λ</i>	Saturated vapor <i>H_y</i>
32	0.08859	0.016022	3.305	0	1,075.4	1,075.4
35	0.09992	0.016021	2,948	3.00	1,073.7	1,076.7
40	0.12166	0.016020	2,445	8.02	1,070.9	1,078.9
45	0.14748	0.016021	2,037	13.04	1,068.1	1,081.1
50	0.17803	0.016024	1,704.2	18.06	1,065.2	1,083.3
55	0.2140	0.016029	1,431.4	23.07	1,062.4	1,085.5
60	0.2563	0.016035	1,206.9	28.08	1,059.6	1,087.7
65	0.3057	0.016042	1,021.5	33.09	1,056.8	1,089.9
70	0.3632	0.016051	867.7	38.09	1,054.0	1,092.0
75	0.4300	0.016061	739.7	43.09	1,051.1	1,094.2
80	0.5073	0.016073	632.8	48.09	1,048.3	1,096.4
85	0.5964	0.016085	543.1	53.08	1,045.5	1,098.6
90	0.6988	0.016099	467.7	58.07	1,042.7	1,100.7
95	0.8162	0.016114	404.0	63.06	1,039.8	1,102.9
100	0.9503	0.016130	350.0	68.05	1,037.0	1,105.0
110	1.2763	0.016166	265.1	78.02	1,031.4	1,109.3
120	1.6945	0.016205	203.0	88.00	1,025.5	1,113.5
130	2.225	0.016247	157.17	97.98	1,019.8	1,117.8
140	2.892	0.016293	122.88	107.96	1,014.0	1,121.9
150	3.722	0.016343	96.99	117.96	1,008.1	1,126.1
160	4.745	0.016395	77.23	127.96	1,002.2	1,130.1
170	5.996	0.016450	62.02	137.97	996.2	1,134.2
180	7.515	0.016509	50.20	147.99	990.2	1,138.2
190	9.343	0.016570	40.95	158.03	984.1	1,142.1
200	11.529	0.016634	33.63	168.07	977.9	1,145.9
210	14.125	0.016702	27.82	178.14	971.6	1,149.7
212	14.698	0.016716	26.80	180.16	970.3	1,150.5

(Continued)

Temperature <i>T</i> , °F	Vapor pressure <i>p_s</i> , lb _f /in. ²	Specific volume, ft ³ /lb		Enthalpy, Btu/lb		
		Liquid <i>v_x</i>	Saturated vapor <i>v_y</i>	Liquid <i>H_x</i>	Vaporization <i>λ</i>	Saturated vapor <i>H_y</i>
220	17.188	0.016772	23.15	188.22	965.3	1,153.5
230	20.78	0.016845	19.386	198.32	958.8	1,157.1
240	24.97	0.016922	16.327	208.44	952.3	1,160.7
250	29.82	0.017001	13.826	218.59	945.6	1,164.2
260	35.42	0.017084	11.768	228.76	938.8	1,167.6
270	41.85	0.017170	10.066	238.95	932.0	1,170.9
280	49.18	0.017259	8.650	249.18	924.9	1,174.1
290	57.53	0.017352	7.467	259.44	917.8	1,177.2
300	66.98	0.017448	6.472	269.73	910.4	1,180.2
310	77.64	0.017548	5.632	280.06	903.0	1,183.0
320	89.60	0.017652	4.919	290.43	895.3	1,185.8
340	117.93	0.017872	3.792	311.30	879.5	1,190.8
350	134.53	0.017988	3.346	321.80	871.3	1,193.1
360	152.92	0.018108	2.961	332.35	862.9	1,195.2
370	173.23	0.018233	2.628	342.96	854.2	1,197.2
380	195.60	0.018363	2.339	353.62	845.4	1,199.0
390	220.2	0.018498	2.087	364.34	836.2	1,200.6
400	247.1	0.018638	1.8661	375.12	826.8	1,202.0
410	276.5	0.018784	1.6726	385.97	817.2	1,203.1
420	308.5	0.018936	1.5024	396.89	807.2	1,204.1
430	343.3	0.019094	1.3521	407.89	796.9	1,204.8
440	381.2	0.019260	1.2192	418.98	786.3	1,205.3
450	422.1	0.019433	1.1011	430.2	775.4	1,205.6

†Abstracted from *Steam Tables*, by Joseph H. Keenan, Frederick G. Keyes, Philip G. Hill, and Joan G. Moore, John Wiley & Sons, New York, 1969, with the permission of the publisher.

Latent heat of vapor is defined as the difference in enthalpy between a fixed mass of vapor and same mass of liquid.

APPENDIX 5



Tyler Standard Screen Scale

This screen scale has as its base an opening of 0.0029 in., which is the opening in 200-mesh 0.0021-in. wire, the standard sieve, as adopted by the National Bureau of Standards.

Mesh	Clear opening, in.	Clear opening, mm	Approximate opening, in.	Wire diameter, in.
	1.050	26.67	1	0.148
†	0.883	22.43	$\frac{7}{8}$	0.135
	0.742	18.85	$\frac{3}{4}$	0.135
†	0.624	15.85	$\frac{5}{8}$	0.120
	0.525	13.33	$\frac{1}{2}$	0.105
†	0.441	11.20	$\frac{7}{16}$	0.105
	0.371	9.423	$\frac{1}{8}$	0.092
2½†	0.312	7.925	$\frac{5}{16}$	0.088
3	0.263	6.680	$\frac{1}{4}$	0.070
3½†	0.221	5.613	$\frac{7}{32}$	0.065
4	0.185	4.699	$\frac{3}{16}$	0.065
5†	0.156	3.962	$\frac{5}{32}$	0.044
6	0.131	3.327	$\frac{1}{8}$	0.036
7†	0.110	2.794	$\frac{7}{64}$	0.0328
8	0.093	2.362	$\frac{1}{32}$	0.032
9†	0.078	1.981	$\frac{3}{64}$	0.033
10	0.065	1.651	$\frac{1}{16}$	0.035
12†	0.055	1.397		0.028
14	0.046	1.168	$\frac{3}{64}$	0.025
16†	0.0390	0.991		0.0235
20	0.0328	0.833	$\frac{1}{32}$	0.0172
24†	0.0276	0.701		0.0141
28	0.0232	0.589		0.0125
32†	0.0195	0.495		0.0118
35	0.0164	0.417	$\frac{1}{64}$ <None>	0.0122
42†	0.0138	0.351		0.0100
48	0.0116	0.295		0.0092
60†	0.0097	0.246		0.0070
65	0.0082	0.208		0.0072
80†	0.0069	0.175		0.0056
100	0.0058	0.147		0.0042
115†	0.0049	0.124		0.0038
150	0.0041	0.104		0.0026
170†	0.0035	0.088		0.0024
200	0.0029	0.074		0.0021
270	0.0021	0.053		
325	0.0017	0.044		

†These screens, for closer sizing, are inserted between the sizes usually considered as the standard series. With the inclusion of these screens the ratio of diameters of openings in two successive screens is $\frac{1}{\sqrt{2}}$.

APPENDIX 6

Properties of Liquid Water

Temperature T , °F	Viscosity [†] μ , cP	Thermal conductivity [‡] k , Btu/ft·h·°F	Density [§] ρ , lb/ft ³	$\psi_T = \left(\frac{k^3 \rho^2 g}{\mu^2}\right)^{1/3}$
32	1.794	0.320	62.42	1,410
40	1.546	0.326	62.43	1,590
50	1.310	0.333	62.42	1,810
60	1.129	0.340	62.37	2,050
70	0.982	0.346	62.30	2,290
80	0.862	0.352	62.22	2,530
90	0.764	0.358	62.11	2,780
100	0.682	0.362	62.00	3,020
120	0.559	0.371	61.71	3,530
140	0.470	0.378	61.38	4,030
160	0.401	0.384	61.00	4,530
180	0.347	0.388	60.58	5,020
200	0.305	0.392	60.13	5,500
220	0.270	0.394	59.63	5,960
240	0.242	0.396	59.10	6,420
260	0.218	0.396	58.53	6,830
280	0.199	0.396	57.94	7,210
300	0.185	0.396	57.31	7,510

[†]From *International Critical Tables*, vol. 5, McGraw-Hill Book Company, New York, 1929, p. 10.

[‡]From E. Schmidt and W. Sellschopp, *Forsch. Geb. Ingenieurw.*, 3:277 (1932).

[§]Calculated from J. H. Keenan and F. G. Keyes, *Thermodynamic Properties of Steam*, John Wiley & Sons., Inc., New York, 1937.

Viscosities of Liquids†



No.	Liquid	X	Y	No.	Liquid	X	Y
63	Sodium hydroxide, 50%	3.2	25.8	70	Toluene	13.7	10.4
64	Sulfur dioxide	15.2	7.1	71	Trichloroethylene	14.8	10.5
65	Sulfuric acid, 98%	7.0	24.8	72	Vinyl acetate	14.0	8.8
66	Sulfuric acid, 60%	10.2	21.3	73	Water	10.2	13.0
67	Tetrachloroethane	11.9	15.7	74	<i>o</i> -Xylene	13.5	12.1
68	Tetrachloroethylene	14.2	12.7	75	<i>m</i> -Xylene	13.9	10.6
69	Titanium tetrachloride	14.4	12.3	76	<i>p</i> -Xylene	13.9	10.9

Coordinates for use with figure on next page.

†By permission, from J. H. Perry (ed.), *Chemical Engineers' Handbook*, 5th ed., pp. 3-212 and 3-213. Copyright © 1973, McGraw-Hill Book Company, New York.

No.	Liquid	X	Y	No.	Liquid	X	Y
1	Acetaldehyde	15.2	4.8	32	Ethyl chloride	14.8	6.0
2	Acetic acid, 100%	12.1	14.2	33	Ethyl ether	14.5	5.3
3	Acetic anhydride	12.7	12.8	34	Ethyl formate	14.2	8.4
4	Acetone, 100%	14.5	7.2	35	Ethyl iodide	14.7	10.3
5	Ammonia, 100%	12.6	2.0	36	Ethylene glycol	6.0	23.6
6	Ammonia, 26%	10.1	13.9	37	Formic acid	10.7	15.8
7	Amyl acetate	11.8	12.5	38	Freon-12	16.8	5.6
8	Amyl alcohol	7.5	18.4	39	Glycerol, 100%	2.0	30.0
9	Aniline	8.1	18.7	40	Glycerol, 50%	6.9	19.6
10	Anisole	12.3	13.5	41	Heptane	14.1	8.4
11	Benzene	12.5	10.9	42	Hexane	14.7	7.0
12	Biphenyl	12.0	18.3	43	Hydrochloric acid, 31.5%	13.0	16.6
13	Brine, CaCl ₂ , 25%	6.6	15.9	44	Isobutyl alcohol	7.1	18.0
14	Brine, NaCl, 25%	10.2	16.6	45	Isopropyl alcohol	8.2	16.0
15	Bromine	14.2	13.2	46	Kerosene	10.2	16.9
16	Butyl acetate	12.3	11.0	47	Linseed oil, raw	7.5	27.2
17	Butyl alcohol	8.6	17.2	48	Mercury	18.4	16.4
18	Carbon dioxide	11.6	0.3	49	Methanol, 100%	12.4	10.5
19	Carbon disulfide	16.1	7.5	50	Methyl acetate	14.2	8.2
20	Carbon tetrachloride	12.7	13.1	51	Methyl chloride	15.0	3.8
21	Chlorobenzene	12.3	12.4	52	Methyl ethyl ketone	13.9	8.6
22	Chloroform	14.4	10.2	53	Napthalene	7.9	18.1
23	<i>m</i> -Cresol	2.5	20.8	54	Nitric acid, 95%	12.8	13.8
24	Cyclohexanol	2.9	24.3	55	Nitric acid, 60%	10.8	17.0
25	Dichloroethane	13.2	12.2	56	Nitrobenzene	10.6	16.2
26	Dichloromethane	14.6	8.9	57	Nitrotoluene	11.0	17.0
27	Ethyl acetate	13.7	9.1	58	Octane	13.7	10.0
28	Ethyl alcohol, 100%	10.5	13.8	59	Octyl alcohol	6.6	21.1
29	Ethyl alcohol, 95%	9.8	14.3	60	Pentane	14.9	5.2
30	Ethyl alcohol, 40%	6.5	16.6	61	Phenol	6.9	20.8
31	Ethyl benzene	13.2	11.5	62	Sodium	16.4	13.9

(Continued)

APPENDIX 8

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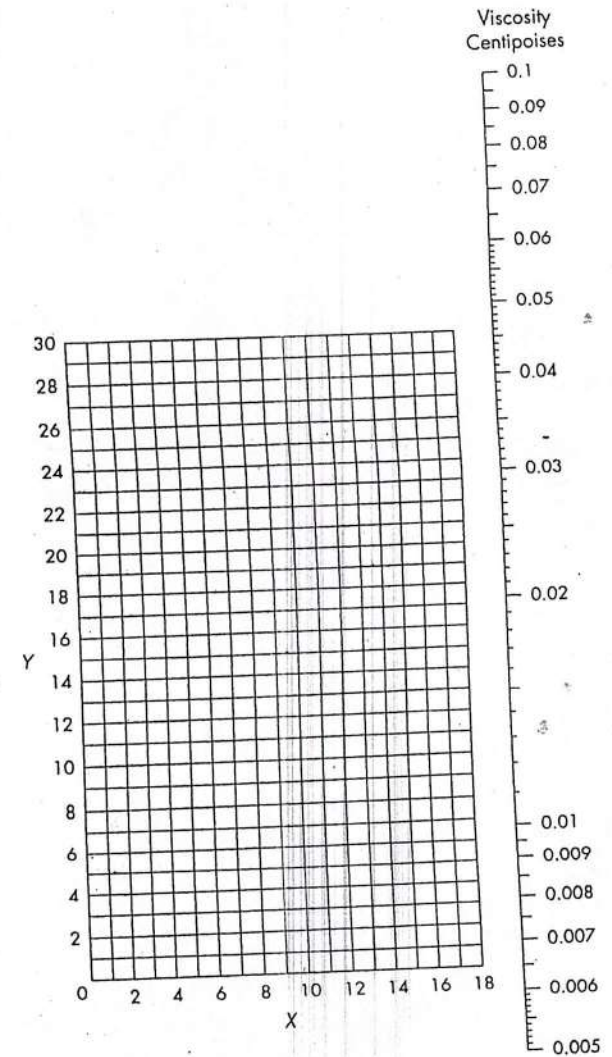
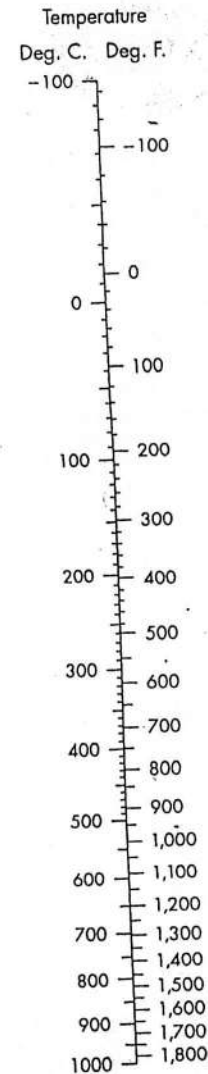
Viscosities of Gases[†]



No.	Gas	X	Y	No.	Gas	X	Y
1	Acetic acid	7.7	14.3	29	Freon-113	11.3	14.0
2	Acetone	8.9	13.0	30	Helium	10.9	20.5
3	Acetylene	9.8	14.9	31	Hexane	8.6	11.8
4	Air	11.0	20.0	32	Hydrogen	11.2	12.4
5	Ammonia	8.4	16.0	33	3H ₂ + N ₂	11.2	17.2
6	Argon	10.5	22.4	34	Hydrogen bromide	8.8	20.9
7	Benzene	8.5	13.2	35	Hydrogen chloride	8.8	18.7
8	Bromine	8.9	19.2	36	Hydrogen cyanide	9.8	14.9
9	Butene	9.2	13.7	37	Hydrogen iodide	9.0	21.3
10	Butylene	8.9	13.0	38	Hydrogen sulfide	8.6	18.0
11	Carbon dioxide	9.5	18.7	39	Iodine	9.0	18.4
12	Carbon disulfide	8.0	16.0	40	Mercury	5.3	22.9
13	Carbon monoxide	11.0	20.0	41	Methane	9.9	15.5
14	Chlorine	9.0	18.4	42	Methyl alcohol	8.5	15.6
15	Chloroform	8.9	15.7	43	Nitric oxide	10.9	20.5
16	Cyanogen	9.2	15.2	44	Nitrogen	10.6	20.0
17	Cyclohexane	9.2	12.0	45	Nitrosyl chloride	8.0	17.6
18	Ethane	9.1	14.5	46	Nitrous oxide	8.8	19.0
19	Ethyl acetate	8.5	13.2	47	Oxygen	11.0	21.3
20	Ethyl alcohol	9.2	14.2	48	Pentane	7.0	12.8
21	Ethyl chloride	8.5	15.6	49	Propane	9.7	12.9
22	Ethyl ether	8.9	13.0	50	Propyl alcohol	8.4	13.4
23	Ethylene	9.5	15.1	51	Propylene	9.0	13.8
24	Fluorine	7.3	23.8	52	Sulfur dioxide	9.6	17.0
25	Freon-11	10.6	15.1	53	Toluene	8.6	12.4
26	Freon-12	11.1	16.0	54	2,3,3-Trimethylbutane	9.5	10.5
27	Freon-21	10.8	15.3	55	Water	8.0	16.0
28	Freon-22	10.1	17.0	56	Xenon	9.3	23.0

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[†]By permission, from J. H. Perry (ed.), *Chemical Engineers' Handbook*, 5th ed., pp.3-210 and 3-211. Copyright © 1973, McGraw-Hill Book Company, New York.



Viscosities of gases and vapors at 1 atm; for coordinates, see table on previous page.

Thermal Conductivities of Various Solids and Insulating Materials[†]



Material	Apparent density ρ , lb/ft ³	Temperature T , °C	Thermal conductivity k , Btu/h · ft ² · (°F/ft)
Asbestos	29	-200	0.043
	36	0	0.087
	36	400	0.129
Bricks			
Alumina	—	1,315	2.7
Building brickwork	—	20	0.4
Carbon	96.7	—	3.0
Fire clay (Missouri)	—	200	0.58
	—	1,000	0.95
	—	1,400	1.02
Kaolin insulating firebrick	19	200	0.050
	19	760	0.113
Silicon carbide, recrystallized	129	600	10.7
	129	1,000	8.0
	129	1,400	6.3
Cardboard, corrugated	—	—	0.37
Concrete			
Clinker	—	—	0.20
Stone	—	—	0.54
1:4 dry	—	—	0.44
Cork, ground	9.4	30	0.025
Glass			
Borosilicate	139	30-75	0.63
Window	—	—	0.3-0.61

(Continued)

Material	Apparent density ρ , lb/ft ³	Temperature T , °C	Thermal conductivity k , Btu/h · ft ² · (°F/ft)
Granite	—	—	1.0-2.3
Ice	57.5	0	1.3
Insulating materials			
Fiberglass batts [‡]	6	20	0.019
	6	150	0.027
	6	200	0.035
	9	20	0.018
	9	150	0.023
	9	20	0.020
Kapok	0.88	20	0.023
Polystyrene foam [§]	1	20	0.020
	2-5	20	0.014
Polyurethane foam [§] (made with fluorocarbon gas)	1.3-3.0	—	0.018
Polyurethane foam [§] (made with CO ₂)	4-8	—	0.018
Wall board	1.3-3.0	—	0.018
	14.8	21	0.028
Magnesia, powdered	49.7	47	0.35
Paper	—	—	0.75
Porcelain	—	200	0.88
Rubber, soft	—	21	0.075-0.092
Snow	34.7	0	0.27
Wood (across grain)			
Oak	51.5	15	0.12
Maple	44.7	50	0.11
Pine, white	34.0	15	0.087
Wood (parallel to grain)			
Pine	34.4	21	0.20

[†]From J. H. Perry (ed.), *Chemical Engineers' Handbook*, 6th ed., McGraw-Hill, New York, p. 3-260, except as noted.

[‡]From *Heat Transfer and Fluid Data Book*, vol. 1, Genium Publishing Corp., Schenectady, NY, 1984, sect. 515.24, p. 1.

[§]From *Modern Plastics Encyclopedia*, vol. 65, no. 11, McGraw-Hill Book Co., New York, 1988, p. 657.

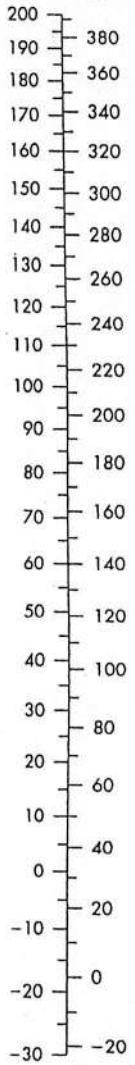
APPENDIX 10

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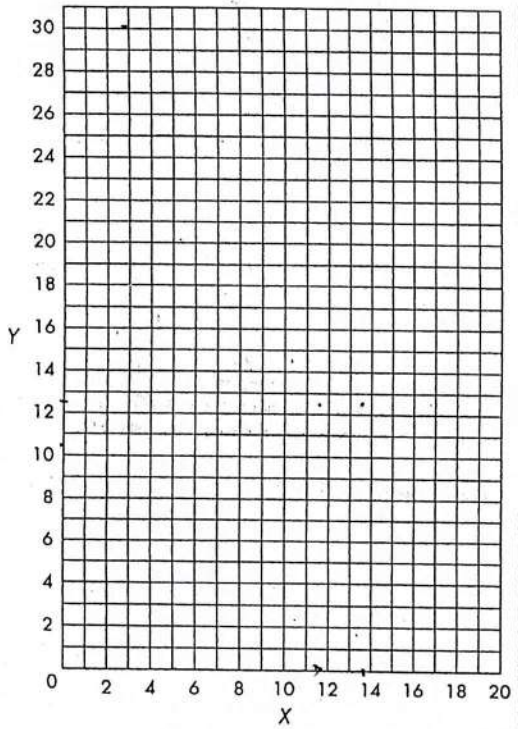
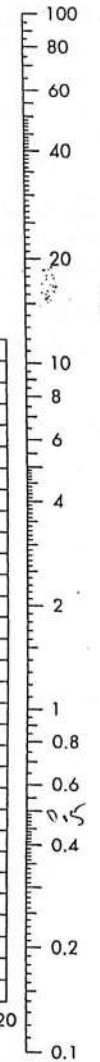
Thermal Conductivities of Metals[†]



Temperature
Deg. C. Deg. F.



Viscosity
Centipoises



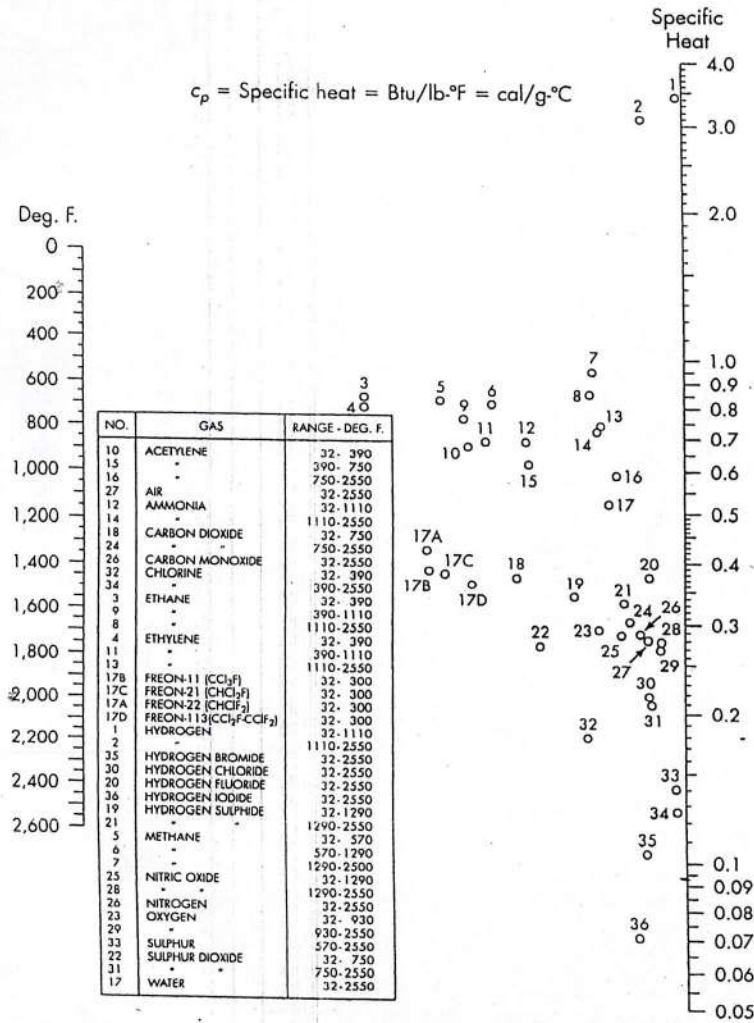
Viscosities of liquids at 1 atm. For coordinates, see table on previous page.

Metal	Thermal conductivity k^{\ddagger}		
	32°F	64°F	212°F
Aluminum	117		119
Antimony	10.6		9.7
Brass (70 copper, 30 zinc)	56		60
Cadmium		53.7	52.2
Copper (pure)	224		218
Gold		169.0	170.0
Iron (cast)	32		30
Iron (wrought)		34.9	34.6
Lead	20		19
Magnesium	92	92	92
Mercury (liquid)	4.8		34
Nickel	36		41.9
Platinum		40.2	238
Silver	242		49
Sodium (liquid)			26
Steel (mild)			25.9
Steel (1% carbon)		26.2	9.4
Steel (stainless, type 304)			9.4
Steel (stainless, type 316)			9.3
Steel (stainless, type 347)			
Tantalum		32	
Tin	36		34
Zinc	65		64

[†]Based on W. H. McAdams, *Heat Transmission*, 3rd ed., McGraw-Hill Book Company, New York, 1954, pp. 445-447.

[‡] k = Btu/ft·h·°F. To convert to W/m·°C, multiply by 1.73073.

Specific Heats of Gases†

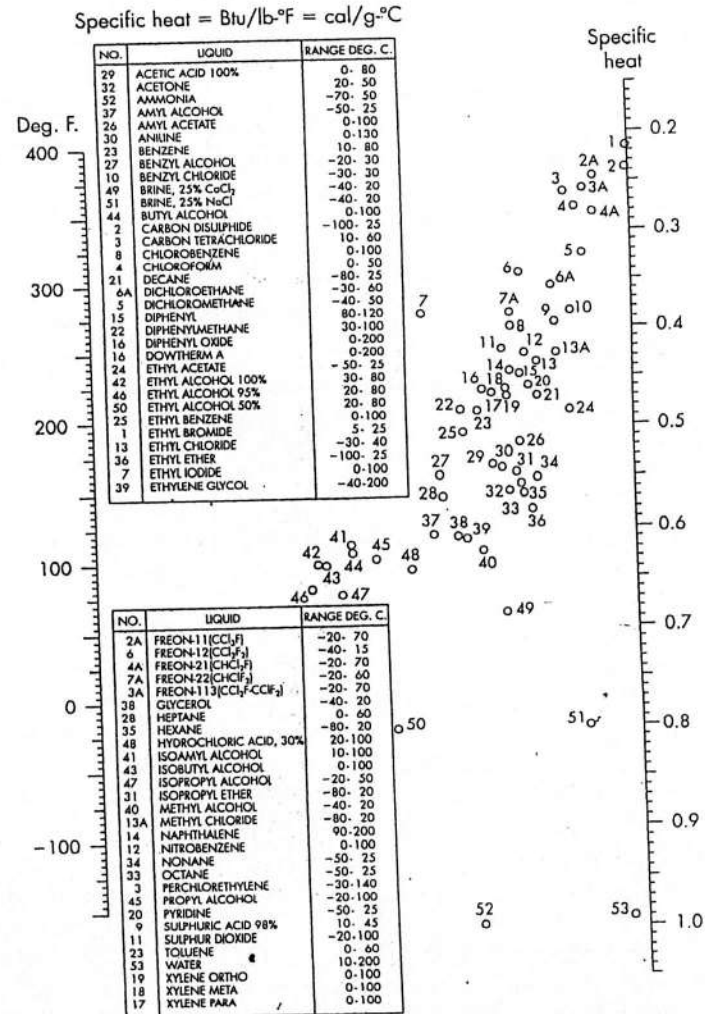


True specific heats c_p of gases and vapors at 1 atm pressure.

†Courtesy of T. H. Chilton.

Specific Heats of Liquids†

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†Courtesy of T. H. Chilton.

APPENDIX 12

Thermal Conductivities of Gases
and Vapors[†]

Substance	Thermal conductivity k^{\ddagger}	
	32°F	212°F
Acetone	0.0057	0.0099
Acetylene	0.0108	0.0172
Air	0.0140	0.0184
Ammonia	0.0126	0.0192
Benzene		0.0103
Carbon dioxide	0.0084	0.0128
Carbon monoxide	0.0134	0.0176
Carbon tetrachloride		0.0052
Chlorine	0.0043	
Ethane	0.0106	0.0175
Ethyl alcohol		0.0124
Ethyl ether	0.0077	0.0131
Ethylene	0.0101	0.0161
Helium	0.0818	0.0988
Hydrogen	0.0966	0.1240
Methane	0.0176	0.0255
Methyl alcohol	0.0083	0.0128
Nitrogen	0.0139	0.0181
Nitrous oxide	0.0088	0.0138
Oxygen	0.0142	0.0188
Propane	0.0087	0.0151
Sulfur dioxide	0.0050	0.0069
Water vapor (at 1 atm abs pressure)		0.0136

[†]Based on W. H. McAdams, *Heat Transmission*, 3rd ed., McGraw-Hill Book Company, New York, 1954, pp. 457-458.

[‡] k = Btu/ft·h·°F. To convert to W/m·°C, multiply by 1.73073.

APPENDIX 13

Thermal Conductivities of Liquids
Other Than Water[†]

(51)

Liquid	Temperature, °F	k^{\ddagger}
Acetic acid	68	0.099
Acetone	86	0.102
Ammonia (anhydrous)	5-86	0.29
Aniline	32-68	0.100
Benzene	86	0.092
<i>n</i> -Butyl alcohol	86	0.097
Carbon bisulfide	86	0.093
Carbon tetrachloride	32	0.107
Chlorobenzene	50	0.083
Ethyl acetate	68	0.101
Ethyl alcohol (absolute)	68	0.105
Ethyl ether	86	0.080
Ethylene glycol	32	0.153
Gasoline	86	0.078
Glycerine	68	0.164
<i>n</i> -Heptane	86	0.081
Kerosene	68	0.086
Methyl alcohol	68	0.124
Nitrobenzene	86	0.095
<i>n</i> -Octane	86	0.083
Sulfur dioxide	5	0.128
Sulfuric acid (90%)	86	0.21
Toluene	86	0.086
Trichloroethylene	122	0.080
<i>o</i> -Xylene	68	0.090

[†]Based on W. H. McAdams, *Heat Transmission*, 3rd ed., McGraw-Hill Book Company, New York, 1954, pp. 455-456.

[‡] k = Btu/ft·h·°F. To convert to W/m·°C, multiply by 1.73073.

Diffusivities and Schmidt Numbers for Gases in Air at 0°C and 1 atm[†]



Gas	Volumetric diffusivity D_{v_i} , ft ² /h [†]	$Sc = \frac{\mu}{\rho D_{v_i}}$
Acetic acid	0.413	1.24
Acetone	0.32 [‡]	1.60
Ammonia	0.836	0.61
Benzene	0.299	1.71
<i>n</i> -Butyl alcohol	0.273	1.88
Carbon dioxide	0.535	0.96
Carbon tetrachloride	0.26 [‡]	1.97
Chlorine	0.43 [‡]	1.19
Chlorobenzene	0.24 [‡]	2.13
Ethane	0.49 [‡]	1.04
Ethyl acetate	0.278	1.84
Ethyl alcohol	0.396	1.30
Ethyl ether	0.302	1.70
Hydrogen	2.37	0.22
Methane	0.74 [‡]	0.69
Methyl alcohol	0.515	1.00
Naphthalene	0.199	2.57
Nitrogen	0.70 [‡]	0.73
<i>n</i> -Octane	0.196	2.62
Oxygen	0.690	0.74
Phosgene	0.31 [‡]	1.65
Propane	0.36 [‡]	1.42
Sulfur dioxide	0.44 [‡]	1.16
Toluene	0.275	1.86
Water vapor	0.853	0.60

[†]By permission, from T. K. Sherwood and R. L. Pigford, *Absorption and Extraction*, 2nd ed., p. 20. Copyright 1952, McGraw-Hill Book Company, New York.

[‡]The value of μ/ρ is that for pure air, 0.512 ft²/h.

[§]Calculated by Eq. (17.28).

^{††}To convert ft²/h to cm²/s, multiply by 0.2581.

Collision Integral and Lennard-Jones Force Constants[†]

(54)

Collision integral Ω_D

$\frac{kT}{\epsilon_{12}}$	Ω_D	$\frac{kT}{\epsilon_{12}}$	Ω_D	$\frac{kT}{\epsilon_{12}}$	Ω_D
0.30	2.662	1.65	1.153	4.0	0.8836
0.35	2.476	1.70	1.140	4.1	0.8788
0.40	2.318	1.75	1.128	4.2	0.8740
0.45	2.184	1.80	1.116	4.3	0.8694
0.50	2.066	1.85	1.105	4.4	0.8652
0.55	1.966	1.90	1.094	4.5	0.8610
0.60	1.877	1.95	1.084	4.6	0.8568
0.65	1.798	2.00	1.075	4.7	0.8530
0.70	1.729	2.1	1.057	4.8	0.8492
0.75	1.667	2.2	1.041	4.9	0.8456
0.80	1.612	2.3	1.026	5.0	0.8422
0.85	1.562	2.4	1.012	6	0.8124
0.90	1.517	2.5	0.9996	7	0.7896
0.95	1.476	2.6	0.9878	8	0.7712
1.00	1.439	2.7	0.9770	9	0.7556
1.05	1.406	2.8	0.9672	10	0.7424
1.10	1.375	2.9	0.9576	20	0.6640
1.15	1.346	3.0	0.9490	30	0.6232
1.20	1.320	3.1	0.9406	40	0.5960
1.25	1.296	3.2	0.9328	50	0.5756
1.30	1.273	3.3	0.9256	60	0.5596
1.35	1.253	3.4	0.9186	70	0.5464
1.40	1.233	3.5	0.9120	80	0.5352
1.45	1.215	3.6	0.9058	90	0.5256
1.50	1.198	3.7	0.8998	100	0.5130
1.55	1.182	3.8	0.8942	200	0.4644
1.60	1.167	3.9	0.8888	400	0.4170

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APPENDIX 16

Prandtl Numbers for Gases
at 1 atm and 100°C†

Gas	$Pr = \frac{c_p \mu}{k}$
Air	0.69
Ammonia	0.86
Argon	0.66
Carbon dioxide	0.75
Carbon monoxide	0.72
Helium	0.71
Hydrogen	0.69
Methane	0.75
Nitric oxide, nitrous oxide	0.72
Nitrogen	0.70
Oxygen	0.70
Water vapor	1.06

†Based on W. H. McAdams, *Heat Transmission*, 3rd ed., McGraw-Hill Book Company, New York, 1954, p. 471.

APPENDIX 17

Prandtl Numbers for Liquids†

Liquid	$Pr = \frac{c_p \mu}{k}$	
	61°F	212°F
Acetic acid	14.5	10.5
Acetone	4.5	2.4
Aniline	69	9.3
Benzene	7.3	3.8
<i>n</i> -Butyl alcohol	43	11.5
Carbon tetrachloride	7.5	4.2
Chlorobenzene	9.3	7.0
Ethyl acetate	6.8	5.6
Ethyl alcohol	15.5	10.1
Ethyl ether	4.0	2.3
Ethylene glycol	350	125
<i>n</i> -Heptane	6.0	4.2
Methyl alcohol	7.2	3.4
Nitrobenzene	19.5	6.5
<i>n</i> -Octane	5.0	3.6
Sulfuric acid (98%)	149	15.0
Toluene	6.5	3.8
Water	7.7	1.5

†Based on W. H. McAdams, *Heat Transmission*, 3rd ed., McGraw-Hill Book Company, New York, 1954, p. 470.

Lennard-Jones force constants

Compound	ϵ/k (K)	σ (Å)
Acetone	560.2	4.600
Acetylene	231.8	4.033
Air	78.6	3.711
Ammonia	558.3	2.900
Argon	93.3	3.542
Benzene	412.3	5.349
Bromine	507.9	4.296
<i>n</i> -butane	310	5.339
<i>i</i> -butane	313	5.341
Carbon dioxide	195.2	3.941
Carbon disulfide	467	4.483
Carbon monoxide	91.7	3.690
Carbon tetrachloride	322.7	5.947
Carbonyl sulfide	336	4.130
Chlorine	316	4.217
Chloroform	340.2	5.389
Cyanogen	348.6	4.361
Cyclohexane	297.1	6.182
Cyclopropane	248.9	4.807
Ethane	215.7	4.443
Ethanol	362.6	4.530
Ethylene	224.7	4.163
Fluorine	112.6	3.357
Helium	10.22	2.551
<i>n</i> -Hexane	339.3	5.949
Hydrogen	59.7	2.827
Hydrogen cyanide	569.1	3.630
Hydrogen chloride	344.7	3.339
Hydrogen iodide	288.7	4.211
Hydrogen sulfide	301.1	3.623
Iodine	474.2	5.160
Krypton	178.9	3.655
Methane	148.6	3.758
Methanol	481.8	3.626
Methylene chloride	356.3	4.898
Methyl chloride	350	4.182
Mercury	750	2.969
Neon	32.8	2.820
Nitric oxide	116.7	3.492
Nitrogen	71.4	3.798
Nitrous oxide	232.4	3.828
Oxygen	106.7	3.467
<i>n</i> -Pentane	341.1	5.784
Propane	237.1	5.118
<i>n</i> -Propyl alcohol	576.7	4.549
Propylene	298.9	4.678
Sulfur dioxide	335.4	4.112
Water	809.1	2.641

¹From J. O. Hirschfelder, C. F. Curtiss, and R. B. Bird, *Molecular Theory of Gases and Liquids*, New York: Wiley, 1954.

(55)

PIPING AND INSTRUMENTATION

(56)

where ΔP_f = pressure drop, N/m²;

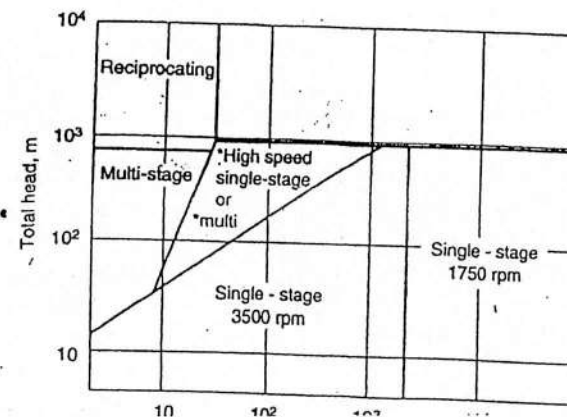
Table 13 Pressure loss in pipe fittings and valves (for turbulent flow)

Fitting or valve	<i>K</i> , number of velocity heads	number of equivalent pipe diameters
45° standard elbow	0.35	
45° long radius elbow	0.2	15
90° standard radius elbow	0.6-0.8	10
90° standard long elbow	0.45	30-40
90° square elbow	1.5	23
Tee-entry from leg	1.2	75
Tee-entry into leg	1.8	60
Union and coupling	0.04	90
Sharp reduction (tank outlet)	0.5	2
Sudden expansion (tank inlet)	1.0	25
Gate valve		50
fully open	0.15	
1/4 open	16	7.5
1/2 open	4	800
3/4 open	1	200
Globe valve, bevel seat		40
fully open	6	
1/2 open	8.5	300
Plug valve - open	0.4	450
		18

The number of equivalent pipe diameters

Table 14 Pipe roughness

Material	Absolute roughness, mm
Drawn tubing	0.0015
Commercial steel pipe	0.046
Cast iron pipe	0.26
Concrete pipe	0.3 to 3.0



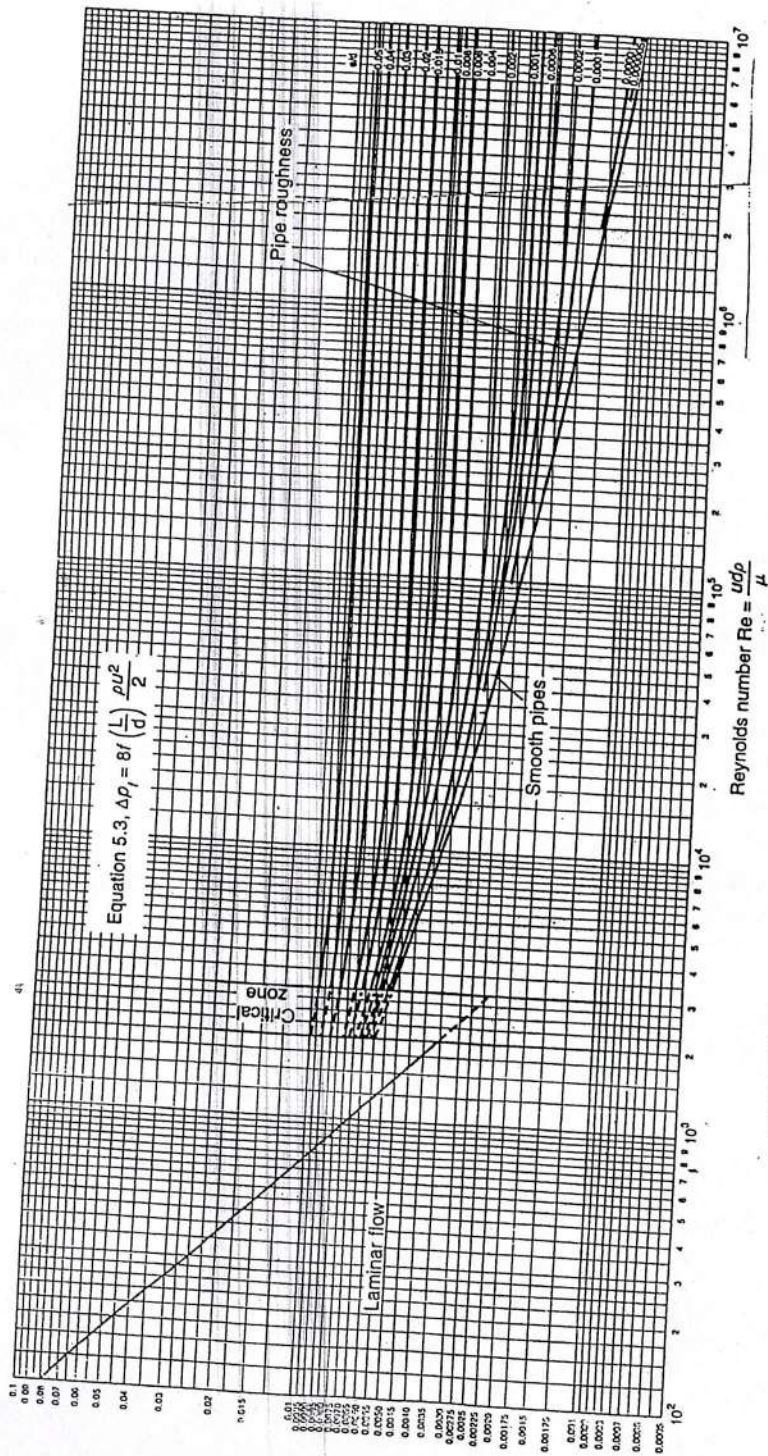


Figure 31 Pipe friction versus Reynolds number and relative roughness



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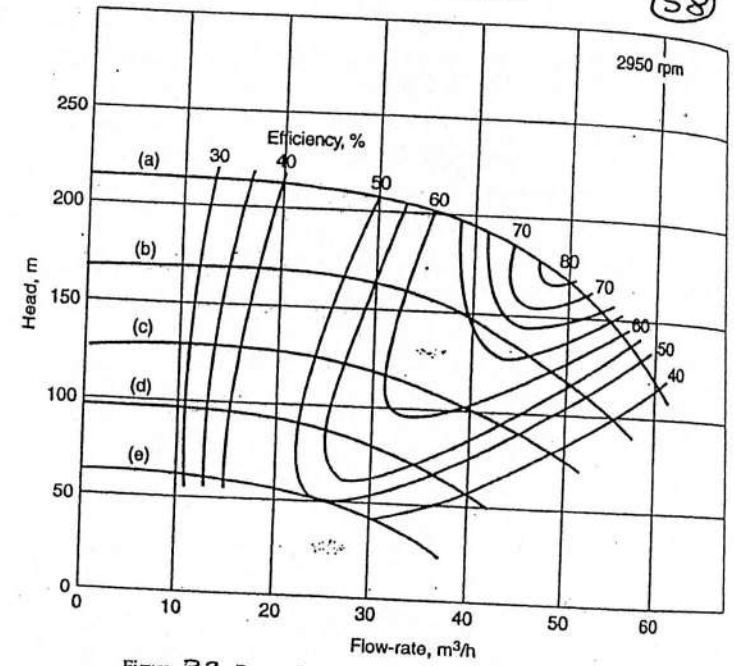


Figure 32 Pump characteristic for a range of impeller sizes
(a) 250 mm (b) 225 mm (c) 200 (d) 175 mm (e) 150 mm.

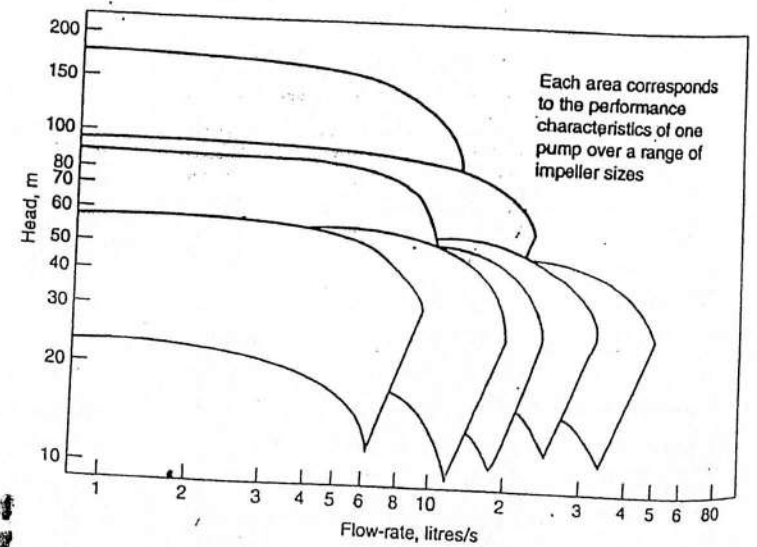


Figure 33 Family of pump curves

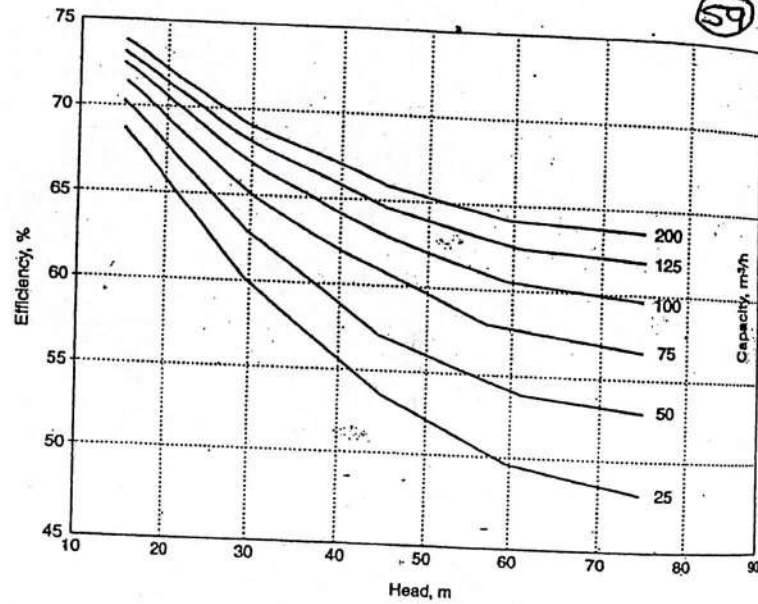


Figure 34 Centrifugal pump efficiency

MATERIALS OF CONSTRUCTION

Table 15 Mechanical properties of common metals and alloys (typical values at room temperature)

	Tensile strength (N/mm ²)	0.1 per cent proof stress (N/mm ²)	Modulus of elasticity (kN/mm ²)	Hardness Brinell	Specific gravity
Mild steel	430	220	210	100-200	7.9
Low alloy steel	420-660	230-460	210	130-200	7.9
Cast iron	140-170	—	140	150-250	7.2
Stainless steel (18Cr, 8Ni)	>540	200	210	160	8.0
Nickel (>99 per cent Ni)	500	130	210	80-150	8.9
Monel	650	170	170	120-250	8.8
Copper (deoxidised)	200	60	110	30-100	8.9
Brass (Admiralty)	400-600	130	115	100-200	8.6
Aluminium (>99 per cent)	80-150	—	70	30	2.7
Invar	400	150	70	100	2.7
Zinc	30	—	15	5	11.3
Titanium	500	350	110	150	4.5



Table 16. PIPE SIZE SELECTION

Typical pipe velocities and allowable pressure drops, which can be used to estimate pipe sizes, are given below:

	Velocity m/s	ΔP kPa/m
Liquids, pumped (not viscous)	1-3	0.5
Liquids, gravity flow	—	0.05
Gases and vapours	15-30	0.02 per cent of line pressure
High-pressure steam, >8 bar	30-60	—

Rase (1953) gives expressions for design velocities in terms of the pipe diameter. His expressions, converted to SI units, are:

Pump discharge	$0.06d + 0.4$ m/s
Pump suction	$0.02d + 0.1$ m/s
Steam or vapour	$0.2d$ m/s

where d is the internal diameter in mm.

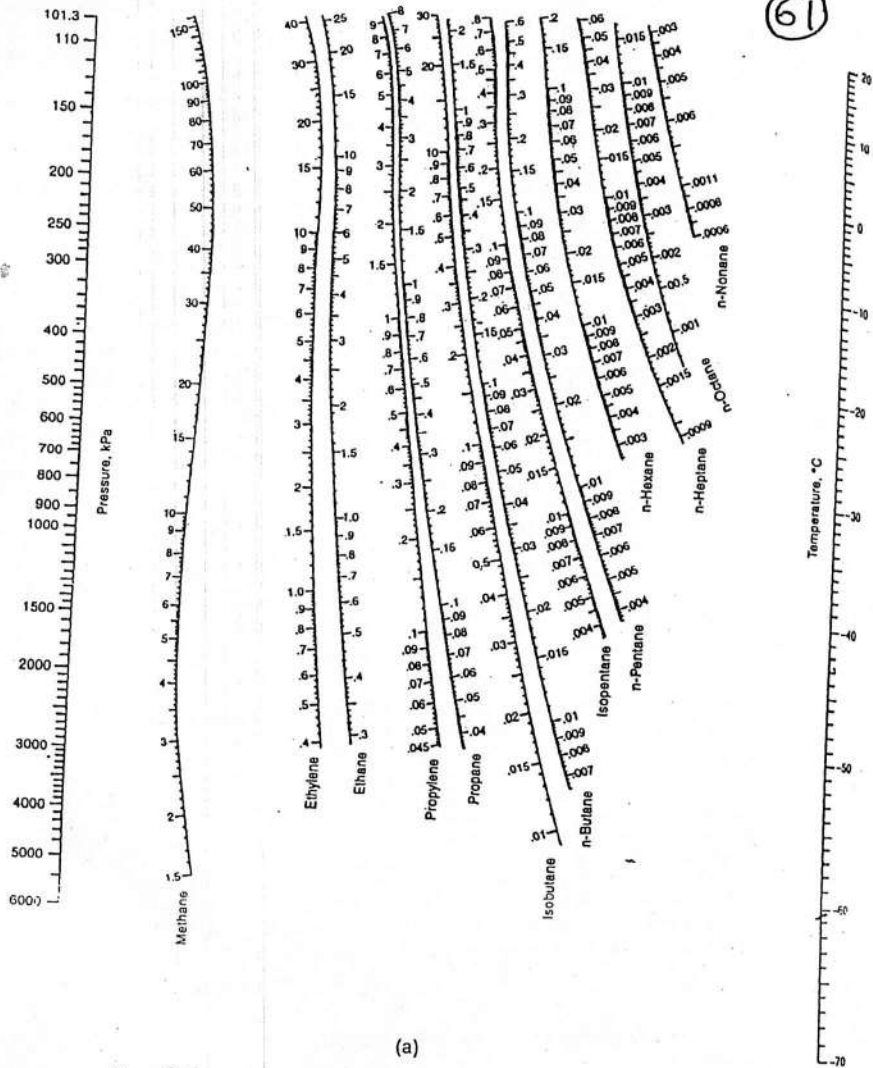
Simpson (1968) gives values for the optimum velocity in terms of the fluid density. His values, converted to SI units and rounded, are:

Fluid density kg/m ³	Velocity m/s
1600	2.4
800	3.0
160	4.9
16	9.4
0.16	18.0
0.016	34.0



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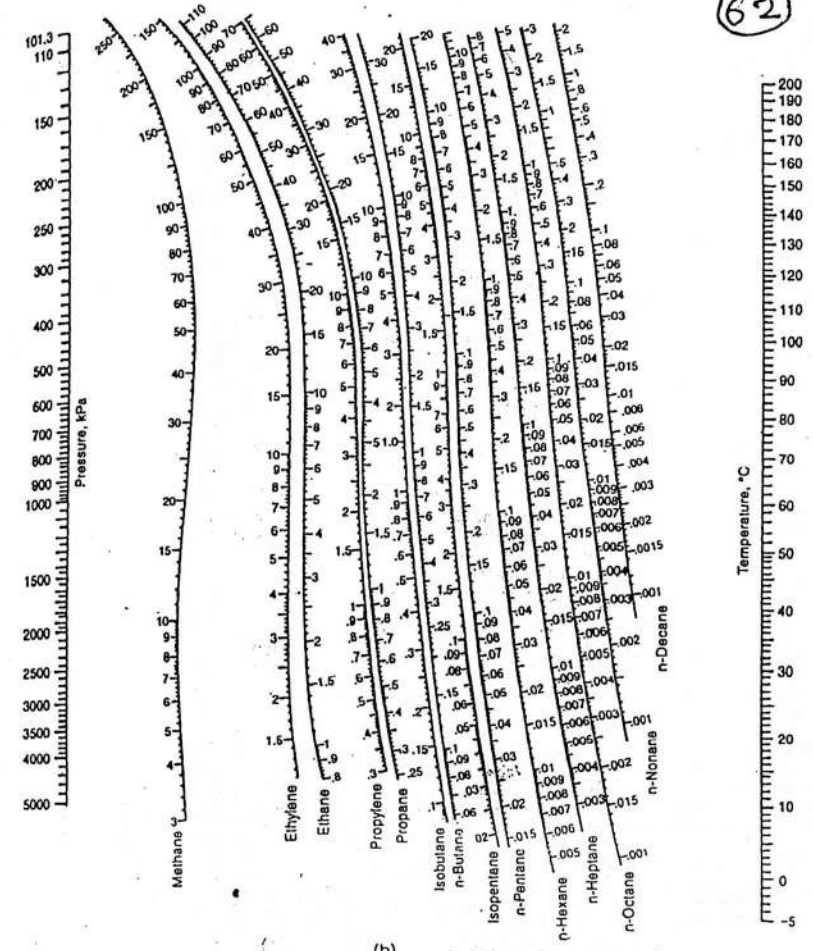


(a)

Figure 35(a) De Priester chart — K -values for hydrocarbons, low temperature.

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(b)

Figure 35(b) De Priester chart — K -values for hydrocarbons, high temperature.

HEAT-TRANSFER EQUIPMENT

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Table 17 Typical overall coefficients

Shell and tube exchangers		
Hot fluid	Cold fluid	U ($W/m^2\text{ }^\circ\text{C}$)
<i>Heat exchangers</i>		
Water	Water	800-1500
Organic solvents	Organic solvents	100-300
Light oils	Light oils	100-400
Heavy oils	Heavy oils	50-300
Gases	Gases	10-50
<i>Coolers</i>		
Organic solvents	Water	250-750
Light oils	Water	350-900
Heavy oils	Water	60-300
Gases	Water	20-300
Organic solvents	Brine	150-500
Water	Brine	600-1200
Gases	Brine	15-250
<i>Heaters</i>		
Steam	Water	1500-4000
Steam	Organic solvents	500-1000
Steam	Light oils	300-900
Steam	Heavy oils	60-450
Steam	Gases	30-300
Dowtherm	Heavy oils	50-300
Dowtherm	Gases	20-200
Flue gases	Steam	30-100
Flue	Hydrocarbon vapours	30-100
<i>Condensers</i>		
Aqueous vapours	Water	1000-1500
Organic vapours	Water	700-1000
Organics (some non-condensables)	Water	500-700
Vacuum condensers	Water	200-500
<i>Vaporisers</i>		
Steam	Aqueous solutions	1000-1500
Steam	Light organics	900-1200
Steam	Heavy organics	600-900
<i>Air-cooled exchangers</i>		
Process fluid		
Water		300-450
Light organics		300-700
Heavy organics		50-150
Gases, 5-10 bar		50-100
10-30 bar		100-300
Condensing hydrocarbons		300-600
<i>Immersed coils</i>		
Coil	Pool	
<i>Natural circulation</i>		
Steam	Dilute aqueous solutions	500-1000
Steam	Light oils	200-300
Steam	Heavy oils	70-150
Water	Aqueous solutions	200-500
Water	Light oils	100-150

(continued overleaf)



CHEMICAL ENGINEERING

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Table 17 (continued)

Immersed coils		
Coil	Pool	U ($W/m^2\text{ }^\circ\text{C}$)
<i>Agitated</i>		
Steam	Dilute aqueous solutions	800-1500
Steam	Light oils	300-500
Water	Heavy oils	200-400
Water	Aqueous solutions	400-700
Water	Light oils	200-300
<i>Jacketed vessels</i>		
Jacket	Vessel	
Steam	Dilute aqueous solutions	500-700
Steam	Light organics	250-500
Water	Dilute aqueous solutions	200-500
Water	Light organics	200-300
<i>Gasketed-plate exchangers</i>		
Hot fluid	Cold fluid	
Light organic	Light organic	2500-5000
Light organic	Viscous organic	250-500
Viscous organic	Viscous organic	100-200
Light organic	Process water	2500-3500
Viscous organic	Process water	250-500
Light organic	Cooling water	2000-4500
Viscous organic	Cooling water	250-450
Condensing steam	Light organic	2500-3500
Condensing steam	Viscous organic	250-500
Process water	Process water	5000-7500
Process water	Cooling water	5000-7000
Dilute aqueous solutions	Cooling water	5000-7000
Condensing steam	Process water	3500-4500

TABLE 18 FLOW AREAS AND EQUIVALENT DIAMETERS IN DOUBLE PIPE EXCHANGERS

Exchanger, IPS	Flow area, in. ²		Annulus, in.	
	Annulus	Pipe	d_e	d_e'
2 × 1½	1.19	1.50	0.915	0.40
2½ × 1½	2.63	1.50	2.02	0.81
3 × 2	2.93	3.35	1.57	0.69
4 × 3	3.14	7.38	1.14	0.53

Table 19 Standard dimensions for steel tubes

Outside diameter (mm)	Wall thickness (mm)				
	1.2	1.6	2.0	2.6	3.2
16	—	—	—	—	—
20	—	1.6	2.0	2.6	—
25	—	1.6	2.0	2.6	3.2
30	—	1.6	2.0	2.6	—

Gas	$\frac{cu}{k}$
Air	0.74
Ammonia	0.78
Carbon dioxide	0.80
Carbon monoxide	0.74
Ethylene	0.83
Hydrogen	0.74
Hydrogen sulfide	0.77
Methane	0.79
Nitrogen	0.74
Oxygen	0.74
Steam	0.78
Sulfur dioxide	0.80

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Table 2.1 Fouling factors (coefficients), typical values

Fluid	Coefficient ($W/m^2 \cdot ^\circ C$)	Factor (resistance) ($m^2 \cdot C/W$)
River water	3000-12,000	0.0003-0.0001
Sea water	1000-3000	0.001-0.0003
Cooling water (towers)	3000-6000	0.0003-0.00017
Towns water (soft)	3000-5000	0.0003-0.0002
Towns water (hard)	1000-2000	0.001-0.0005
Steam condensate	1500-5000	0.00067-0.0002
Steam (oil free)	4000-10,000	0.0025-0.0001
Steam (oil traces)	2000-5000	0.0005-0.0002
Refrigerated brine	3000-5000	0.0003-0.0002
Air and industrial gases	5000-10,000	0.0002-0.0001
Flue gases	2000-5000	0.0005-0.0002
Organic vapours	5000	0.0002
Organic liquids	5000	0.0002
Light hydrocarbons	5000	0.0002
Heavy hydrocarbons	2000	0.0005
Boiling organics	2500	0.0004
Condensing organics	5000	0.0002
Heat transfer fluids	5000	0.0002
Aqueous salt solutions	3000-5000	0.0003-0.0002

TABLE 2.2 TUBE COUNT ENTRY ALLOWANCES

Shell ID, in.	Nozzle, in.
Less than 12	2
12-17 1/4	3
19 1/4-21 1/4	4
23 1/4-29	6
31-37	8
Over 39	10

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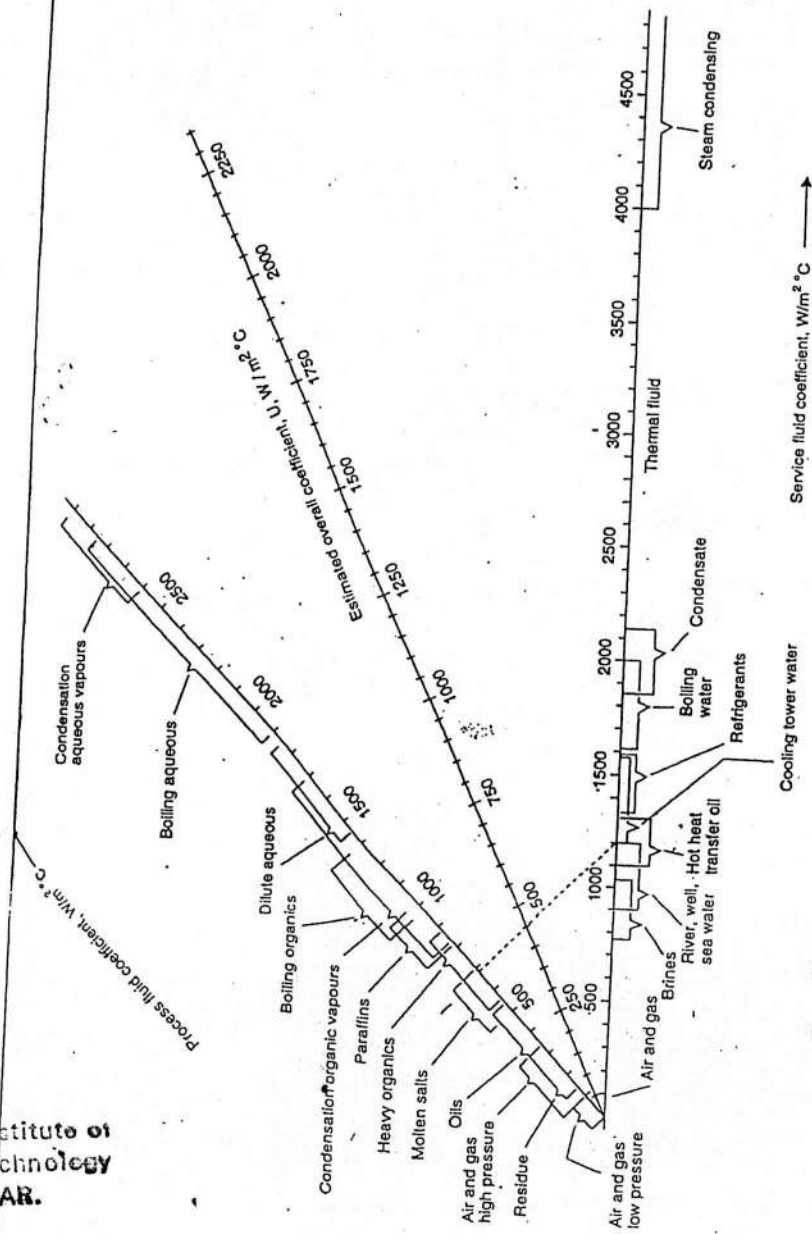


Figure 3.6 Overall coefficients (Join process side duty to service side and read U from centre scale)

HEAT-TRANSFER EQUIPMENT

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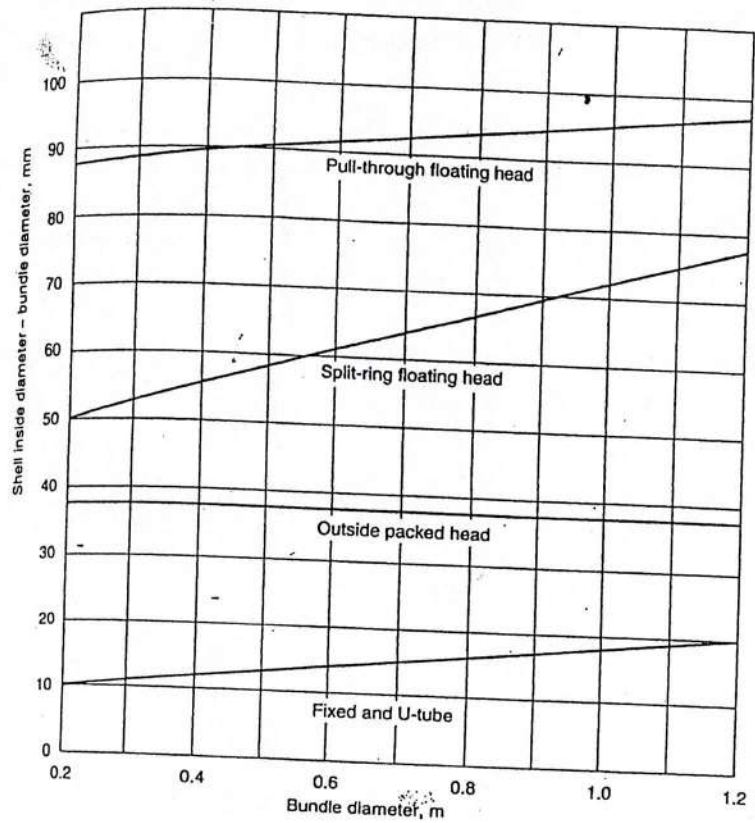


Figure 37 Shell-bundle clearance

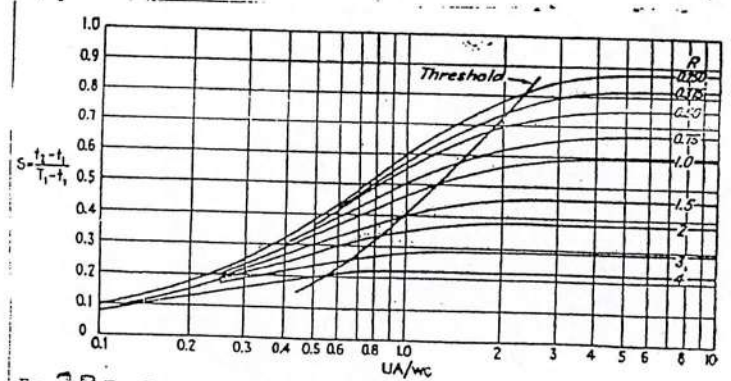


Fig. 38 Ten Broeck chart for determining t_2 when T_1 and t_1 are known in a 1-2 exchanger. (Industrial & Engineering Chemistry.)

(68)

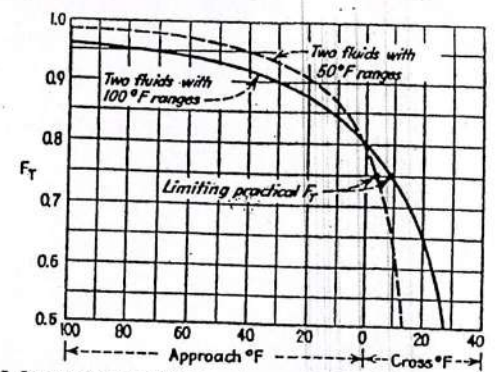


Fig. 39 Influence of approach temperature on F_T with fluids having equal ranges in a 1-2 exchanger.

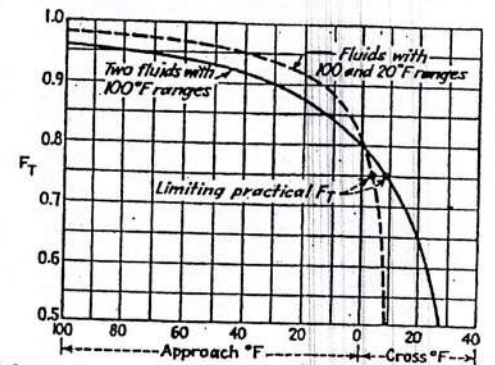


Fig. 40 Influence of approach temperature on F_T with fluids having unequal ranges in a 1-2 exchanger.

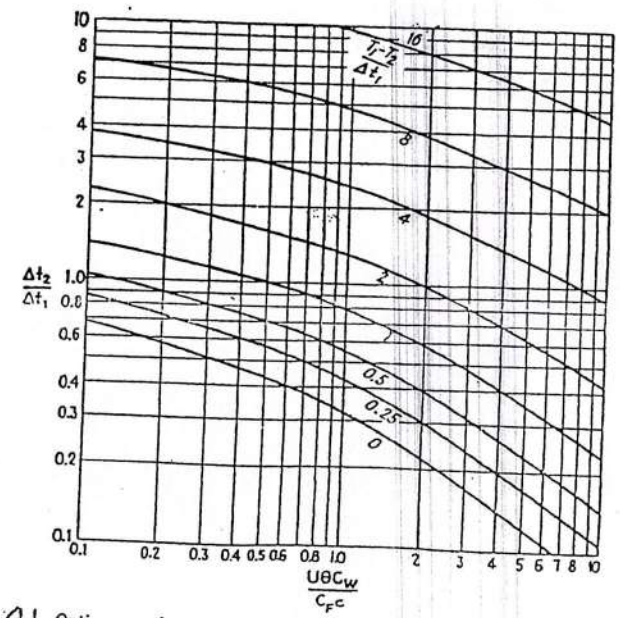
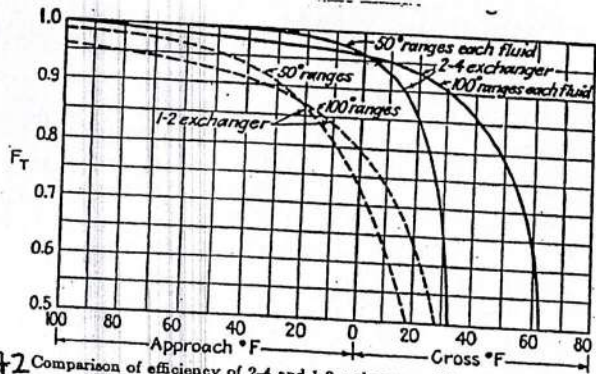


Fig. 41 Optimum outlet water temperature. (Perry, Chemical Engineers' Handbook, McGraw-Hill Book Company, Inc., New York, 1950.)



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Fig. 42 Comparison of efficiency of 2-4 and 1-2 exchangers with equal fluid temperature ranges.

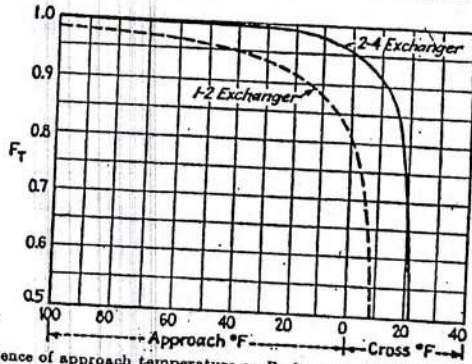


Fig. 43 Influence of approach temperature on F_T for unequal fluid temperature ranges.

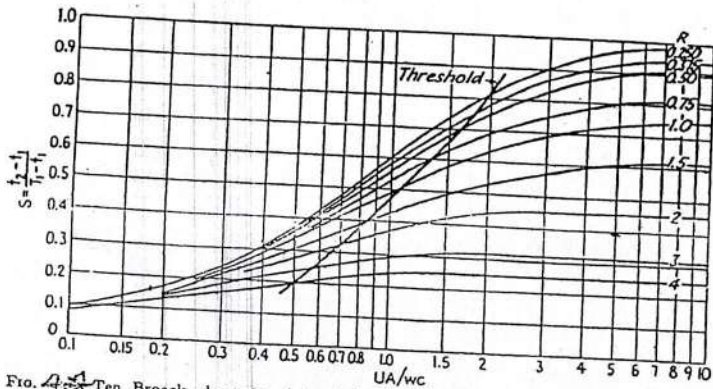
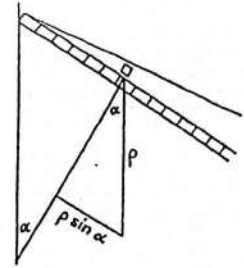
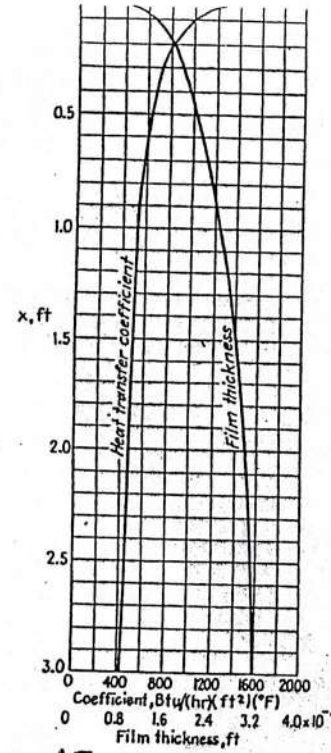
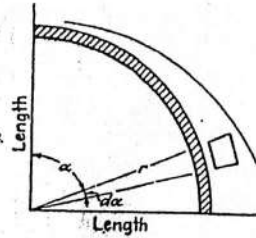


Fig. 44 Tea Broeck chart for determining t_1 in a 2-4 exchanger. (Industrial and Engineering Chemistry.)

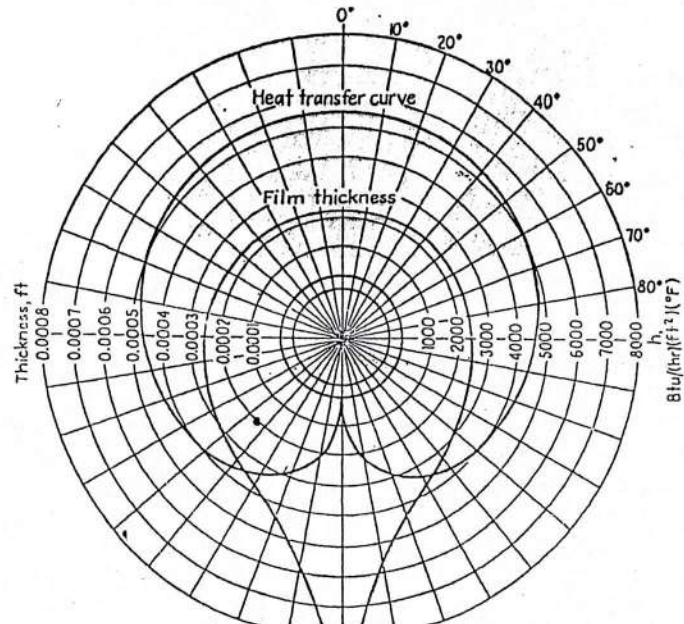


Film on an inclined surface



Condensate film on a horizontal

Fig. 45 Vertical film thickness and condensing coefficients for a descending film. (After Nusselt.)



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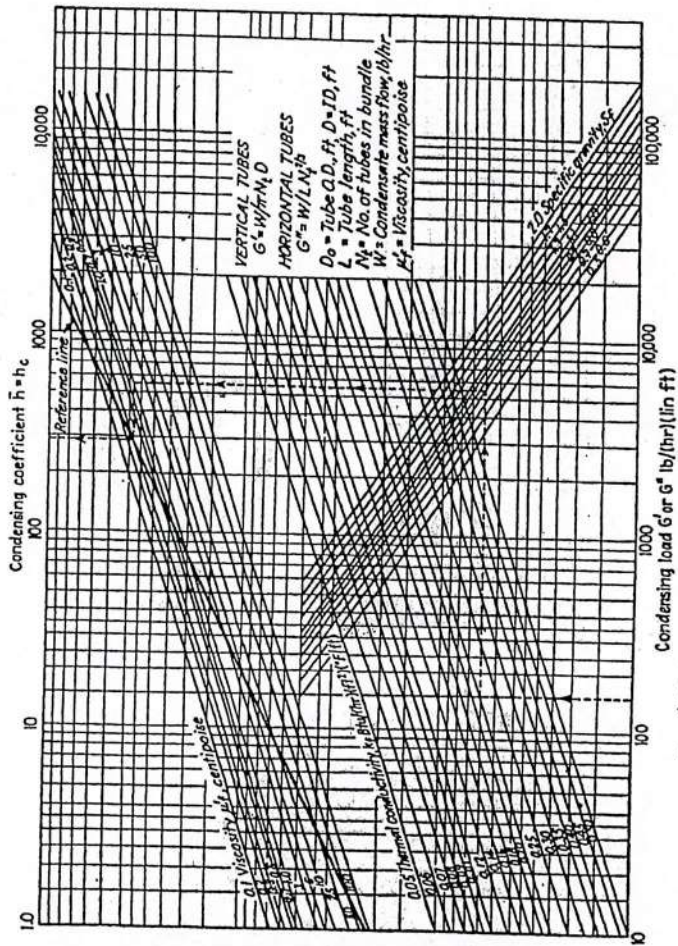


Fig. 47 Condensing coefficients.

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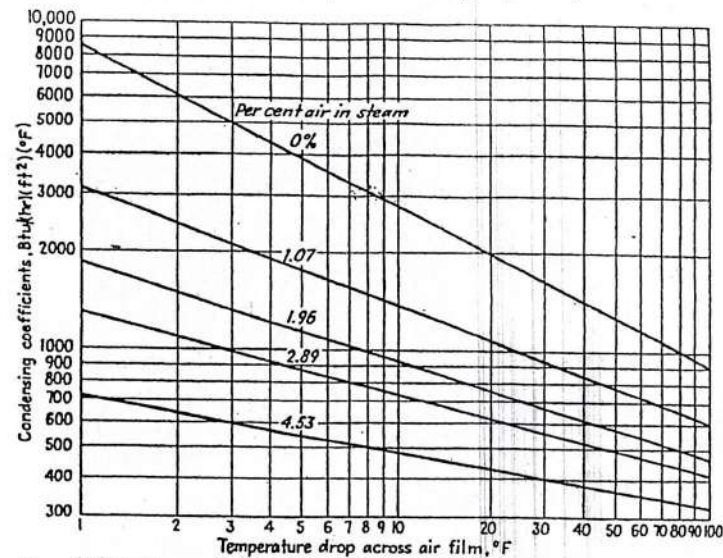


Fig. 48 Influence of air on the condensing coefficient of 230°F steam. (Data of Othmer.)

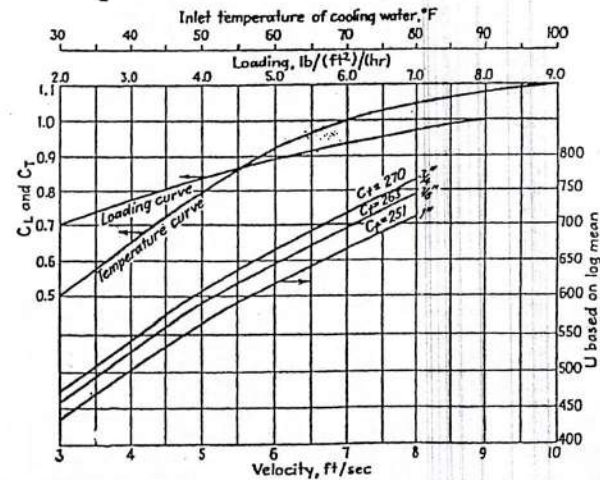
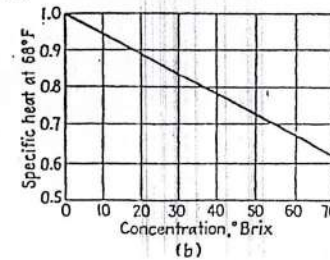
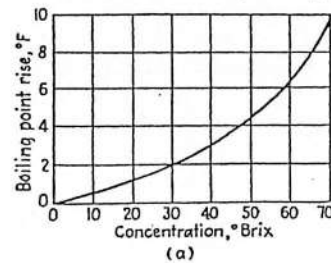


Fig. 49 Overall coefficients in surface condensers. (Heat Exchange Institute.)



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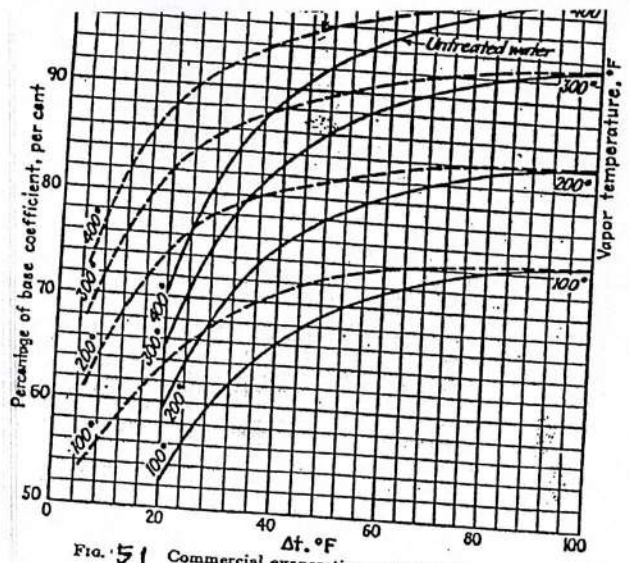


Fig. 51 Commercial evaporation coefficients for water.

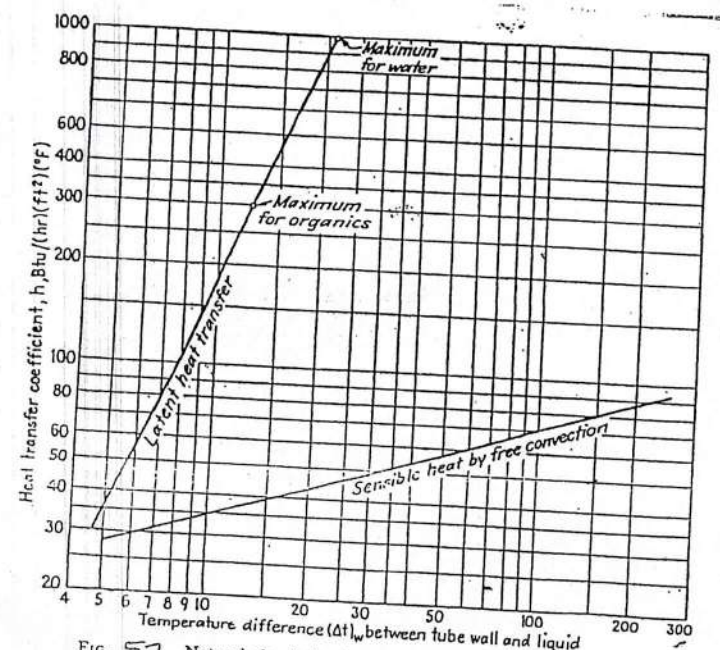


Fig. 52 Natural-circulation boiling and sensible film coefficients.

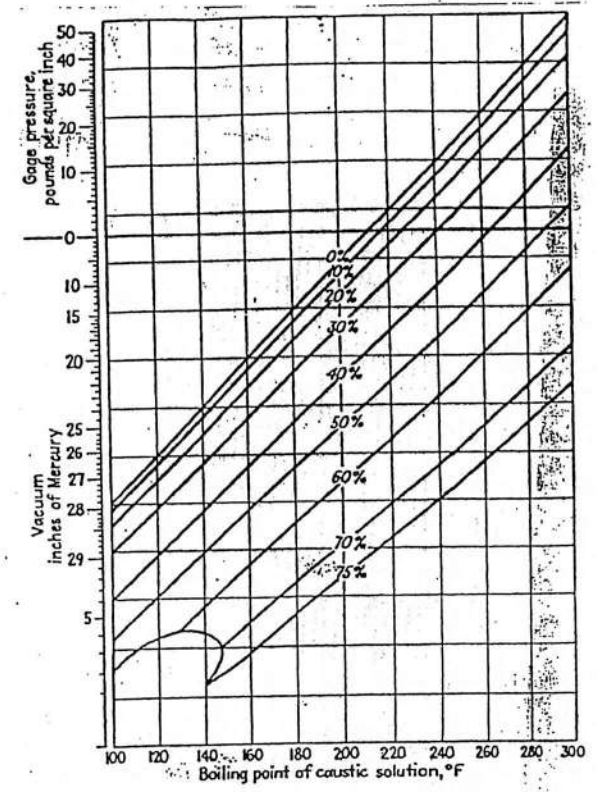
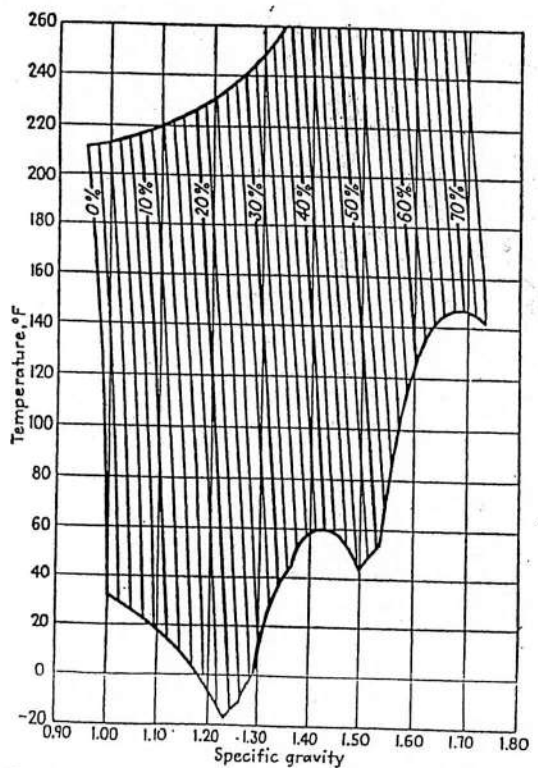


Fig. 53 Boiling-point-pressure relations of caustic soda solutions. (Columbia Alkali Corporation.)

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54. Specific gravity of caustic soda solutions. (Columbia Alkali Corporation.)

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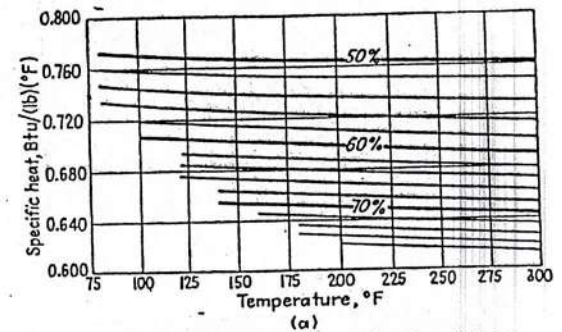


FIG. 55 a. Specific heats of high-concentration caustic soda solutions.

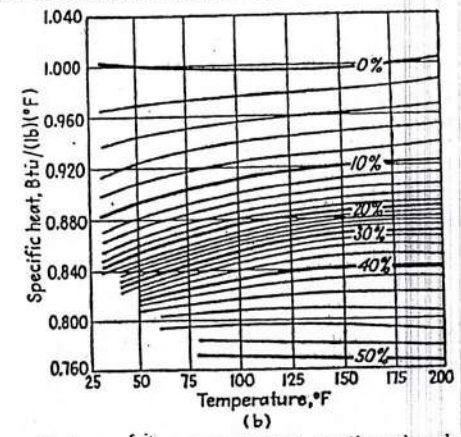


FIG. 55 b. Specific heats of low-concentration caustic soda solutions. (Columbia Alkali Corporation.)

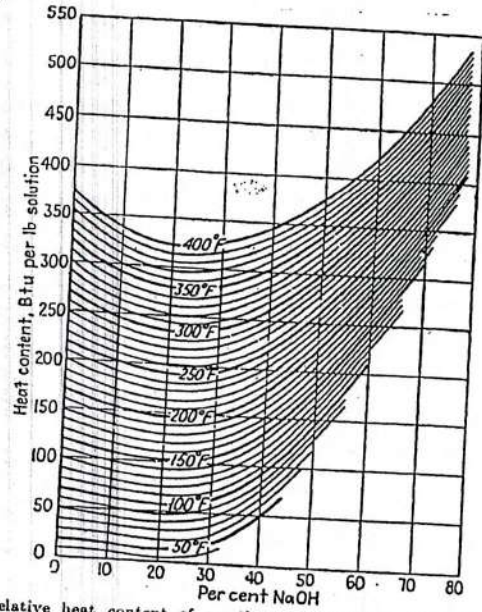


Fig. 56. Relative heat content of caustic soda solutions. (Columbia Alkali Corporation.)



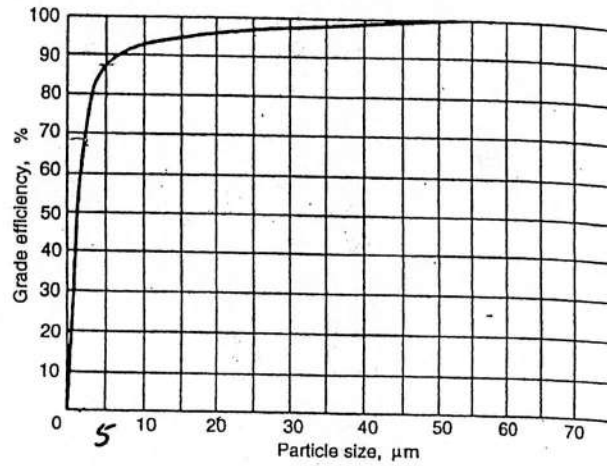
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Table 23 Gas-cleaning equipment

Type of equipment	Minimum particle size (μm)	Minimum loading (mg/m^3)	Approx. efficiency (%)	Typical gas velocity (m/s)	Maximum capacity (m^3/s)	Gas pressure drop (mm H_2O)	Liquid rate ($\text{m}^3/10^3 \text{ m}^3 \text{ gas}$)	Space required (relative)
<i>Dry collectors</i>								
Settling chamber	50	12,000	50	1.5-3	none	5	—	Large
Baffle chamber	50	12,000	50	5-10	none	3-12	—	Medium
Louver	20	2,500	80	10-20	15	10-50	—	Small
Cyclone	10	2,500	85	10-20	25	10-70	—	Medium
Multiple cyclone	5	2,500	95	10-20	100	50-150	—	Small
Impingement	10	2,500	90	15-30	none	25-50	—	Small
<i>Wet scrubbers</i>								
Gravity spray	10	2,500	70	0.5-1	50	25	0.05-0.3	Medium
Centrifugal	5	2,500	90	10-20	50	50-150	0.1-1.0	Medium
Impingement	5	2,500	95	15-30	50	50-200	0.1-0.7	Medium
Packed	5	250	90	0.5-1	25	25-250	0.7-2.0	Medium
Jet	0.5 to 5 (range)	250	90	10-100	50	none	7-14	Small
Venturi	0.5	250	99	50-200	50	250-750	0.4-1.4	Small
<i>Others</i>								
Fabric filters	0.2	250	99	0.01-0.1	100	50-150	—	Large
Electrostatic precipitators	2	250	99	5-30	1000	5-25	—	Large

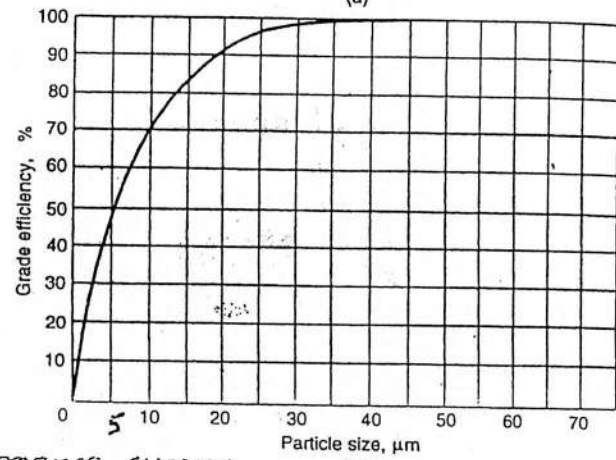
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High Efficiency cyclone



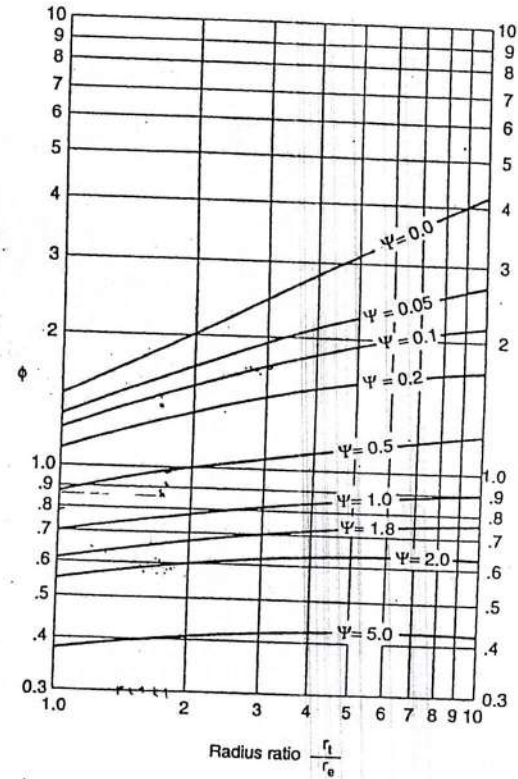
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High Throughput cyclone



(b)

Fig-57 Performance curves



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Figure 58 Cyclone pressure drop factor

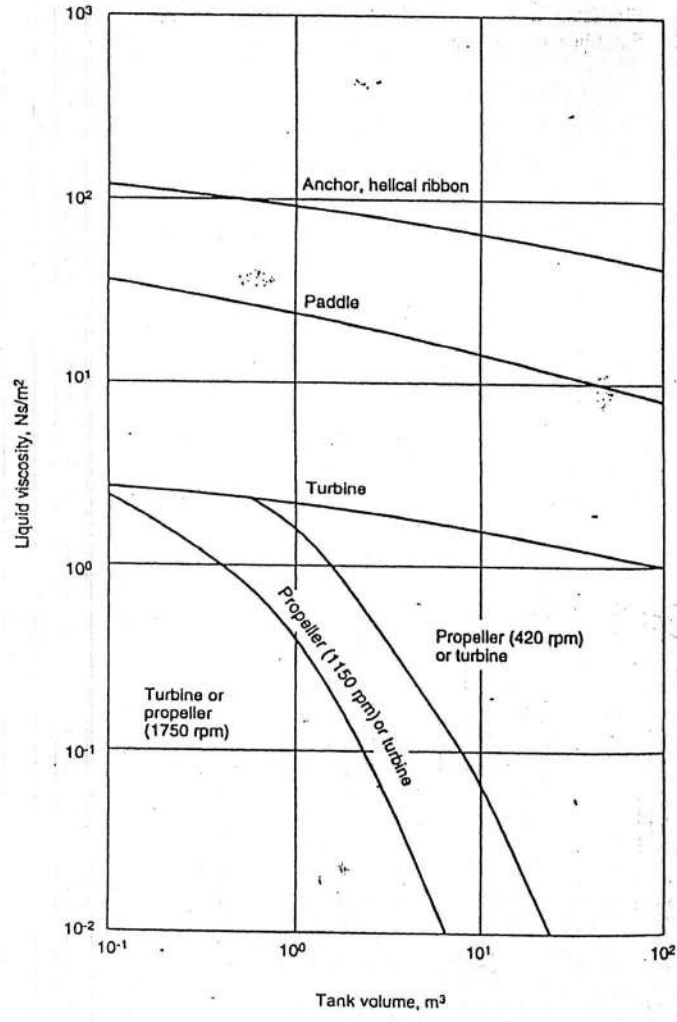


Figure 59 Agitator selection guide

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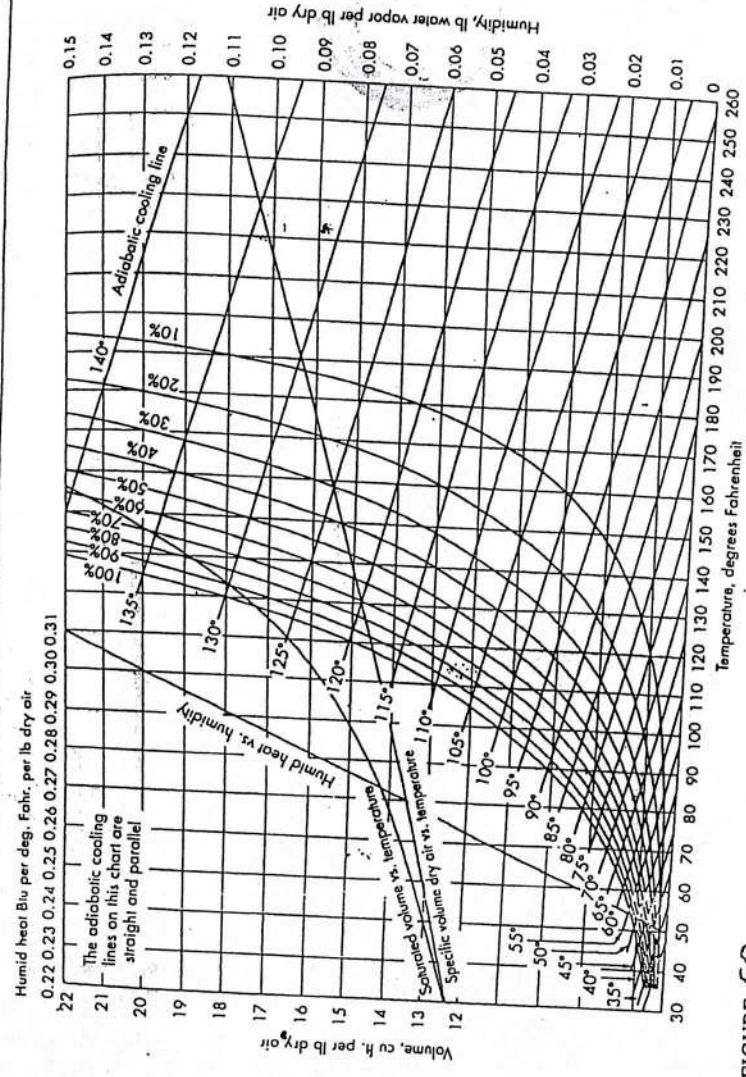


FIGURE 60 Humidity chart. Air-water at 1 atm.

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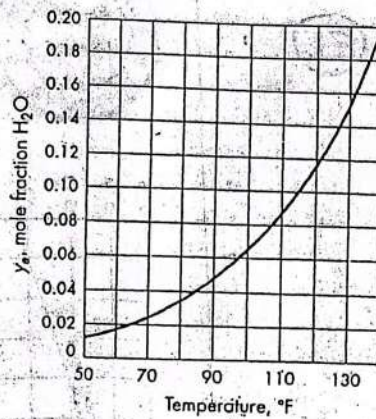


FIGURE 61
Equilibria for the system air-water at 1 atm.

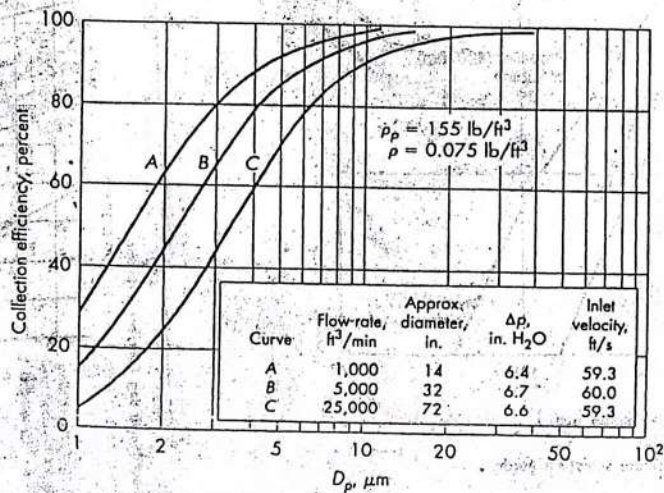


FIGURE 62
Collection efficiency of typical cyclones. (By permission, Fisher-Klosterman Inc., Louisville, KY.)